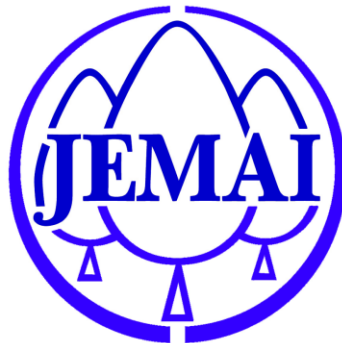


For Environmental Seminar in EiMAS

Introduction of air pollution control



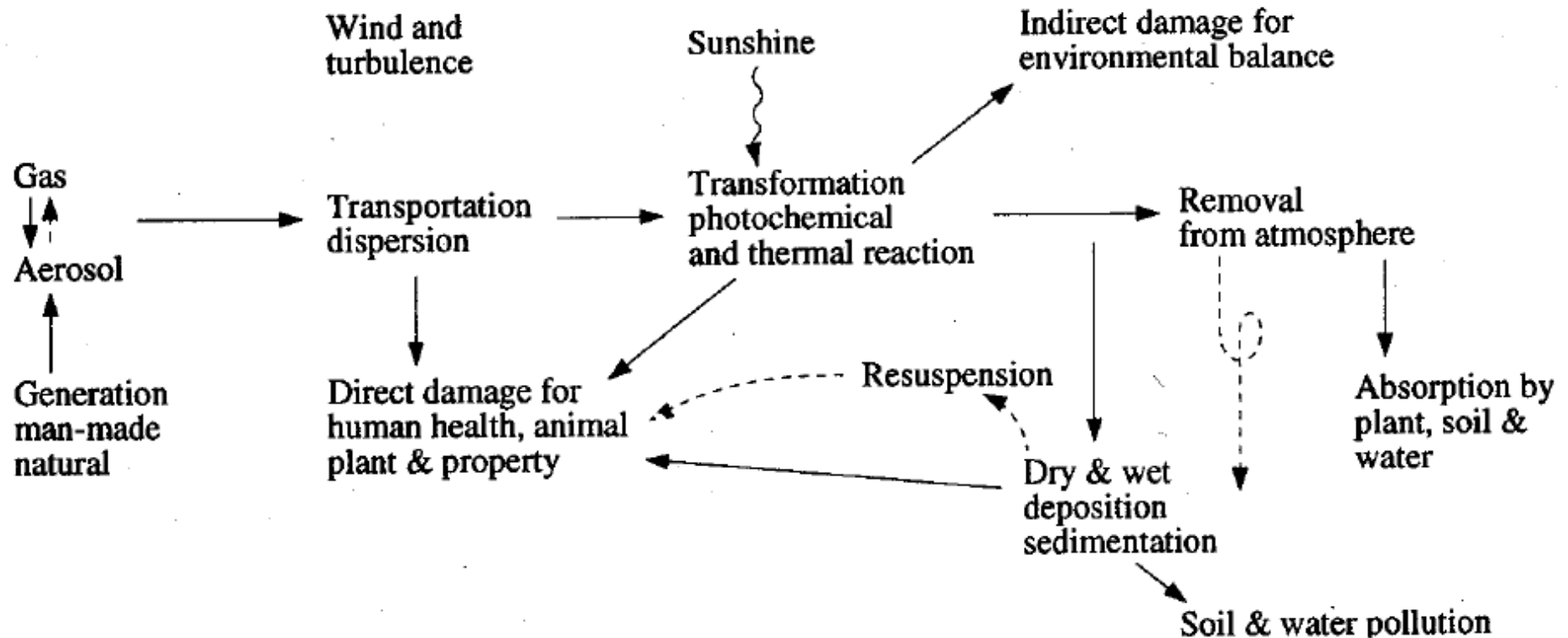
March 10, 2011

**Japan Environmental Management Association for Industry
(JEMAI)**

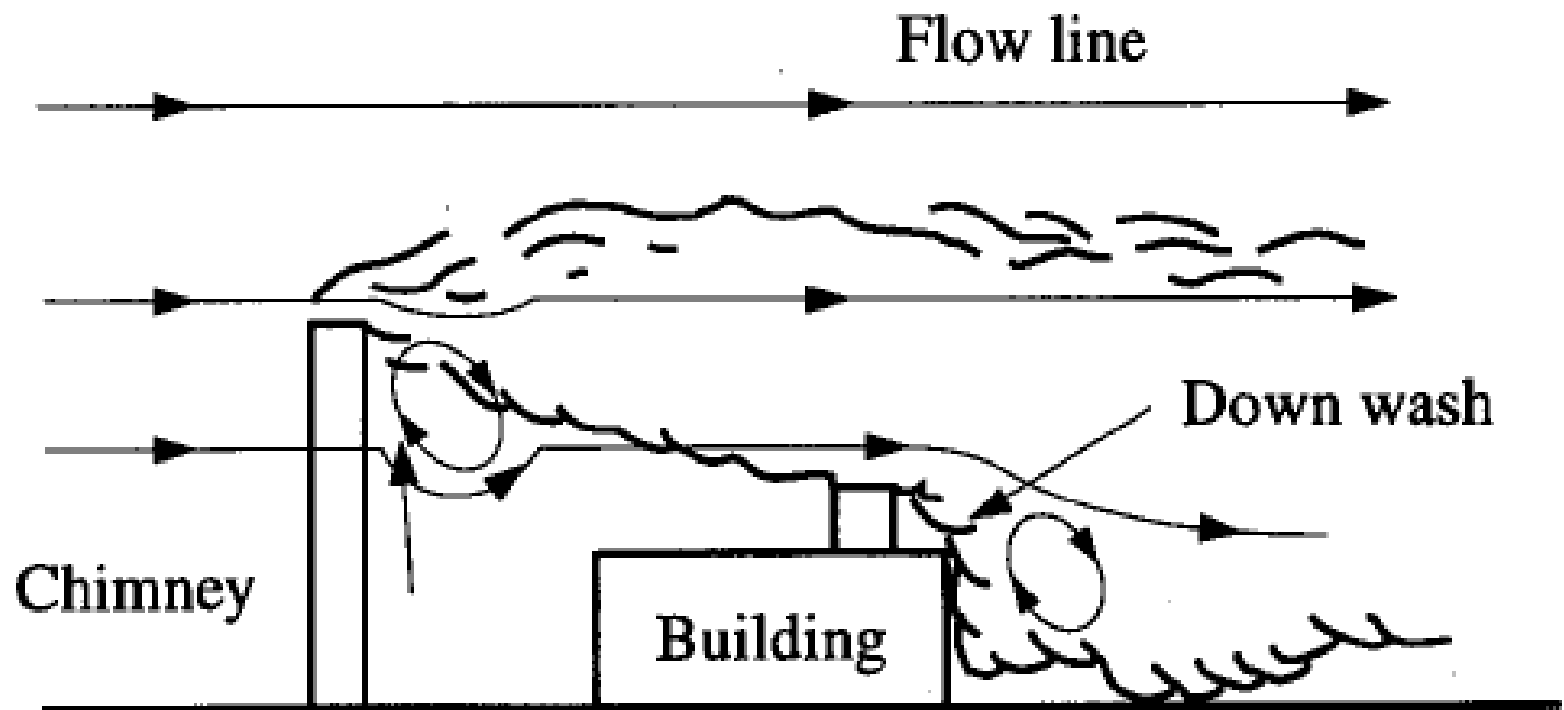
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Life cycle of air pollutants



