# **Chapter 9**

# The atmospheric chemistry of sulphur and nitrogen in power station plumes

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#### Abstract

Emissions of sulphur and nitrogen compounds from power stations represent a significant fraction of the total emissions of these elements to the atmosphere. Understanding their subsequent chemical reactions in the atmosphere is of fundamental importance as without it, a quantitative assessment of their contribution to local and regional scale air pollution is not possible. Here the atmospheric chemistry of sulphur dioxide and the oxides of nitrogen, and their resultant likely behaviour in the plumes of power stations are reviewed.

#### 1. Introduction

At least 90% of the sulphur present in fossil fuel enters the gas phase in the form of sulphur dioxide (SO<sub>2</sub>) during combustion, and, unless it is deliberately removed from the flue gas, is emitted to the atmosphere, leading to the global anthropogenic emission of about 65 Tg SO<sub>2</sub> (as S) yr<sup>-1</sup> (Benkovitz et al., 1996; Spiro et al., 1992). Globally, an increasing proportion of this reactive sulphur is emitted from power plants, as power generation becomes more and more concentrated on large units. High-temperature combustion processes also inevitably produce oxides of nitrogen (NO<sub>x</sub> = NO + NO<sub>2</sub>), leading to the global emission of about 21–25 Tg NO<sub>x</sub> (expressed as N) yr<sup>-1</sup> (Benkovitz et al., 1996; Dignon, 1992). SO<sub>2</sub> and NO<sub>x</sub> are important air pollutants with both environmental and health effects attributed to them. Both compounds may lead to the deposition of acidity ("acid deposition" or "acid rain") on the regional scale and NO<sub>x</sub> takes part in chemical reactions that lead to the formation of ozone (O<sub>3</sub>) in the troposphere, also on the regional scale. However, here the

First published in Atmospheric Environment 35 (2001) 1155-1170

focus is on the processes that affect  $SO_2$  and  $NO_x$  oxidation in power station plumes, particularly with respect to how these processes influence the concentrations of the primary pollutants and their products in the relatively near field, for example at receptor sites located tens of kilometres from the source.

# 2. Review of the chemistry of sulphur dioxide and the oxides of nitrogen in the atmosphere

A very considerable body of literature exists on the atmospheric chemistry of sulphur and nitrogen occurring inside power station plumes. This is derived from theoretical and experimental studies of the chemistry of S and N compounds in the gas and aerosol phases, supplemented by observations of concentration changes in the atmosphere, both inside and outside of power station plumes.

#### 2.1. Gas-phase oxidation of sulphur dioxide

In the gas phase,  $SO_2$  can potentially be subject to a large number of reactions involving reactive transient oxidants (Calvert et al., 1978). These reactions, shown in Table 1, are all thermodynamically possible in the atmosphere under ambient conditions of temperature and pressure, but have widely differing elementary rate constants, ranging from about  $10^{-12}$  to  $\sim 10^{-20}$  cm<sup>3</sup> molec<sup>-1</sup> s<sup>-1</sup>. Coupled with the wide range of concentrations of these various oxidants in the atmosphere, this variation in rate constants ensures that only very few of these possible reactions play any appreciable role in the oxidation of  $SO_2$  in the atmosphere. In fact, the reactions of SO<sub>2</sub> with oxygen atoms and ozone are unlikely to be important in the gas phase, with the possible exception of the reaction with the  $O(^{3}P)$  atom in the very early stages of stack gas dispersion.  $O(^{3}P)$  is formed by the photodissociation of NO<sub>2</sub>, and under conditions of very high NO<sub>2</sub> concentrations, such as might exist in a plume close to the point of emission, it is possible that significant  $O({}^{3}P)$  concentrations may result in appreciable SO<sub>2</sub> oxidation rates. However, as plume dilution with background air occurs, the instantaneous rate of this reaction will quickly fall.

Oxidation of SO<sub>2</sub> by ozone (O<sub>3</sub>) is highly exothermic ( $\Delta H = -242 \text{ kJ mol}^{-1}$ ). However with a gas-phase rate constant of  $k = \sim 8 \times 10^{-24} \text{ m}^3 \text{ molec}^{-1} \text{ s}^{-1}$ and a maximum likely ozone concentration of  $\sim 5 \times 10^{12} \text{ molec cm}^{-3}$  there will normally be insignificant SO<sub>2</sub> oxidation by this route (<  $1.4 \times 10^{-5}\% \text{ h}^{-1}$ ). Although the rate of the gas-phase reaction of SO<sub>2</sub> with ozone is extremely slow, the addition of an alkene to a dilute O<sub>3</sub>-SO<sub>2</sub> mixture in air results in the significant oxidation of the SO<sub>2</sub> (Cox and Penkett, 1971, 1972). The mechanisms behind this enhancement in oxidation rate are not fully elucidated but

Reaction	$-\Delta H^{\circ}$ (kJ mol <sup>-1</sup> ) 25°C	$\sum k (\mathrm{cm}^3 \mathrm{molec}^{-1} \mathrm{s}^{-1})$
$\label{eq:constraints} \hline \hline \hline O_2(^1\Delta_g) + SO_2 \rightarrow SO_4 \mbox{ (biradical)} \\ O_2(^1\Delta_g) + SO_2 \rightarrow SO_4 \mbox{ (cyclic)} \\ O_2(^1\Delta_g) + SO_2 \rightarrow SO_3 + O(^3P) \\ O_2(^1\Delta_g) + SO_2 \rightarrow SO_2(^3\Sigma_g^-) + SO_2 \\ \hline \hline \hline \end{tabular}$	$ \begin{array}{c} 105 \\ \sim 117 \\ -56.5 \\ 94 \end{array} $	$3.9 \times 10^{-20}$
$\begin{array}{l} O_2(^{1}\varSigma_g^+) + SO_2 \rightarrow SO_4 \ (biradical) \\ O_2(^{1}\varSigma_g^+) + SO_2 \rightarrow SO_4 \ (cyclic) \\ O_2(^{1}\varSigma_g^+) + SO_2 \rightarrow SO_3 + O(^{3}P) \\ O_2(^{1}\varSigma_g^+) + SO_2 \rightarrow SO_2 + O_2(^{1}\varDelta_g) \end{array}$	$ \begin{array}{c} 167\\ 180\\ 6.3\\ 62.8 \end{array} $	$6.6 \times 10^{-16}$
$O(^{3}P) + SO_{2}(+M) \rightarrow SO_{3}(+M)$	347	$5.7 \times 10^{-14}$
$SO_3 + SO_2 \rightarrow O_2 + SO_3$ $NO_2 + SO_2 \rightarrow NO + SO_2$	241 41.4	$< 8 \times 10^{-30}$ $8.8 \times 10^{-30}$
$NO_3 + SO_2 \rightarrow NO_2 + SO_3$	136	$< 7 \times 10^{-21}$
$ONOO + SO_2 \rightarrow NO_2 + SO_3$	$\sim$ 126	$< 7 \times 10^{-21}$
$N_2O_5 + SO_2 \rightarrow N_2O_4 + SO_3$	100	$< 4 \times 10^{-23}$
$HO_2 + SO_2 \rightarrow HO + SO_3$	69.9	
$HO_2 + SO_2(+M) \rightarrow HO_2SO_2(+M)$	29.3	$< 1 \times 10^{-18}$
$CHO_3O_2 + SO_2 \rightarrow CHO_3O + SO_3$	$\sim$ 113	$< 1 \times 10^{-18}$
$CHO_3O_2 + SO_2(+M) \rightarrow CHO_3O_2SO_2(+M)$	$\sim$ 130	$\sim$ 1.4 $\times$ 10 <sup>-14</sup>
$(CH_3)_3CO_2 + SO_2 \rightarrow (CH_3)_3CO + SO_3$	$\sim 109$	
$(CH_3)_3CO_2 + SO_2 \rightarrow (CH_3)_3CO_2SO_2$	$\sim$ 126	$< 7.3 \times 10^{-19}$
$CHO_3COO_2 + SO_2 \rightarrow CH_3CO_2 + SO_3$	$\sim$ 138	
$CHO_3COO_2 + SO_2 \rightarrow CH_3COO_2SO_2$	$\sim 155$	$< 7 \times 10^{-19}$
$\text{HO} + \text{SO}_2(+M) \rightarrow \text{HOSO}_2(+M)$	$\sim 155$	$1.1 \times 10^{-12}$
$CHO_3O + SO_2(+M) \rightarrow CH_3OSO_2(+M)$	$\sim 100$	$\sim$ 5.5 $\times$ 10 <sup>-13</sup>
$SO_3 + H_2O \rightarrow H_2SO_4$	24.8	$9.1 \times 10^{-13}$

Table 1. Enthalpy changes and rate constants for potentially important reactions of ground state  $SO_2$  and  $SO_3$  molecules in the lower atmosphere (adapted from Calvert, 1984)

are most likely due to the formation of the Criegee intermediate  $(CH_2O_2)$  and its reaction with SO<sub>2</sub>. However, the significance of this reaction in the real atmosphere is difficult to assess, since the effect of addition of NO to the reaction mixture, and competition between NO and SO<sub>2</sub> for reaction with  $CH_2O_2$ , is not fully known.

By far the most important route of oxidation of  $SO_2$  in the gas phase is by reaction with the hydroxyl radical, OH (e.g. McAndrew and Wheeler, 1962; Harris and Wayne, 1975; Castleman and Tang, 1976; Atkinson et al., 1976; Davis et al., 1979a, b; Cox and Sheppard, 1980; Harris et al., 1980; Leu, 1982).

In the unpolluted atmosphere, OH is produced by the photolysis of  $O_3$  and the subsequent reaction of oxygen atoms with water vapour:

$$O_3 + h\nu \rightarrow O({}^3P) + O_2 \quad \lambda > 315 \,\mathrm{nm}$$

 $O(^{3}P) + O_{2} + M \rightarrow O_{3} + M$ 

or

$$O_3 + h\nu \rightarrow O(^1D) + O_2 \quad \lambda < 315 \text{ nm}$$
  
 $O(^1D) + M \rightarrow O(^3P) + M \quad 96\%$ 

but

$$O(^{1}D) + H_{2}O \rightarrow 2OH \quad 4\%$$

In polluted air, the photolysis of nitrous acid (HONO) and hydrogen peroxide  $(H_2O_2)$  produce OH directly

$$HONO + hv \rightarrow OH + NO \quad \lambda < 400 \text{ nm},$$

$$H_2O_2 + h\nu \rightarrow 2OH \quad \lambda < 360 \text{ nm}.$$

Under more polluted conditions, OH radicals are produced by the photolysis of the products of the incomplete combustion of fossil fuels, especially aldehydes, ketones and other oxygenated organic compounds. For example, formaldehyde photolysis leads to

> HCHO +  $h\nu \rightarrow$  H + CHO  $\lambda < 335 \text{ nm}$ CHO + O<sub>2</sub>  $\rightarrow$  HO<sub>2</sub> + CO H + O<sub>2</sub> + M  $\rightarrow$  HO<sub>2</sub> + M HO<sub>2</sub> + HO<sub>2</sub>  $\rightarrow$  H<sub>2</sub>O<sub>2</sub> + O<sub>2</sub>

then

$$H_2O_2 + h\nu \rightarrow 2OH \quad \lambda < 360 \,\mathrm{nm}.$$

Hydroxyl then rapidly reacts with SO<sub>2</sub> by addition:

$$OH + SO_2 + M \rightarrow HOSO_2 + M$$

where M is another molecule (usually  $N_2$ ) that is required to absorb excess kinetic energy from the reactants. At the pressures pertaining in the lower atmosphere the rate of this reaction is independent of the concentration of M and hence it is effectively a second-order reaction.

Many attempts have been made to measure the rate constant for the OH- $SO_2$  reaction in the laboratory (e.g. Cox, 1975; Castleman and Tang, 1976;

252

Atkinson et al., 1976; Cox and Sheppard, 1980; Harris et al., 1980) and rather a wide range of values have been obtained. However, Atkinson and Lloyd (1984) recommend an effective bimolecular rate constant at 1 atm and 298 K of  $9 \times 10^{-13}$  cm<sup>3</sup> molec<sup>-1</sup> s<sup>-1</sup>, with an uncertainty of around  $\pm 50\%$ . For an average ambient OH concentration of  $1 \times 10^6$  radicals cm<sup>-3</sup> (Hewitt and Harrison, 1985) the lifetime of SO<sub>2</sub> with respect to this one gas phase reaction will be ~13 d in the "typical" troposphere.

Once formed, the free radical HOSO<sub>2</sub> will rapidly react with oxygen to form SO<sub>3</sub>, which in turn will rapidly react with water vapour to form sulphuric acid,  $H_2SO_4$  (Goodeve et al., 1934; Cox and Penkett, 1971; Calvert et al., 1978; Stockwell and Calvert, 1983):

$$HOSO_2 + O_2 \rightarrow HO_2 + SO_3$$
,

$$SO_3 + H_2O \rightarrow H_2SO_4$$
.

Eatough et al. (1994) point out that the rate of conversion of SO<sub>2</sub> to sulphate by OH will increase with both increasing temperature and relative humidity. In practise, the rate of the homogeneous gas-phase conversion of SO<sub>2</sub> to sulphate can vary from much less than  $1\% h^{-1}$  up to a probable maximum of  $10\% h^{-1}$  under optimum atmospheric conditions.

#### 2.2. Aqueous phase oxidation of sulphur dioxide

The presence of aqueous droplets in the atmosphere offers another phase in which oxidation of SO<sub>2</sub> can occur. After transport of the gas to the surface of the droplet and transfer of the gas across the air-liquid interface, SO<sub>2</sub> can dissolve in water and establish an equilibrium with its ionic products, with the aqueous-phase concentrations described at equilibrium by the Henry's law constant. As a result, dissolved SO<sub>2</sub> actually consists of three species, hydrated SO<sub>2</sub> (SO<sub>2</sub>·H<sub>2</sub>O), the bisulphite ion (HSO<sub>3</sub><sup>-</sup>) and the sulphite ion (SO<sub>3</sub><sup>2-</sup>):

$$SO_2 + H_2O \rightleftharpoons SO_2 \cdot H_2O$$
,

$$SO_2 \cdot H_2O \rightleftharpoons HSO_3^- + H^+,$$

$$HSO_3^- \rightleftharpoons SO_3^{2-} + H^+$$

The predominant form depends upon the acidity of the solution in which the  $SO_2$  dissolves, since the hydrogen ion concentration will drive the equilibrium either to the left or right (Martin and Damschen, 1981). The oxidation state of the sulphur in the various products is +4, and hence S(IV) is used to denote all

these forms of sulphur taken together. In contrast, the oxidised form of sulphur (i.e.  $H_2SO_4$  and  $SO_4^{2-}$ ) is in the +6 oxidation state and hence is referred to as S(VI). There are several possible routes of oxidation of S(IV) to S(VI) and these are now briefly considered.

Molecular oxygen may oxidise S(IV) to S(VI) but in the absence of a catalyst the reaction is insignificant. Although both iron (III) and manganese (II) appear to catalyse the reaction it is still relatively slow and unlikely to be of significance (e.g. Huss et al., 1982; Martin and Good, 1991; Martin et al., 1991).

As noted above,  $O_3$  reacts very slowly with  $SO_2$  in the gas phase, but in the liquid phase the reaction is rapid (e.g. Penkett et al., 1979):

$$S(IV) + O_3 \rightarrow S(VI) + O_2$$

At ambient gas-phase concentrations of 30–60 ppb and a Henry's law constant of  $0.01 \text{ mol } 1^{-1} \text{ atm}^{-1}$ , the expected aqueous-phase equilibrium concentration of O<sub>3</sub> will be around  $(3-6) \times 10^{-10} \text{ mol } 1^{-1}$ . Although this concentration is around 6 orders of magnitude lower than that for dissolved O<sub>2</sub>, oxidation of S(IV) by O<sub>3</sub> is much more important under most conditions because of the much higher rate constant for the reaction, which is pH dependent (e.g. Lagrange et al., 1994; Botha et al., 1994). At a pH greater that around 4 this is likely to be an important route of oxidation of S(IV) in water droplets.