Down wash of smoke behind stuck and building



Theory of air mass movement

- Air mass moves adiabatic up/down.
 - up: adiabatic expansion → temp. down
 - down: adiabatic compression → temp. up

$$\frac{dT}{dz} = -\gamma_d$$

Dry adiabatic rate γ_d : $0.98^\circ\text{C}/100\text{m}$

(constant in lower atmosphere)

$\gamma > \gamma_d$ (γ : actual atmospheric temp. inclination)

Temp. of air mass upped becomes higher than ambient air and accelerates its speed.

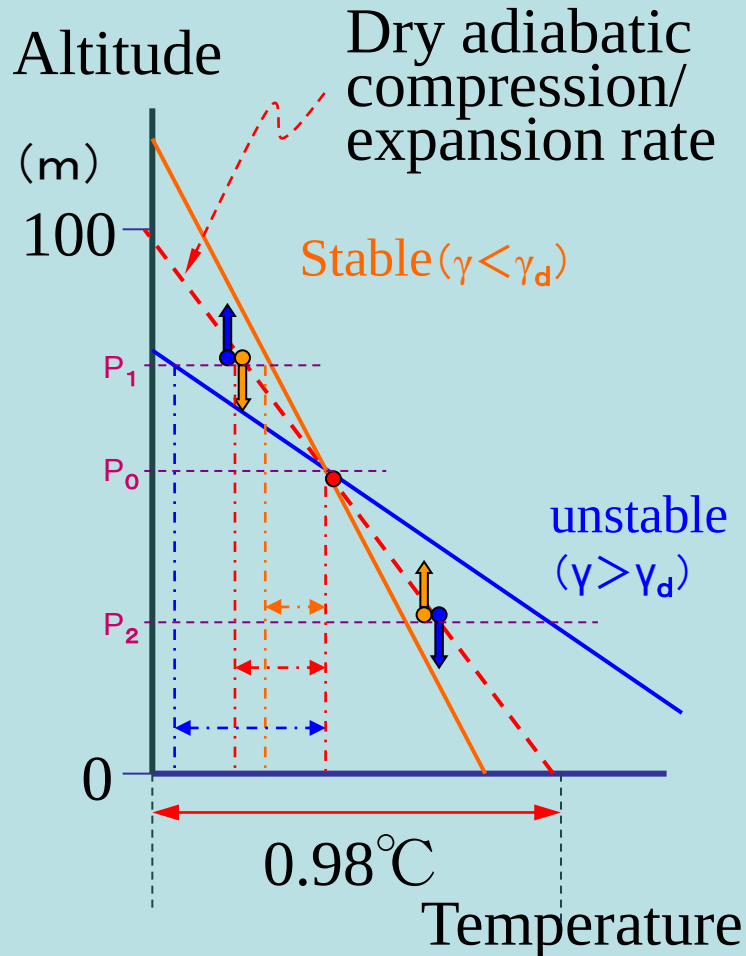
→ unstable by heat

$\gamma < \gamma_d$

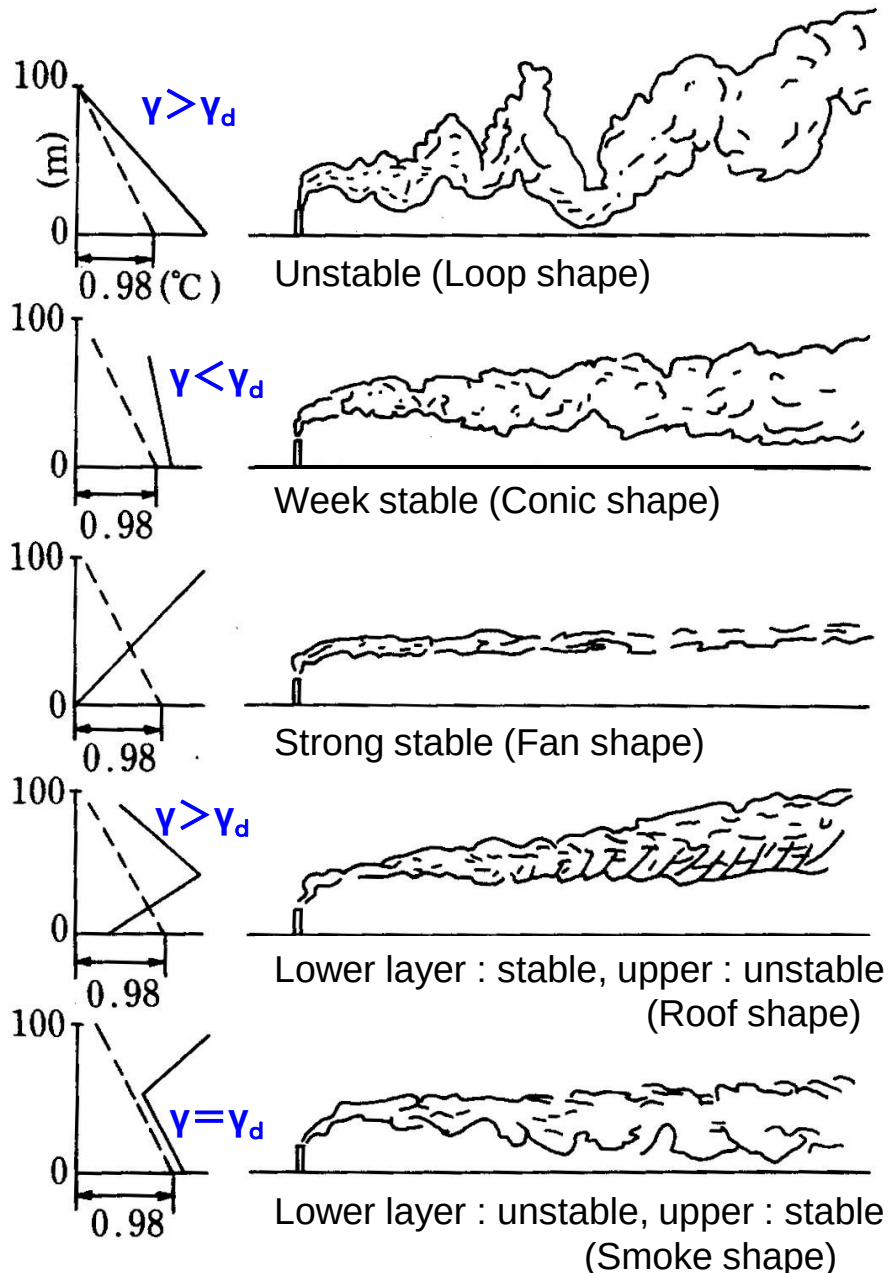
Temp. of air mass upped becomes lower than ambient air and restrains its speed.