Hydrogen peroxide has been shown to oxidise S(IV) relatively rapidly in solution and in fact is one of the most effective oxidants of S(IV) in solution (Penkett et al., 1979). Because of its high solubility, with a Henry's law constant of  $1 \times 10^5$  M atm<sup>-1</sup>, a 1 ppb gas-phase concentration of  $H_2O_2$  would produce an equilibrium aqueous-phase concentration at 298 K of around  $1 \times 10^{-4}$  moll<sup>-1</sup>, or 6 orders of magnitude greater than the solution-phase equilibrium  $O_3$  concentration. The rate constant for the reaction of  $H_2O_2$  and S(IV) is largely pH independent, and at a gas-phase  $H_2O_2$  concentration of 1 ppb is around  $300 \times 10^{-6}$  M h<sup>-1</sup> (ppb  $SO_2$ )<sup>-1</sup>. Organic peroxides have also been proposed as potential aqueous phase S(IV) oxidants but have lower Henry's law constants and lower gas-phase concentrations than does  $H_2O_2$  and are considered to normally be of minor importance in this regard (Lind et al., 1987).

The different routes of aqueous-phase oxidation of S(IV) can be compared as a function of pH and temperature (Seinfeld and Pandis, 1998), using starting conditions of, for example, 5 ppb SO<sub>2</sub>, 1 ppb NO<sub>2</sub>, 1 ppb H<sub>2</sub>O<sub>2</sub>, 50 ppb O<sub>3</sub>, 0.3  $\mu$ M Fe(III) and 0.03  $\mu$ M Mn(II). Under practically all conditions, oxidation by dissolved H<sub>2</sub>O<sub>2</sub> is the predominant pathway for sulphate formation. Only at pH values greater than 5 does oxidation by O<sub>3</sub> start to dominate, and at pH 6 this route is around 10 times faster than that by H<sub>2</sub>O<sub>2</sub>. Assuming a liquid cloud water content of 1 g m<sup>-3</sup>, the rate of oxidation by H<sub>2</sub>O<sub>2</sub> can exceed 500% h<sup>-1</sup>. In contrast to the homogeneous gas-phase reactions of SO<sub>2</sub> the aqueous-phase process is therefore largely controlled by mixing and reactant limitations, rather than kinetic considerations (Eatough et al., 1994).

#### 2.3. Gas-phase oxidation of the oxides of nitrogen

Homogeneous formation of nitric acid by the oxidation of NO and NO<sub>2</sub> appears to be a much less complicated, and better understood process than the formation of sulphuric acid from sulphur dioxide. Most work on NO<sub>x</sub> oxidation has been carried out in polluted air and this may hinder extrapolation of predicted oxidation rates to the case of power station plumes. NO and smaller amounts of NO<sub>2</sub> are formed during high temperature combustion processes, with power stations emitting NO<sub>x</sub> (the sum of NO and NO<sub>2</sub>) as ~ 95% NO and ~ 5% NO<sub>2</sub>.

The termolecular reaction of NO with O<sub>2</sub>:

$$2NO + O_2 \rightarrow 2NO_2$$

is very slow at atmospheric temperatures and, except at extremely high NO concentrations, is insignificant compared with the reactions of NO with  $O_3$ , OH, HO<sub>2</sub> (hydroperoxy) and RO<sub>2</sub> (alkylperoxy):

 $NO + O_3 \rightarrow NO_2 + O_2$ ,  $NO + HO_2 \rightarrow NO_2 + OH$ ,  $NO + RO_2 \rightarrow NO_2 + RH$ .

The peroxyradicals,  $HO_2$  and  $RO_2$ , are formed in chain reactions in the atmosphere, initiated by the attack of hydroxyl on reactive hydrocarbons. For example, in the simplest (but slowest) case involving methane

$$CH_4 + OH \rightarrow CH_3 + H_2O,$$

$$CH_3 + O_2 + M \rightarrow CH_3O_2 + M,$$

$$CH_3O_2 + NO \rightarrow NO_2 + CH_3O,$$

$$CH_3O + O_2 \rightarrow HCHO + HO_2,$$

$$H_2O + NO \rightarrow NO_2 + OH.$$

There is some observational evidence that the termolecular reaction with  $O_2$  may play a role in the rapid oxidation of NO to NO<sub>2</sub> in highly polluted urban air in the wintertime, when the concentrations of the photochemically produced oxidants  $O_3$ , OH, HO<sub>2</sub> and RO<sub>2</sub> are likely to be very low. However the role of free radical chemistry is also now thought to be significant, even in wintertime smog episodes (Harrison and Shi, 1996; Shi and Harrison, 1997; Harrison et al., 1998).

Overall, then, the predominant fate of emitted NO is oxidation to  $NO_2$  which can then react with OH during the daytime:

$$NO_2 + OH + M \rightarrow HNO_3 + M.$$

A great variety of experimental studies support the view that this reaction is relatively rapid, with an effective 2nd order rate constant at 1 atm in air of around  $1.1 \times 10^{-11}$  cm<sup>3</sup> molec<sup>-1</sup> s<sup>-1</sup> at 298 K (Atkinson and Lloyd, 1984), approximately ten times the rate of the SO<sub>2</sub>–OH reaction.

A second potentially important source of nitric acid involves the reaction of the nitrate radical, NO<sub>3</sub>, with some organic compounds. The nitrate radical is formed in the presence of NO<sub>2</sub> and O<sub>3</sub> and is in equilibrium with  $N_2O_5$  in the atmosphere:

$$O_3 + NO_2 \rightarrow NO_3 + O_2$$
  
 $k = 3.2 \times 10^{-17} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1}$  (Atkinson and Lloyd, 1984)

$$NO_3 + NO_2 \rightleftharpoons N_2O_5$$
.

NO<sub>3</sub> reacts relatively rapidly with a variety of organics, and in the case of alkanes and aldehydes, the reaction is believed to proceed by hydrogen abstraction to form nitric acid:

$$NO_3 + RH \rightarrow HNO_3$$
,

$$NO_3 + RCHO \rightarrow RCO + HNO_3$$
.

In polluted urban air, alkane concentrations (excluding CH<sub>4</sub>) are typically around 100 ppb  $(2.5 \times 10^{12} \text{ molec cm}^{-3})$  and total aldehyde concentrations are of the order of tens of ppb. Using an estimated NO<sub>3</sub> concentration of 100 ppt, the calculated rate of formation of HNO<sub>3</sub> formation by this route would be around 0.3 ppb h<sup>-1</sup>. This can be compared to the daytime rate of formation of HNO<sub>3</sub> by reaction of NO<sub>2</sub> with the OH radical of around 2 ppb h<sup>-1</sup>, at an NO<sub>2</sub> concentration of 50 ppb and an average OH concentration of 1 × 10<sup>6</sup> cm<sup>-3</sup> (Hewitt and Harrison, 1985). Thus the rate of nighttime formation of HNO<sub>3</sub> is likely to be rather insignificant relative to the rate of daytime formation. Another potential source of nitric acid is the hydrolysis of  $N_2O_5$  (Platt and Perner, 1980):

$$N_2O_5 + H_2O \rightarrow 2HNO_3$$

where  $k < 1.3 \times 10^{-11} \text{ cm}^3 \text{ molec}^{-1} \text{ s}^{-1}$  (Tuazon et al., 1983). This rate constant is sufficiently large to ensure that this reaction may contribute significantly to HNO<sub>3</sub> formation in the polluted atmosphere. In fact, Tuazon et al. (1983) estimated a formation rate of  $0.3 \text{ ppb} \text{ h}^{-1}$  at NO<sub>2</sub> and NO<sub>3</sub> concentrations of 3 ppb and 100 ppt, respectively, at 50% relative humidity. This is similar to the rate of formation due to the reactions of the nitrate radical with alkanes and aldehydes. Other studies, including Jones and Seinfeld (1983) and Richards et al. (1981, 1983) confirm this.

## 2.4. Aqueous phase oxidation of the oxides of nitrogen

Some field studies (e.g. Lazrus et al., 1983) have indicated appreciable formation of nitric acid in the aqueous phase in the atmosphere (NO<sub>2</sub> conversion rates of ~ 8% h<sup>-1</sup>, Gertler et al., 1984), but laboratory studies are less conclusive. In fact, aqueous phase oxidation of the oxides of nitrogen probably proceeds far too slowly under ambient conditions to contribute to either the significant removal of these gas-phase compounds or to cloud-water acidification (rate constants of  $2 \times 10^{10}$  and  $1.3 \times 10^9$  M<sup>-1</sup> s<sup>-1</sup>, for the reactions of NO and NO<sub>2</sub> with OH, respectively).