→ stable by heat

$\gamma = \gamma_d$ → neutral by heat
(adiabatic distribution)



Typical types of smoke plumes and their corresponding temperature profiles



Loop shape: All layer is unstable.

Smoke moves widely up and down. High conc. of smoke appears momentary near emission point. Fine daytime

Conic shape: All layer is neutral or weak stable

Smoke diffuses same speed vertically and horizontally. Maximum conc. point appears farther than loop shape.

Fan shape: All layer is strong stable (reverse temp.)

Smoke can not move vertically. Smoke only diffuses horizontally like a fan. Fine nighttime and morning.

Roof shape: Lower layer is stable and upper is unstable

Inclination of temp. changes in reverse. Smoke diffuses upper side of reverse layer. One reason of Smog.

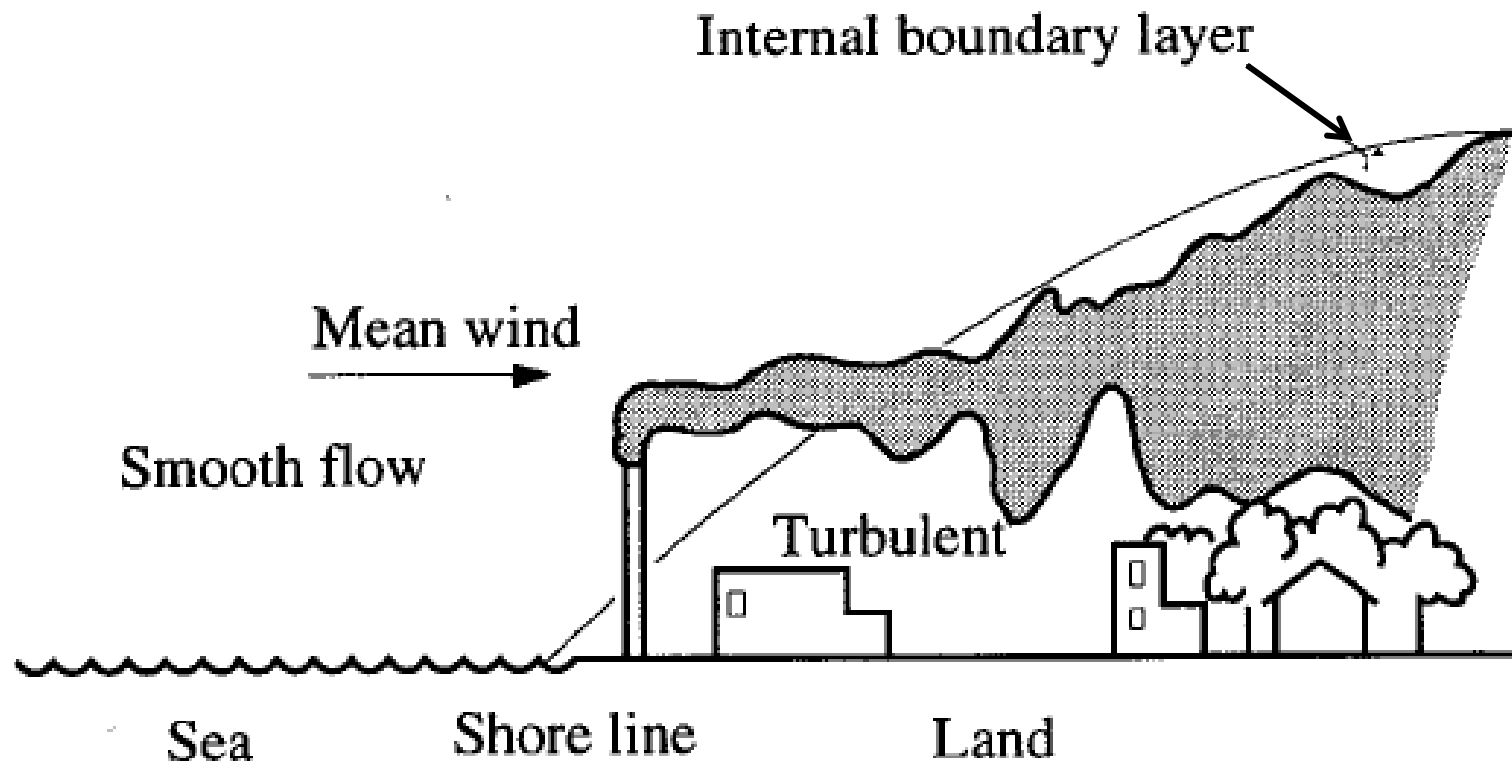
Smoke shape: Lower layer is stable and upper is unstable

Because lower layer is unstable, smoke circulate only in a lower layer. (Fumigation)

Cause of formation and characteristics of surface inversion layer

Name	Cause and characteristics
Geographical inversion of temperature	When air current moves over mountains, because of foehn phenomenon warm air stands over cold air. Basin and/or valley.
Front inversion of temperature.	Because of moving of front cold air exists under warm air. Air pollution becomes serious in case of a stationary front.
Subsidence inversion of temperature	In region of anticyclone, air subsidence causes temp. rise and deep inversion layer is formed during day and night. Photochemical smog appears.
Radiation inversion of temperature	On calm clear night, ground surface is cooled by radiation loss and then strong inversion layer is formed. Smoke from surface is trapped in this layer.
Advection inverse of temperature	This inversion is formed when warm air flows over cold surface. Fog is frequently associated with this type of inversion.