## 2.5. Sulphuric and nitric acids compared

Once formed in the atmosphere sulphuric and nitric acids show very different behaviours, both physically and chemically. Nitric acid is more volatile and hence exists in significant concentrations in the gas phase, while sulphuric acid has a very low vapour pressure under ambient conditions and hence exists in the form of aerosol phase particles.

Both nitric acid and sulphuric acid will react with alkaline substances in the atmosphere to produce salts, the most important of these under ambient conditions being the ammonium compounds resulting from reactions with ammonia (APEG, 1999; Lee and Atkins, 1994; Langford et al., 1992).

When  $HNO_3$  reacts with  $NH_3$  an equilibrium is established (Hidleman et al., 1984):

$$HNO_3 + NH_3 \rightleftharpoons NH_4NO_3$$
.

The ammonium nitrate exists as a solid if the relative humidity is less than that of deliquescence. At higher relative humidities it will exist as aerosol droplets. However at elevated temperatures, above  $\sim 310$  K, little NH<sub>4</sub>NO<sub>3</sub> will exist in

the atmosphere, since the dissociation constant is temperature dependent and the above reaction will move to the left (Mozurkewich, 1993).

In polluted air, where high concentrations of both NO<sub>x</sub> and SO<sub>2</sub> are present, the oxidation chemistries of these compounds become intertwined. As NO<sub>x</sub> concentrations increase, so the gas-phase concentration of OH will decrease, hence lowering the rate of oxidation of SO<sub>2</sub>. Similarly, high concentrations of NO<sub>x</sub> will lead to a decrease in the rate of formation of H<sub>2</sub>O<sub>2</sub> as the NO molecules will compete for reaction with HO<sub>2</sub>, so reducing the number of HO<sub>2</sub> radicals available for the self-reaction needed to produce H<sub>2</sub>O<sub>2</sub>.

#### 2.6. Removal of sulphur and nitrogen by wet and dry deposition processes

Both the primary pollutants,  $SO_2$  and  $NO_x$ , and their secondary products,  $H_2SO_4$ ,  $HNO_3$ ,  $SO_4^{2-}$  and  $NO_3^-$ , as well as their further reaction products, e.g.  $(NH_4)_2SO_4$  and  $NH_4NO_3$ , are subject to continuous removal from the boundary layer by the process of dry deposition to the Earth's surface. This process may be parameterized by the use of a deposition velocity, the magnitude of which varies from compound to compound and with environmental conditions and the nature of the surface. A typical range of deposition velocities reported for various pollutants and surfaces is  $0.1-2 \text{ cm s}^{-1}$ . Additionally, intermittent deposition may occur for soluble gases and particles by the process of wet deposition. Although wet deposition may be extremely efficient, it is, by its nature, sporadic.

The current understanding of dry deposition has recently been authoritatively reviewed by Wesely and Hicks (2000) while recent measurements of the deposition velocity of SO<sub>2</sub> include those of Horvath et al. (1998), who found values of  $0.19-0.20 \,\mathrm{cm \, s^{-1}}$  over short vegetation. However, it is recognized that more direct measurements of deposition fluxes and deposition velocities are required for the improved parametization of deposition models. Such models (e.g. those contained within the Acid Deposition and Oxidant Model (ADOM: Pleim et al., 1984), the Regional Acid Deposition Model (RADM: Walmsley and Wesely, 1996) and the Routine Deposition Model (RDM: Brook et al., 1999) appear to give a reasonable description of pollutant deposition integrated over time and space (e.g. monthly deposition fluxes on a  $10 \text{ km} \times 10 \text{ km}$  grid) but their utility in describing removal rates from a plume as it rapidly moves over complex and varying terrain are very limited (Park, 1998). Similarly, wet deposition, resulting from cloud and precipitation scavenging, can be very effective in removing pollutants (Martin, 1984; Pruppacher and Klett, 1978; Bidleman, 1988) but is extremely difficult to model for a plume, due to its intermittent nature.

#### 3. Power station plume chemistry

#### 3.1. Observations

A large number of field studies have been carried out with the aim of validating the understanding of sulphur and nitrogen pollution chemistry obtained theoretically or in the laboratory and/or with the aim of obtaining observational estimates of the rate of oxidation of sulphur and nitrogen (and hence the rate of formation of sulphate and nitrate) in power station plumes. The oxidation rates observed in plumes may well be expected to differ from those predicted or observed in ambient or background air for a number of reasons, including the possibility of enhanced concentrations of catalysts and the rapid depletion of oxidants (e.g. removal of  $O_3$  by reaction with NO) within the plume. However, very few studies have procured sufficient simultaneous measurements of  $SO_2$  and  $NO_x$  concentrations to allow a full understanding of the relative rates of removal of these gases from discrete plumes. This poses a major limitation on the conclusions that can be drawn.

The SO<sub>2</sub> oxidation rates seen in plumes from point sources vary from nearly zero to more that  $16\% h^{-1}$ . In urban plumes even higher oxidation rates, up to  $30\% h^{-1}$ , have been reported. Part of this variation may be attributable to uncertainties in data collection and interpretation, but the wide variations in plume compositions and background conditions, both chemical and meteorological, are also important.

As already noted above, heterogeneous oxidation of SO<sub>2</sub> may be very rapid under certain conditions and will depend on the amount of water vapour available for the formation of droplets. Additionally, experimental studies (e.g. Haury et al., 1977) and modelling of the H<sub>2</sub>SO<sub>4</sub>-H<sub>2</sub>O gas-phase binary system have shown that the rates of nucleation and condensation and hence of the rate of formation of sulphate aerosol is largely controlled by the concentration of water vapour present. However, most field studies of plume chemistry, particularly those involving aircraft, have been conducted in conditions where the aqueous-phase reactions were not favoured. The SO<sub>2</sub> oxidation rates discussed below are summarised in Table 2. Although the focus of most early field studies was the formation of sulphate and nitrate (in the frame of a general concern about acid deposition and environmental acidification), more recently the focus has shifted somewhat to the role of power plant plumes to the formation of ozone and other oxidants in the lower atmosphere. For example, Gillani et al. (1998a, b), Ryerson et al. (1998), Luria et al. (1999, 2000), Sillman (2000), St. John and Chameides (2000) and Nunnermacker et al. (2000) all studied the formation of  $O_3$  in power plant plumes, rather than, explicitly, sulphate and nitrate formation.

Location of source	Plume age (h)	Stack distance (km)	Travel time (h) of sampling	Month and year rate	Oxidation data (% h <sup>-1</sup> )	No of rate points	Average (% h <sup>-1</sup> )	Rate derivation, method comments	Reference
Coal fired power	·								
plants									
Cumberland, TN, USA	1.5–10	8160	1.67–12	Aug. 1978	< 0.1-7.5	19	3	Particulate S/total S ratio	Gillani et al. (1977, 1978, 1981, 1983)
Johnsonville, TN, USA	6–8	56160	68	Aug. 1978	0.8-8.5	6	3	Dry conditions only	
Cumberland, TN, USA	1.3–10.7		2.15-4.77	Jul./Aug. 1976	1.1-8.5	5	5.5	Average daytime rate	Zak (1981)
	0–7		1.35-7.03	Aug. 1978	0.4–16.7	5	6.1	Stack to first measurement	
								Particulate S/gaseous S ratio	
Keystone, PA, USA			0.5–2.67	Apr./May/Sep./ Oct. 1978	0.01-5.92	13	0.05	At r.h 42-64%	Dittenhoeffer and De Pena (1980)
							0.78	At r.h 65-90%	
							3.31	At r.h 91-100%	
								Particulate S/total	
								S ratio	
Paradise, KY, USA			0.2-3.8	Jun.	0-1.3	5		Particulate S/total	Meagher et al.
								S ratio	(1981)
Colbert, AL, USA		7–50	0.28-5.20	May/Jun.	0.78–2.79	12	1.3	Morning rate	Meagher and Luria (1982)

Table 2.	Oxidation rates of S(IV) in plumes (adapted from Harter, 1985)
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Table 2. (Continued	l)								
Location of source	Plume age (h)	Stack distance (km)	Travel time (h) of sampling	Month and year rate	Oxidation data (% h <sup>-1</sup> )	No of rate points	Average $(\% h^{-1})$	Rate derivation, method comments	Reference
Widows Creek, AL, USA		2-49.3	0.43-6.01	Aug.	0.34-3.41	17	1	Morning rate	
							2.4	Afternoon rate Particulate S/total S ratio	
Cumberland, TN, USA	0.76–9 11–2	9 11-200		Aug. 1978 0.1–7	0.1–7	21	3	Late morning & afternoon	Forrest et al. (1981)
							0.5	Night & early morning	(1)0()
							2	Average diurnal rate Particulate S/total S ratio	
Bowen, GA, USA			0.12-3.33	Dec. 1979	0–2.3	7	< 0.2	Particulate S/total S ratio	Liebsch and De Pena (1982)
Breed, IN, USA	1.3-6.8			Jun./Nov. 1977	0-3.7	7	1	Particulate S/total S ratio	Easter et al. (1980)
Cobb. MI, USA	1.1-3			May/Nov. 1977	0.2-8.4	6	2.6		<b>()</b>
Labadie, MO, USA	0.8-12	12-320	0.83-12	Jul. 1976	0.3–3.2	17	1–3	Particulate S/total S ratio	Gillani and Wilson (1980)
Labadie, MO, USA	0.7-12.5	14360		Aug. 1974/Jul. 1976	0.1-4.8	50	1.6	Particulate S/total S ratio Rate 1-4% h <sup>-1</sup> d <sup>-1</sup> , < 0.5 night	Husar et al. (1978)
Leland-Olds, ND, USA			0.38-1.08	Jun. 1978	0-0.06	4		Change in total particle volume & particulate S/total S ratio	Hegg and Hobbs (1980)

Location of source	Plume	Stack	Travel time (h) of sampling	Month and year rate	Oxidation	No of rate points	Average (% h <sup>-1</sup> )	Rate derivation, method comments	Reference
	age (h)	distance (km)			data (% h <sup>-1</sup> )				
Big Brown, TX, USA			0.63-1.32	Jun. 1978	0.15-5.7	4			
Sherburne Co. MN, USA			0.17–2.7	Jun. 1978	0-2.2	4			
Centralia, WA, USA			0.03-1.42	Mar./Oct. 1976	0.03-0.56	5		Change in total particle volume	Hobbs et al. (1979)
				Sep./Oct. 1977					
Four Corners, NM, USA			0.78–0.87	Jun. 1977	0.34-6.6	3			
Navajo AZ, USA	3-6.1			Jun./Jul. 1979	0.7–13	22	1.9	Rate at noon	Wilson and McMurry (1981)
							0.9	Diurnal average Particle volume/ Total S ratio	
Great Basin, NV, USA	0.36–10.5			Jul./Aug. 1979	1–7	16		Particulate S/total S ratio	Eatough et al. (1981)
Navajo, AZ, USA	2.5–11	25–115	2.67-10.92	Jul./Dec. 1979	0-0.8	13		Particulate S/total S ratio	Richards et al. (1981)
Four Corners, NM, USA		2–90	0.3-12.5	Jun. 1978	0.15-0.5	3		Varies with stack distance CN production/ SO <sub>2</sub> ratios	Mamane and Pueschel (1980)
Nanticoke Ont., Canada	0.15-1.93	3-43		Jun. 1978	0-8.7	7	4	Plume age < 2 h with fumigation Particulate S/total S ratio	Anlauf et al. (1982)

262

Location of source	Plume	Stack	Travel time	Month and	Oxidation	No of rate	Average	Rate derivation,	Reference
	age (h)	distance	(h) of	year rate	data (% h <sup>-1</sup> )	points	$(\% h^{-1})$	method comments	
		(km)	sampling						
Nanticoke Ont., Canada	0.07–2.9	2–93		Nov. 1975	0.32-12.6	19		Varies with stack distance Particulate S/total S ratio	Melo (1977)
Oil fired power plants									
Anclote, FL, USA		0.50	0–1.67	Aug. 1976/Feb. 1977			≤ 0.25	Steady state rate	Forrest et al. (1979b)
								Particulate S/total S ratio	
Andrus, MS, USA	1.2-6.6			May/Oct. 1977	0–5.1	9	2.2	Particulate S/total S ratio	Easter et al. (1980)
Northport, NY, USA	0–3.3		0–2	Various, over 3 yr		60	< 1	Rate essentially incalculable Particulate S/total S ratio	Garber et al. (1981)
Metal smelters									
Mt Isa, Qld, Australia	0.08–14.83	2–256		Jun. 1977	0.06-0.45	65	0.25	Diurnally averaged rate Gaseous S/total S ratio	Roberts and Williams (1979)
Mt Isa, Qld, Australia	2.2-42.5	60–1001		Jul. 1979			0.15	Diurnally averaged rate	Williams et al. (1981)

Table 2. (Continued)

Table 2. (Continued)

Location of source	Plume	Stack	Travel time	Month and	Oxidation	No of rate	Average	Rate derivation,	Reference
	age (h)	distance (km)	(h) of sampling	year rate	data (% h <sup>-1</sup> )	points	$(\% h^{-1})$	method comments	
Urban plumes								·····	
St Louis, MO, USA				Aug. 1975	10-14	18		Gaseous S/total S ratio	Alkezweeny and Powell (1977)
Milwaukee, WI, USA			0–3	Aug. 1976/Jul. 1977	1-9		4	Sulphate and light scattering	Miller and Alkezweeny (1980)
St Louis, MO, USA				Jun. 1976	0-4			Measurements	Forrest et al. (1979a)
								Particulate S/total S ratio	
Budapest Hungary		50	~3h	Jul./Aug. 1978	3-31	8	10		Horvath and Bonis (1980)
Long-range transport trajectories									
Sweden		9001900	2361	Summer (Anr-Sen.)	0.3-5.2	12	1.4	Particulate S/gaseous S ratio	Traegaardh (1980)
		1300-2500	27-55	Winter (OctMar.)	0.4-1.3	4	0.8		

One of the first airborne investigations of  $SO_2$  oxidation in the plume of a power station was that of Flyger et al. (1978), who used an  $SF_6$  tracer to monitor dispersion and deposition from the plume emitted from a 122 m high stack. They estimated that half the  $SO_2$  was lost from the plume within 45 km of the source, corresponding to a travel time (and half-life) of about 90 min.

Gillani et al. (1978) studied the gas-to-particle conversion rate of sulphur emitted from a coal fired power station in Kansas. They observed that the ratio of particle phase to total sulphur was related linearly to the total solar radiation dose experienced by the plume. This resulted in the amount of sulphur lost by deposition to the ground surface being about 25% in the first 200 km of travel, comparable to the amount of particulate sulphate formed. The maximum rate of particulate sulphur formation was less than  $3\% h^{-1}$  and only occurred during the daytime. Further analysis of the same data set was carried out by Husar et al. (1978) who concluded that SO<sub>2</sub> oxidation rates were 1-4% h<sup>-1</sup> during the daytime and < 0.5% h<sup>-1</sup> during the night. In a further re-examination of these data, Gillani and Wilson (1980) concluded that the condition of the background airmass which receives the plume, the extent of plume - background air interactions and photochemical processes are the most important factors in determining the SO<sub>2</sub> oxidation rate. This is probably because of the dominant role of O<sub>3</sub>, both directly and as a source of OH. Additionally, the entertainment of non-methane hydrocarbons from polluted background air can provide a source of peroxy radicals HO<sub>2</sub> and RO<sub>2</sub>), allowing replenishment of the O<sub>3</sub> removed by reaction with NO in the plume.

Put together, the Kansas experiment suggests that sulphate aerosol forms relatively rapidly during the daytime when sufficient oxidants (OH, HO<sub>2</sub> and RO<sub>2</sub>), are available in the plume. Initially, close to the point of emission, oxidant depletion occurs rapidly within the plume by consumption of O<sub>3</sub> by emitted NO, thus limiting the concentrations of OH (which is formed by the photolysis of O<sub>3</sub>). If sufficient mixing with background air occurs, O<sub>3</sub> concentrations will recover, either by mixing in of O<sub>3</sub> or of non-methane hydrocarbons, which can in turn form peroxy radicals. These can both contribute to O<sub>3</sub> formation, by rapidly converting NO to NO<sub>2</sub> without consumption of O<sub>3</sub>, and can directly offer a route of oxidation of SO<sub>2</sub>.