Internal boundary layer formed over land near the sea shore and smoke plume diffusing in the layer



Past Air Pollution in Japan

(Smog : Primary particle)



1966年(神奈川県環境農政部提供)

1966



2001年(川崎市港湾局提供)

2001

Air Pollution Caused by VOC

(Fume : Secondary Particle)

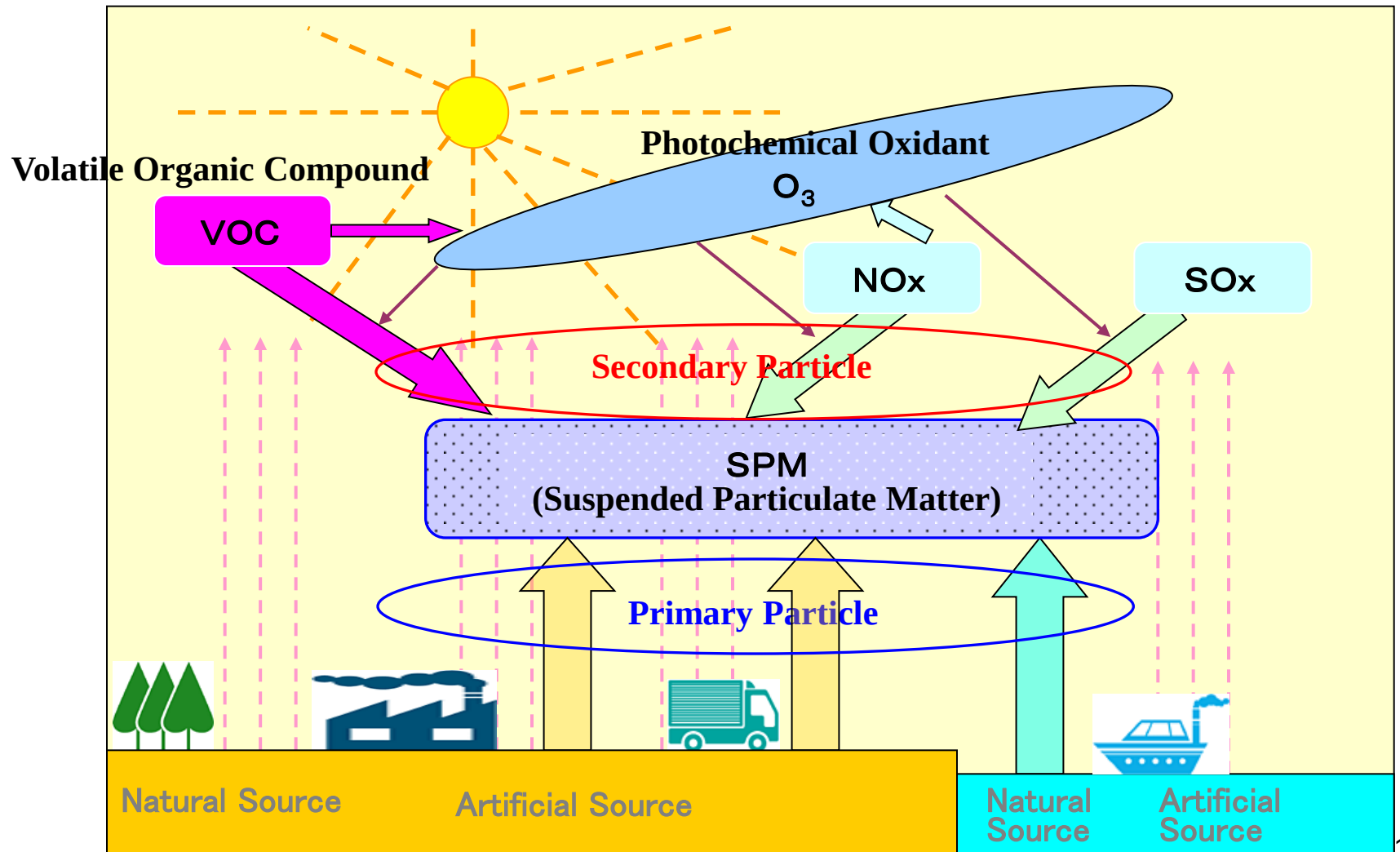


September 3, 2003



September 4, 2003

Reaction of VOC in the Atmosphere



Frequency of appearance of various smoke specks on leaves according to the kind of gas pollutant

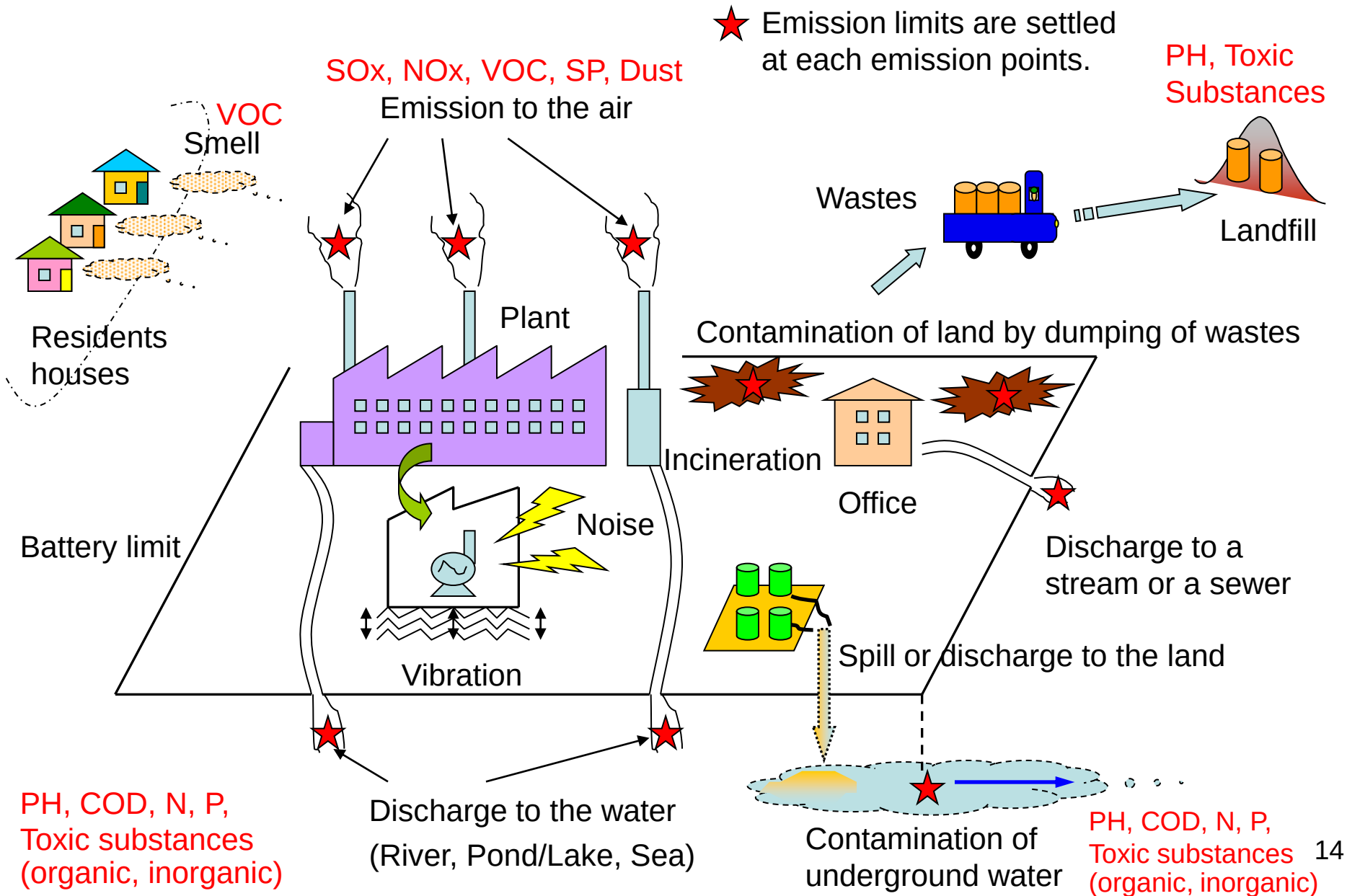
	Smoke specks on the leaf periphery and apex.	Inter-vein smoke specks	Point like speck on the whole leaf	Point like specks on the leaf periphery and the apex.	Etiolation on the whole leaf	Etiolation on the leaf apex and at the periphery
						