Clearly, SO<sub>2</sub> oxidation rates in the bulk plume are likely to be lower than in background air due to oxidant limitation. However, it is possible that at the plume top and edges, where plume dilution is greatest, conversion rates may be significantly enhanced. Zak (1981) observed daytime conversion rates up to 5.5% h<sup>-1</sup> in a plume edge. Similarly, when the plume top is in contact with clouds, fast liquid-phase reactions will enhance the SO<sub>2</sub> oxidation rate, up to 10% h<sup>-1</sup> (Gillani et al., 1981).

Another important consideration is the  $SO_2/NO_x$  ratio. This is a critical parameter in determining sulphate formation rates because  $SO_2$  and  $NO_x$  compete for the same oxidising radicals, and oxidation of NO<sub>2</sub> by OH is much faster  $(\times 10)$  than that of SO<sub>2</sub>. Hence the presence of NO<sub>x</sub> in a plume will inhibit SO<sub>2</sub> oxidation rates (and sulphate formation rates) relative to the rates in background air.

Mamane and Pueschel (1980) used the concentrations of particles in the plume of the Four Corners power station to estimate an SO<sub>2</sub> oxidation rate of about 0.15% h<sup>-1</sup> in the first 0.3 h, increasing to 0.5% h<sup>-1</sup> in the next two hours of travel time, decreasing again to  $\sim 0.3\%$  h<sup>-1</sup>. Outside the Four Corners plume, Davis et al. (1979a, b) estimated SO<sub>2</sub> oxidation rates due to reaction with OH of 0.2% h<sup>-1</sup> in the early morning and 2.3% h<sup>-1</sup> around noon, with an average conversion rate of 0.7% h<sup>-1</sup>.

Dittenhoeffer and De Pena (1978) found that gas-phase photochemical reactions were the dominant sulphate formation mechanisms during the daytime in a power station-plume at Keystone, Pennsylvania, at low relative humidities. However, when the plume merged with a cooling tower plume, liquid-phase oxidation predominated. In a later study of the Keystone plume they found an average SO<sub>2</sub> oxidation rate of about 1% h<sup>-1</sup> in the first 2 h of plume travel, rising to 6% h<sup>-1</sup> when the plume encountered clouds (Dittenhoeffer and De Pena, 1982).

Meagher et al. (1977) used an instrumented aircraft to determine the rate of SO<sub>2</sub> oxidation within the plume of the Cumberland Valley coal-fired power station in Tennessee. Most of the oxidation of SO<sub>2</sub> that was observed appeared to occur in the immediate vicinity of the power plant. Beyond 10 km, an average oxidation rate of 0.2% h<sup>-1</sup> was found. In a later modelling study, Meagher and Luria (1982) simulated the chemistry of a plume from a power station of similar size and location to the Cumberland Valley plant. Hydroxyl was found to be the most important oxidant of SO<sub>2</sub>, except when high background concentrations of hydrocarbons were used, in which case oxidation by HO<sub>2</sub> and RO<sub>2</sub> became significant. Rapid attenuation of oxidation rates were observed, as oxidant limitation became significant, following the removal of O<sub>3</sub> by NO, and plume dilution by incorporation of background air was required before radical chemistry became established. Forrest et al. (1981) found a daytime average conversion rate of  $3\% h^{-1}$  in summer, varying with time of day, and an average of 0.5% h<sup>-1</sup> at night. The Cumberland Valley plant was studied more recently, during the 1995 Southern Oxidant Study, when Gillani et al. (1998a, b) found nitrate formation rates of 10-15% h<sup>-1</sup> and a high differential loss rate of nitrogen species (relative to  $SO_2$ ) of about  $0.12 h^{-1}$ .

Summer and wintertime oxidation rates of SO<sub>2</sub> were obtained in the plume from a northern Alberta power station by Lusis et al. (1978). In February the oxidation rate was found to be low (less than  $0.5\% h^{-1}$ ), increasing to 1–  $3\% h^{-1}$  in June, again suggesting the role played by photochemical processes. Another wintertime study (Liebsch and De Pena, 1982), this time of the Bowen, Georgia, power station plume, found that the highest conversion rate was  $0.2\% h^{-1}$ , except when high relative humidity was observed, when the conversion rate increased to  $2.3\% h^{-1}$ . Meagher and Luria (1981) also observed increased conversion rates, up to  $2.8\% h^{-1}$ , in periods of high relative humidity.

Data obtained from five different coal-fired power stations in the western USA at times favourable to gas-phase photochemical reactions gave SO<sub>2</sub> to SO<sub>4</sub><sup>2-</sup> conversion rates of 0–5.7% h<sup>-1</sup> for travel times of 10–162 min (Hegg and Hobbs, 1980). In a later study carried out in Arizona, they failed to find measurable conversion rates in four flights out of five (Hegg and Hobbs, 1983), while in another study on the plume from the coal-fired Mohave station, an SO<sub>2</sub> to particle conversion rate of 0.6% h<sup>-1</sup> was estimated (Hegg et al., 1985).

Anlauf et al. (1982) found an average summertime  $SO_2$  to  $SO_4^{2-}$  oxidation rate of 4% h<sup>-1</sup> in the plume of the Nanticoke coal-fired power station in Ontario at distances downwind from the stack of 3–43 km at relative humidities of 30–50%. Eatough et al. (1982) studied sulphur chemistry in the plume of the Kennecott copper smelter in Utah and found  $SO_2$  to sulphate conversion rates as high as 6% h<sup>-1</sup> in hot, dry and sunny summer conditions.

Luria et al. (1983) attempted to obtain SO<sub>2</sub> oxidation rates by airborne sampling of the plume from the coal-fired Colbert Steam Plant, Alabama, and by studying stack gases from the plant in a reaction chamber. Quite good agreement was obtained between the two methods of estimation, with an SO<sub>2</sub> to SO<sub>4</sub><sup>2-</sup> oxidation rate of 2.2% h<sup>-1</sup> found on the first day of study. On the second day the power station plume merged and mixed with an urban plume and an enhanced oxidation rate of 4.1% h<sup>-1</sup> was seen, presumably because of enhanced free radical chemistry occurring as a result of the presence of reactive hydrocarbons. This study also provided one of the very few estimates of NO<sub>x</sub> oxidation rates obtained from plume observations and a first-order rate coefficient for NO<sub>x</sub> removal of 27% h<sup>-1</sup> was found.

Cheng et al. (1987) studied the plume from an oil sand extraction plant in Alberta. This contained relatively high aerosol concentrations close to the source, and the aerosol surface was believed to be wet. SO<sub>2</sub> to SO<sub>4</sub><sup>2-</sup> conversion rates of 0–2.8% h<sup>-1</sup> in winter, and 0–6% h<sup>-1</sup> in summer, were found. Heterogeneous processes were believed to be appreciable on the wet aerosol surfaces close to the point of emission.

The heterogeneous oxidation of  $SO_2$  in power station plumes has also been studied in field experiments. Gillani and Wilson (1983) used measurements made under wet conditions from three plumes in Missouri and Tennessee when the power station plumes interacted with clouds and during light rain. Variable oxidation rates were observed, but during light rain the liquid-phase rate was around 8% h<sup>-1</sup>. In a modelling study of plume–cloud interactions, Gillani et

al. (1983) estimated a daytime liquid-phase sulphate formation rate of about  $(12 \pm 6)\% h^{-1}$ .

In one of the few European field studies of plume sulphur chemistry, Clark et al. (1984) followed the chemical composition of cloud water in a power station plume over the North Sea in winter. The plume was trapped in a shallow layer filled with stratocumulus cloud, restricting dilution and allowing total depletion of  $O_3$  in the boundary layer. An SO<sub>2</sub> conversion rate of about  $1\% h^{-1}$  was estimated at 5 h travel time, comparable to an estimated rate of  $4.3\% h^{-1}$  in background air over the same period.

## 3.2. Other plume observations

The occurrence and chemistry of sulphur, and to a lesser extent, nitrogen, compounds has been studied in plumes other than those from coal-fired power stations. Oil-fired stations, metal smelters and urban plumes have all been studied, and have yielded some information relevant to understanding plume chemistry. However, since the chemical composition of emissions from these types of plumes will be different to those from coal-fired power stations, so the dominant routes of oxidation and their rates will be different. For example, the concentrations of trace metals will be different, giving rise to different rates of catalysis (Garber et al., 1981). Newman (1981) observed sulphur oxidation rates five times greater in an oil-fired power station plume than in a coal-fired station plume, but this has not been borne out by more recent work.

Forrest et al. (1979a) studied the Anclote oil-fired power station in Florida and measured an SO<sub>2</sub> oxidation rate of < 0.25% h<sup>-1</sup>. Garber et al. (1981) measured a similarly low rate in a variety of meteorological conditions in the Northport, NY, oil-fired plume. However, Eatough et al. (1981) found no significant differences in SO<sub>2</sub> oxidation rate in an oil-fired plume to that from a coal-fired station. Somewhat higher rates  $(3.1 \pm 0.8\%$  h<sup>-1</sup>) were observed by Eatough (1984) in the plume from a Pacific coast oil-fired power station, with a rate of oxidation of  $30 \pm 4\%$  h<sup>-1</sup> when the plume passed through a fog bank. Enger and Hoegstoem (1979) qualitatively describe a similarly enhanced SO<sub>2</sub> oxidation rate under conditions of very high relative humidity in Sweden.

The rate of conversion of SO<sub>2</sub> to sulphate aerosol particles was determined by a comprehensive measurement programme in the plume emitted from an oil sands extraction plant at Fort McMurray in Alberta (Cheng et al., 1987). A single parcel of air was tracked and sampled by an aircraft and conversion rates of 0-2.8% h<sup>-1</sup> were observed in winter and 0-6% h<sup>-1</sup> in summer. It was suggested that heterogeneous processes were responsible for the oxidation in winter and close to the point of emission when the aerosol particles in the plume were wet. Plumes from metal smelters might be expected to contain relatively high concentrations of trace metals and hence have elevated  $SO_2$  oxidation rates due to catalytic effects. However, Roberts and Williams (1979) found an  $SO_2$  conversion rate of only 0.15% h<sup>-1</sup> in a smelter plume at Mt Isa, Australia, and Eatough et al. (1981, 1982) found similarly low rates.

Urban plumes differ from point source plumes in having relatively higher NO<sub>x</sub> and hydrocarbon concentrations, derived from vehicle exhausts. In general it might be expected that higher oxidation rates of SO<sub>2</sub> and NO<sub>x</sub> will be experienced in an urban plume than in a point source plume, due to the more reactive nature of a hydrocarbon-rich plume (Winchester, 1980; Ellestad, 1980). The St Louis, Missouri, plume was extensively studied in the 1970s. Alkezweeny and Powell (1977) found S(IV) conversion rates of 10-14% h<sup>-1</sup> in the summertime while Zak (1981) estimated a daytime rate of  $8.5 \pm 4\%$  h<sup>-1</sup> and a nighttime rate of  $1.1 \pm 0.5\%$  h<sup>-1</sup>. In a study of the Milwaukee urban plume a rate of 6-8% h<sup>-1</sup> was seen on one day and < 1% h<sup>-1</sup> on the following day, in similar meteorological and precursor conditions (Miller and Alkezweeny, 1980; Alkezweeny et al., 1982). Recently, the urban plumes of Atlanta (e.g. St. John and Chameides, 2000) and Nashville (e.g. Nunnermacker et al., 2000) and other major conurbations have been extensively studied, but with a clear focus on O<sub>3</sub> formation.

#### 3.3. Plume fringe activity

It is quite clear from the above review of sulphur and nitrogen chemistry and of power station plume studies that the oxidation of SO<sub>2</sub> and NO<sub>2</sub> is likely to be rather slower in a power station plume than in ambient air, since the supply of oxidants will quickly become limiting, at least in clear air where homogeneous photochemically driven gas-phase reactions predominate. Primary emissions of NO will soon eliminate O<sub>3</sub> from the plume, so cutting off the production of OH. However, the situation is likely to be somewhat different at the fringes of the plume where the plume mixes with ambient air. Increased chemical reactivity on the fringes of a power station plume was first observed by Davis and Klauber (1975) who saw an increase in the O<sub>3</sub> concentration at the edges of a power station plume, which they erroneously attributed to photochemical reactions involving SO<sub>2</sub>. In fact O<sub>3</sub> formation in the plume fringe is almost certainly due to the photochemical reactions of NO, NO<sub>2</sub> and hydrocarbons, the latter derived largely from the background air, as described by Calvert et al. (1978). Such O<sub>3</sub> enhancements in plume fringes have now been repeatedly observed (e.g. Gillani et al., 1978; Lusis et al., 1978; Miller et al., 1978; Forrest et al., 1979b).

#### 3.4. Model calculations

As well as the experimental studies summarised above, several attempts have been made to estimate sulphur and nitrogen oxidation rates in power station plumes using models of the gas and aerosol phase chemistry believed to be occurring in such plumes. Eltgroth and Hobbs (1979) developed an early model, supported by data, that suggested that homogeneous gas to particle conversion of SO<sub>2</sub> to SO<sub>4</sub><sup>2-</sup> is greatest at the edges of a plume, due to the mixing in of ambient air. Hov and Isaksen (1981) developed a comprehensive plume model where the chemistry and meteorology of the boundary layer interact with a power station plume, which was given spatial resolution in the cross wind direction. The model predicted the formation of O<sub>3</sub> in the plume fringes, with chemical activity enhanced in the fringes, but becoming more pronounced towards the centreline of the plume with time. SO<sub>2</sub> to SO<sub>4</sub><sup>2-</sup> oxidation rates varied (1–5% h<sup>-1</sup>), with nitric acid formation proceeding more rapidly. Depletion of NO and NO<sub>2</sub> occurred very rapidly, with about 80% of the NO<sub>x</sub> being converted to HNO<sub>3</sub> and NO<sub>3</sub> within three hours.

Seigneur (1982) modelled sulphate aerosol formation in power station plumes, using a gas and aerosol phase chemistry scheme and a particle growth model. Rather slow SO<sub>2</sub> oxidation rates were predicted: 0.5% h<sup>-1</sup> by homogeneous processes. Importantly, the rate was found to be sensitive to the background hydrocarbon and NO<sub>x</sub> concentrations, as well as to humidity and to the photolysis rate of NO<sub>2</sub>. A similar dependence on the background hydrocarbon and NO<sub>x</sub> concentrations was found in the plume chemistry model of Meagher and Luria (1982). SO<sub>2</sub> oxidation rates of 1–2% h<sup>-1</sup> were predicted during the spring and summer, reducing in winter.

Joos and Mendonca (1986) integrated a chemistry model with a comprehensive model of secondary aerosol formation processes, with validation of the output using observational data from a plume study. The sulphate formation rate was found to be: very sensitive to relative humidity (increasing with relative humidity); sensitive to temperature only at high relative humidities, where SO<sub>2</sub> solubility decreases as the temperature increases; very sensitive to solar intensity; and not very sensitive to background O<sub>3</sub> concentration. The formation rate of nitrate aerosol in the plume was found to be: very sensitive to temperature, because the HNO<sub>3</sub>/NH<sub>3</sub>/NH<sub>4</sub>NO<sub>3</sub> equilibrium is temperature dependent; not very sensitive to relative humidity, although model limitations may make this conclusion invalid; very sensitive to solar irradiation; and slightly more sensitive to the background ozone concentration than is the SO<sub>2</sub> oxidation rate. The relative insensitivity of this model to background O<sub>3</sub> is important since it implies that the OH radical concentrations in the plume depend more upon NO<sub>x</sub>/reactive hydrocarbon photochemical reactions in the plume than on the amount of O<sub>3</sub> mixed into the plume. In addition, the model showed that the

net contribution of the plume to sulphate aerosol concentrations was always significant, but that the plume contribution to nitrate aerosol was only significant when there was a relatively low background  $NO_x$  concentration and a reactive hydrocarbon/ $NO_x$  ratio greater than 10.

Recently, a reactive plume model incorporating transport, chemistry and aerosol dynamics has been used by Karamchandani and Seigneur (1999) to simulate sulphate and nitrate chemistry in power station plumes. They made simulations for winter and summer emissions with travel times of 8 and 10 h, respectively, and with different start times. NO<sub>x</sub> and SO<sub>2</sub> emission rates were held constant at 88 and 161 ton d<sup>-1</sup> respectively. The effects of changes in the chemical composition of the background air were investigated by varying ambient O<sub>3</sub>, hydrocarbon and PAN concentrations, the hydrolysis rate of N<sub>2</sub>O<sub>5</sub> and the horizontal and vertical dispersion coefficients.