SO ₂	?	≡	+	?	++	+
H ₂ SO ₄ mist	+	+	++	+	+	?
Cl ₂	≡	++	+	++	+	++
HCl	++			++		+
HF	≡	?	?	?	+	++
O ₃		++	≡	+	++	?
PAN		++				
NO ₂	+	≡	++			

(Note) Damage frequency : ≡ Very frequently ++ Frequently + Occasional ? Seldom 12

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Environmental Aspects caused by Production Activities



Examples

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Characteristics of fuels

Fuel \ Factors	Sulfur content (%)	Specific gravity kg/m ³	Calorific power kcal/l	Exhaust gas Nm ³ /l
A heavy oil	0.69	0.84	9390	11.4
B heavy oil	1.82	0.91	9540	12.1
C heavy oil	1.91	0.93	9690	12.2
Light oil	0.40	0.83	9130	11.5
Kerosene	0.004	0.79	8690	10.9
LNG*	0.001	0.71	10498	16.2
Coal**	0.817	1.53	6149	9.1
Firewood**	0.092	0.80	3832	11.4

* /Nm³

** /kg

(JEA⁽²⁾, MITI⁽³⁾)

Examples of Facilities accompanying Fume, Smoke and Dust Emission

Facility	Kinds of emission
Boiler	Cinders, fly ash, fume and smoke
Cement kiln	Clinker dust, dust
Ore calcinating furnace	Metal oxides, fly ash, mineral powder, fume, dust
Blast furnace	Mineral powder, coke powder, slag dust, dust
Ferroalloy furnace	SiO ₂ dust, dust
Steel manufacturing open-hearth furnace	Ferrous oxide, dust
Ceramic furnace	Fly ash, dust
Steel converter	Dust
Cement kiln	Dust
Cupola	Dust
Coke oven	Powder, dust
Metal silicon furnace	SiO ₂ dust
Carbon black furnace	Dust
Wastes incinerators	Dust, fly ash
Coal carbonization furnace	Tar mist
Sulfuric acid plant	Sulfuric acid mist
Zinc plating	Zinc oxide, ammonium fume
Mineral pulverization, screening, powder disposal transportation equipment	Dust, powder dust
Street paving material disposal furnace	Dust, SiO ₂ dust, tar mist

Major Artificial Sources of Pollutants

Substance	Emission source facilities, etc.
SO _x	Various types of boilers, chemical plants, diesel cars, vessels, coal heating, etc.
NO _x	Various types of combustion facilities, chemical plants, furnaces, automobiles, vessels, aircrafts, home heating, etc.
Suspended particulate (SP) Total suspended particulate (TSP)	Various types of boilers, furnaces, various manufacturing devices accompanying dust generation, automobiles, vessels, aircrafts, civil engineering, stock yard of coal
Hydrocarbons (HC) VOC	Petrochemical plant, oil-storage tank, painting and coating, automobiles, vessels, aircrafts, etc.
HCl, Cl ₂	Garbage incinerators, HCl manufacturing
HF	Manufacturing facilities of aluminum, glass, phosphate fertilizer, phosphoric acid, fluoric resins, etc.
CO	Automobiles
Offensive odor	Live-stock raising, food processing, paper and pulpmill, fertilizers, refuse disposal, leather manufacturing, chemical industry

Specific Substances and Related Industries (1/2)

Name of substance	Chemical formula	Related industries
Hydrogen fluoride	HF	Fertilizer industry, ceramic industry, aluminum industry
Hydrogen sulfide	H ₂ S	Petroleum refinery, gas industry, ammonia industry, pulp mill
Selenium dioxide	SeO ₂	Metal refinery, chemical industry
Hydrogen chloride	HCl	Soda industry, plastic process
Nitrogen dioxide	NO ₂	Nitric acid manufacture, various industries accompanying combustion
Sulfur dioxide	SO ₂	Sulfuric acid production, industries using heavy oil as fuel, metal industry, pulp mill
Chlorine	Cl ₂	Soda industry, other chemical industries
Silicon fluoride	SiF ₄ , Si ₂ F ₆	Fertilizer industry
Phosgene	COCl ₂	Dyeing industry, organic synthesis
Carbon disulfide	CS ₂	Carbon disulfide manufacture, solvent, plant fumigation
Hydrogen cyanide	HCN	Hydrocyanic acid manufacture, iron manufacture, gas industry, chemical industry, electroplating
Ammonia	NH ₃	Fertilizer, plating, organic, inorganic drugs, blue print
Phosphorus trichloride	PCl ₃	Drug manufacture, phosphorus dichloride
Phosphorus pentachloride	PCl ₅	Phosphorus trichloride, phosphorus oxide
Yellow phosphorus	P ₄	Phosphorus refinery, phosphorus compound manufacture

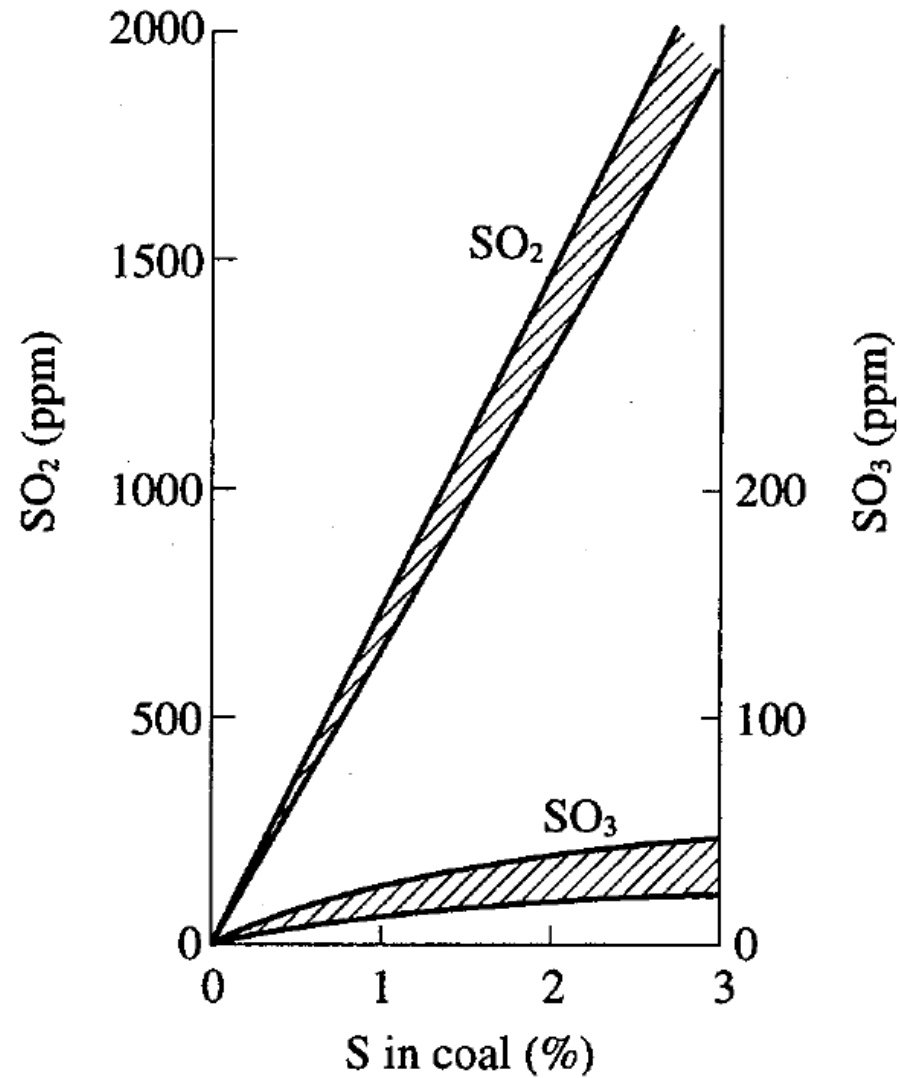
Specific Substances and Related Industries (2/2)

Name of substance	Chemical formula	Related industries
Chlorosulfonic acid	HSO_3Cl	Drug manufacture, dyestuffs manufacture
Formaldehyde	HCHO	Formalin manufacture, leather, synthetic resin
Acrolein	$\text{CH}_2=\text{CHCHO}$	Acrylic acid manufacture, synthetic resin, varnish manufacture
Hydrogen phosphide	PH_3	Phosphoric acid manufacture, phosphoric acid fertilizer manufacture
Benzene	C_6H_6	Petroleum refinery, formalin manufacture, painting industry, organic solvent
Methanol	CH_3OH	Methanol manufacture, formalin manufacture, painting industry, resin industry
Nickel carbonyl	$\text{Ni}(\text{CO})_4$	Petrochemistry, nickel refinery
Sulfuric acid (contains SO_3)	H_2SO_4	Sulfuric acid manufacture, fertilizer industry, inorganic chemistry
Bromine	Br_2	Dyes, medicine, agricultural chemicals
Carbon monoxide	CO	Gas industry, metal refinery, internal combustion
Phenol	$\text{C}_6\text{H}_5\text{OH}$	Tar industry, chemical drug, painting industry, resin industry
Pyridine	$\text{C}_5\text{H}_5\text{N}$	Pharmaceutical, chemical industry, etc.
Mercaptan	$\text{C}_m\text{H}_n\text{SH}$	Petroleum, petrochemistry, pharmaceutical, feed manufacture

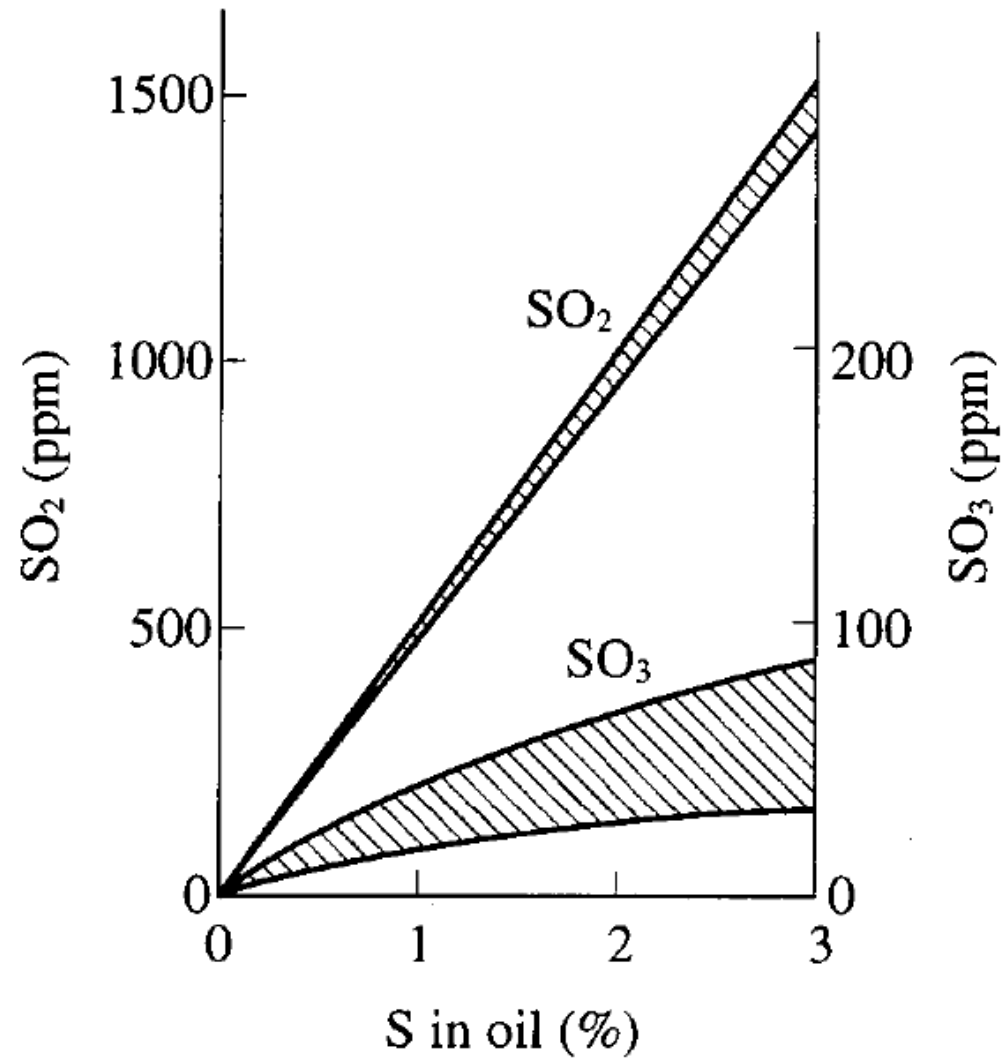
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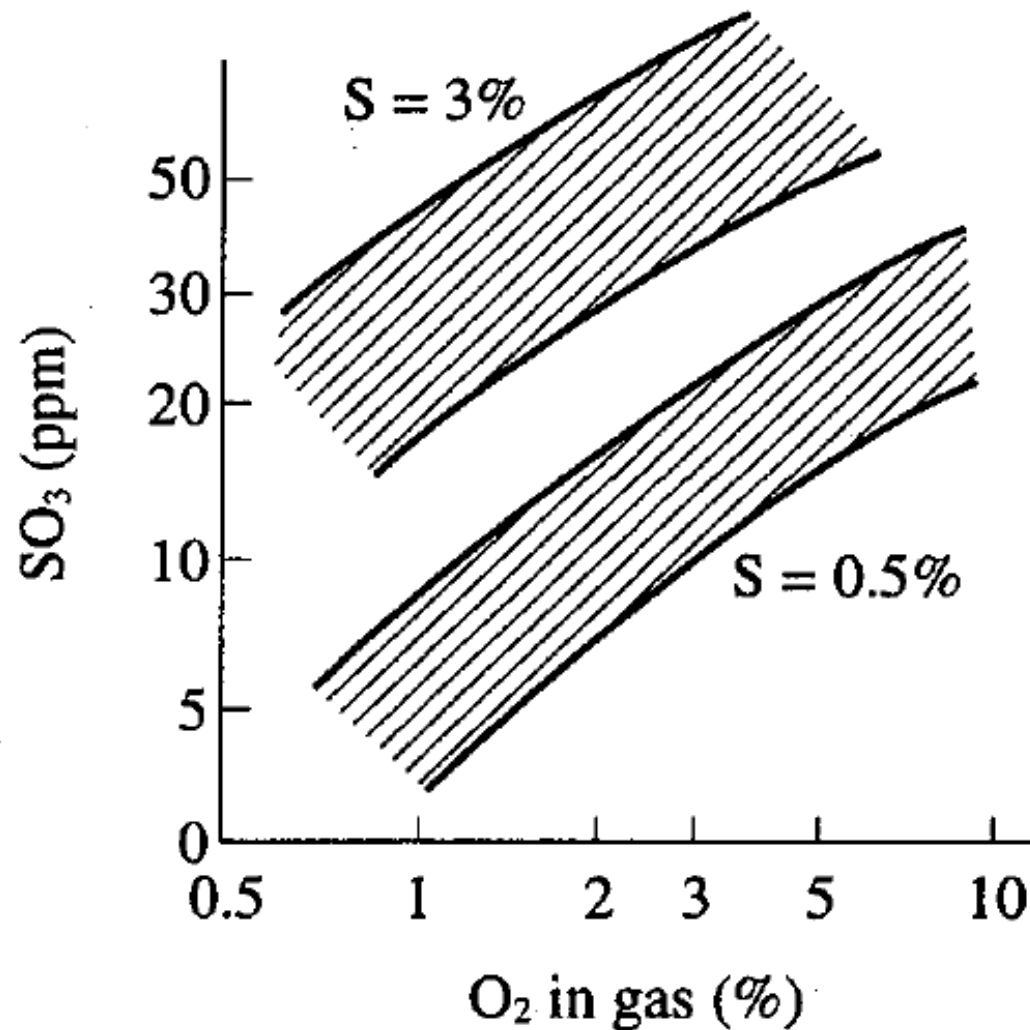
Sulfur content in coal and SO_x in combustion gas