The model results very largely confirmed the many earlier predictions of plume chemistry: oxidation rates in the plume are lower than in background air; excess nitrate concentrations in the plume were 4–7 times greater than the excess sulphate concentrations (i.e.  $NO_x$  removal was 4–7 times greater than  $SO_2$  removal in the same travel time); conversion of  $NO_x$  and  $SO_2$  was at a maximum in the daytime in summer and at a minimum during the night and in winter;  $NO_x$  conversion proceeded at night in clear air by the hydrolysis of  $N_2O_5$  whereas  $SO_2$  conversion did not; and in the presence of clouds  $SO_2$  is rapidly oxidised during both the day and night. Background  $O_3$ , reactive hydrocarbon and PAN concentrations had significant effects on the  $SO_2$  and  $NO_x$  conversion rates.

Duncan et al. (1995) demonstrated the possible use of emission inventories coupled with chemistry and transport modelling as a tool for apportionment of the sources of  $NO_x$  and  $SO_2$  measured at particular locations. Since the sulphur content of gasoline differs from that of coal and of heavy fuel oil, plumes from mobile and point sources should be identifiable by their characteristic  $SO_2$  to  $NO_x$  ratios. However, since these ratios will vary over time, due to the different oxidation rates of these species in the atmosphere, and will vary with ambient conditions, as one or other of the multitude of possible  $NO_x$  and/or SO<sub>2</sub> oxidation routes becomes dominant, this is not a trivial task. In this study, these changes over time were ignored and an average  $SO_2/NO_x$  ratio of 0.05 was used for mobile sources and 2.67-4.56 for power station plumes. This was justified on the grounds that the study was confined to a relatively small area with plume travel times of 3-10h at maximum. They concluded that the four major power stations in the study area accounted for about 15% of the ambient  $NO_x$  at the surface measurement sites on average, but that in the short term this value was extremely variable, due to the intermittent nature of plume fumigation.

#### 3.5. Summary of plume chemistry

As can be seen from the foregoing review of  $SO_2$  and  $NO_x$  chemistry, the field observations of concentration changes in plumes and the theoretical modelling studies, there is now significant convergence in our understanding and prediction of processes affecting the removal of  $SO_2$  and  $NO_x$  and the formation of sulfate and nitrate in power station plumes. This understanding can be summarised as:

- (a) In non-cloudy conditions, SO<sub>2</sub> removal in power station plumes occurs primarily during the daytime by reaction with the OH radical, whereas NO<sub>x</sub> removal occurs both during the daytime, by fast reaction with OH, and at nighttime by the NO<sub>3</sub>/N<sub>2</sub>O<sub>5</sub> pathway.
- (b) In non-cloudy conditions, NO<sub>x</sub> removal will occur much more rapidly ( $\sim$ 10 times faster) than SO<sub>2</sub> removal.
- (c) In cloudy conditions,  $SO_2$  will be removed rapidly by reactions in the aqueous phase, but  $NO_x$  will not.
- (d) The dry deposition velocity of SO<sub>2</sub> is greater than that of NO<sub>x</sub> leading to more rapid removal of SO<sub>2</sub> by this process. Conversely, nitrate aerosol is likely to be removed more rapidly by dry deposition than is sulphate aerosol.
- (e) These differences in removal rates will cause changes in the ratios of S and N concentrations with time of travel from the point of emission. In clear air, as the plume travels downwind, the  $SO_2/NO_x$  ratio will increase. Conversely, the ratio of sulphate aerosol to nitrate aerosol concentration will decrease downwind. In cloudy conditions, where aqueous-phase reactions become important and photochemical processes become less important,  $SO_2$  oxidation will proceed faster than  $NO_x$  oxidation and hence the  $SO_2/NO_x$  ratio may decrease.
- (f)  $SO_2$  and  $NO_x$  removal rates will normally be lower in a plume than in background air, due to oxidant limitations, in both the gas and aerosol phases, with plume fringes offering an intermediate oxidation environment.
- (g) Absolute oxidation rates of SO<sub>2</sub> and NO<sub>x</sub> will vary with plume and background air composition and ambient conditions. In sunny conditions a maximum SO<sub>2</sub> conversion rate of around  $3\% h^{-1}$  and a maximum NO<sub>x</sub> conversion rate of around  $30\% h^{-1}$  might be expected. However, lower rates may be expected in a "normal" power station plume as oxidant supply becomes diminished by consumption of O<sub>3</sub>, although the rate of oxidation of NO<sub>x</sub> will remain ~10 times that of SO<sub>2</sub> in photochemically active conditions.

Unfortunately, however, there do remain significant restrictions in our ability to translate these points into a complete description of  $SO_2$  and  $NO_x$  behaviour in a power station plume. These arise because of the lack of field data of  $NO_x$  oxidation rates inside discrete plumes, a poor understanding of the effects of oxidant limitation on  $NO_x$  oxidation and a poor understanding of the rapidity with which oxidant limitation can be reversed once a plume encounters polluted urban air or mixes with background air. Despite these limitations, it is clear that ground level  $SO_2/NO_x$  ratios may vary with travel time and ambient conditions. In conditions of simple meteorology and plume dynamics, with clear air and adequate sunlight, the photochemical removal of  $NO_x$ will proceed up to 10 times faster than that of  $SO_2$ . At night,  $SO_2$  conversion will be effectively zero in clear air while  $NO_x$  conversion proceeds. In cloudy conditions the opposite effect will pertain, as the  $SO_2$  conversion rate will be increased, but the  $NO_x$  conversion rate will be reduced. Whether or not the resultant ratio changes are observable in the ground-level concentrations of the plume will depend upon the travel time, the ambient conditions and on the nature and magnitude of other sources of  $SO_2$  and  $NO_x$ .

#### 3.6. Source apportionment using ratios of S/N

The discussion above of the atmospheric chemistry of  $SO_2$  and  $NO_x$  clearly suggests that when elevated concentrations of these pollutants are observed at ground level as a result of emissions from multiple sources, the unambiguous identification of these sources, from consideration of the ratios of their concentrations, is not straightforward. Indeed, such unambiguous source apportionment is not likely without use of a sophisticated chemical and transport model of the atmosphere and then only under ideal conditions. However, in an idealised dry atmosphere with simple photochemistry occurring and in the absence of other sources of the pollutants, an observable increase in the  $SO_2/NO_x$ ratio in a power station plume as it travels downwind may be expected. In fact, such elevated ratios of  $SO_2/NO_x$  measured downwind could be taken as evidence that power station emissions were responsible for the elevated concentrations of SO<sub>2</sub>. However, if other sources of pollutants are present then this idealised pattern of changing ratios could be distorted. In particular, vehicular or other sources of NO<sub>x</sub> could substantially reduce the SO<sub>2</sub>/NO<sub>x</sub> ratio below that expected for a power station plume. Thus high SO<sub>2</sub>/NO<sub>x</sub> ratios (>  $\sim$ 5) are almost certainly indicative of pollution from major combustion processes, but low SO<sub>2</sub>/NO<sub>x</sub> ratios ( $<\sim$ 5) do not unambiguously rule out power stations as being the source of the  $SO_2$ . In wet weather, when liquid phase chemical conversion processes will occur, the situation is much more complex. In both wet and dry conditions it is necessary to correct for background concentrations of the pollutants before consideration of the ratios.

#### 4. Conclusions

Pollution by the products of fossil fuel combustion remains a major environmental issue, with ecological, health and material damage effects well documented. As well as the direct effects of  $SO_2$  and  $NO_x$  and their indirect effects on acid deposition and visibility reduction, consideration is now being given to the role of power plant plumes to  $O_3$  formation. Current understanding of the chemistries of  $SO_2$  and  $NO_x$  in plumes is sufficiently advanced to allow the broad description and prediction of their behaviour under ideal or near-ideal conditions. However, the effects of oxidant limitation and of more complicated atmospheric conditions cause major problems to the prediction of plume behaviour in the ambient atmosphere. Chemical models of plume behaviour require integration with models of the physical dispersion and transport of the plume if a full description of concentration changes is to be effected. The need for large-scale integrated field experiments for the validation of chemistry-transport models remains.

#### Acknowledgements

This work was funded by TXU Europe Power.

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