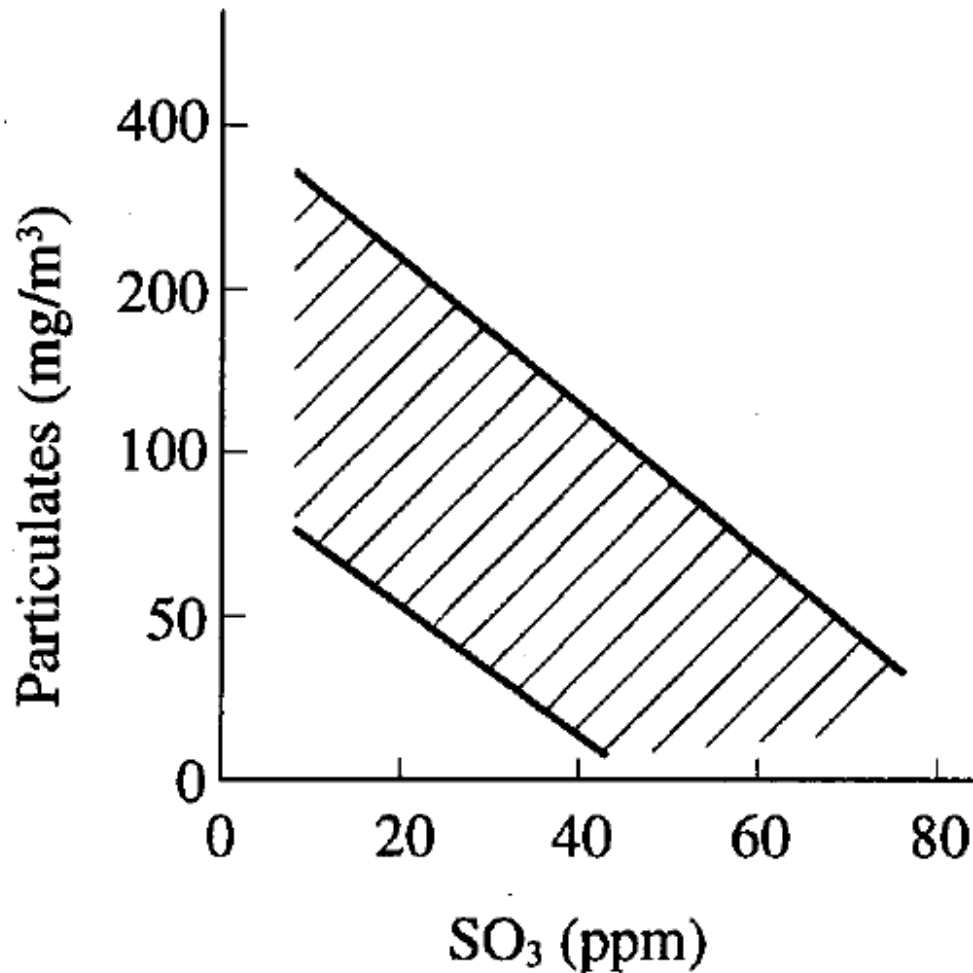
Sulfur content in heavy oil and SO_x in combustion gas



Oxygen and SO_3 in heavy oil combustion gas

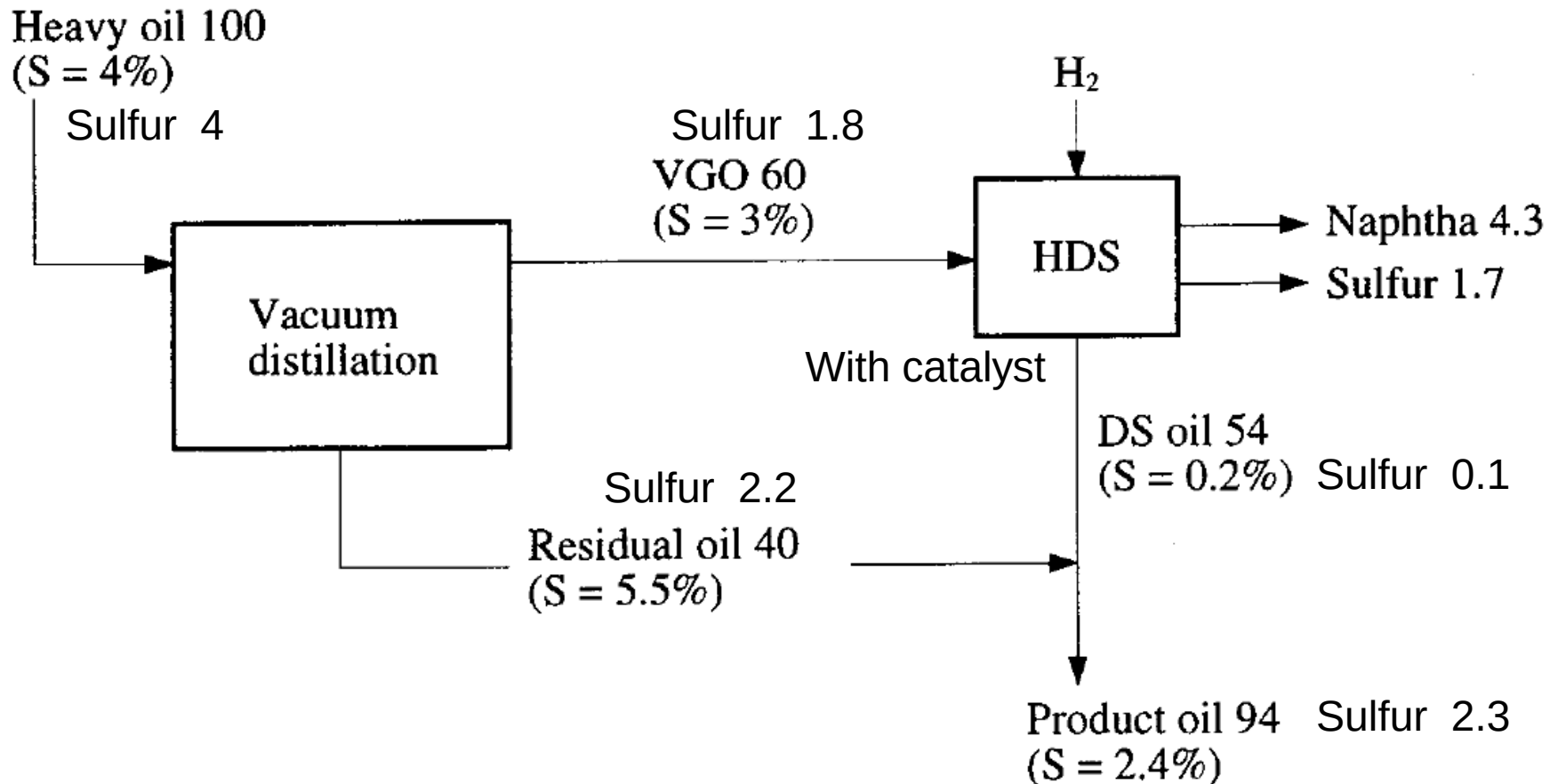


Particulates and SO₃ in combustion gas of heavy oil (S=2-3%)

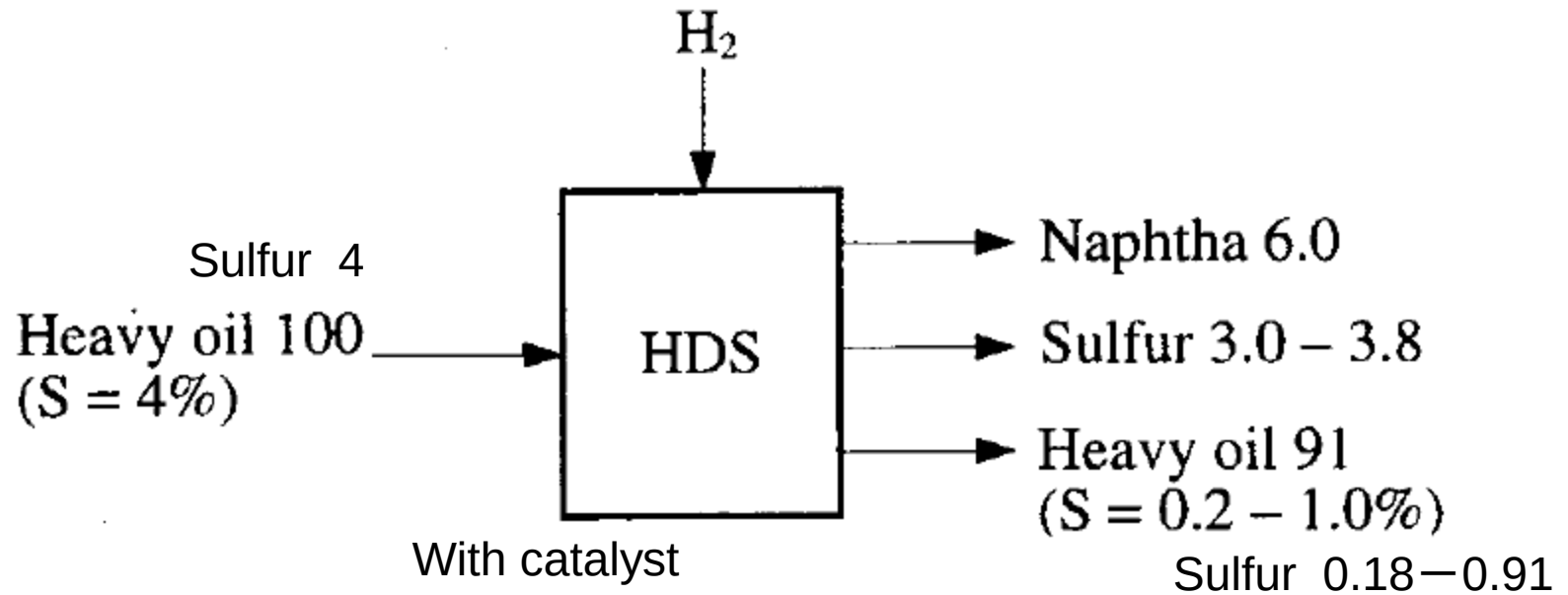


Sulfur removal from fuels

(a) Vacuum gas oil (VGO) hydrodesulfurization (HDS) process

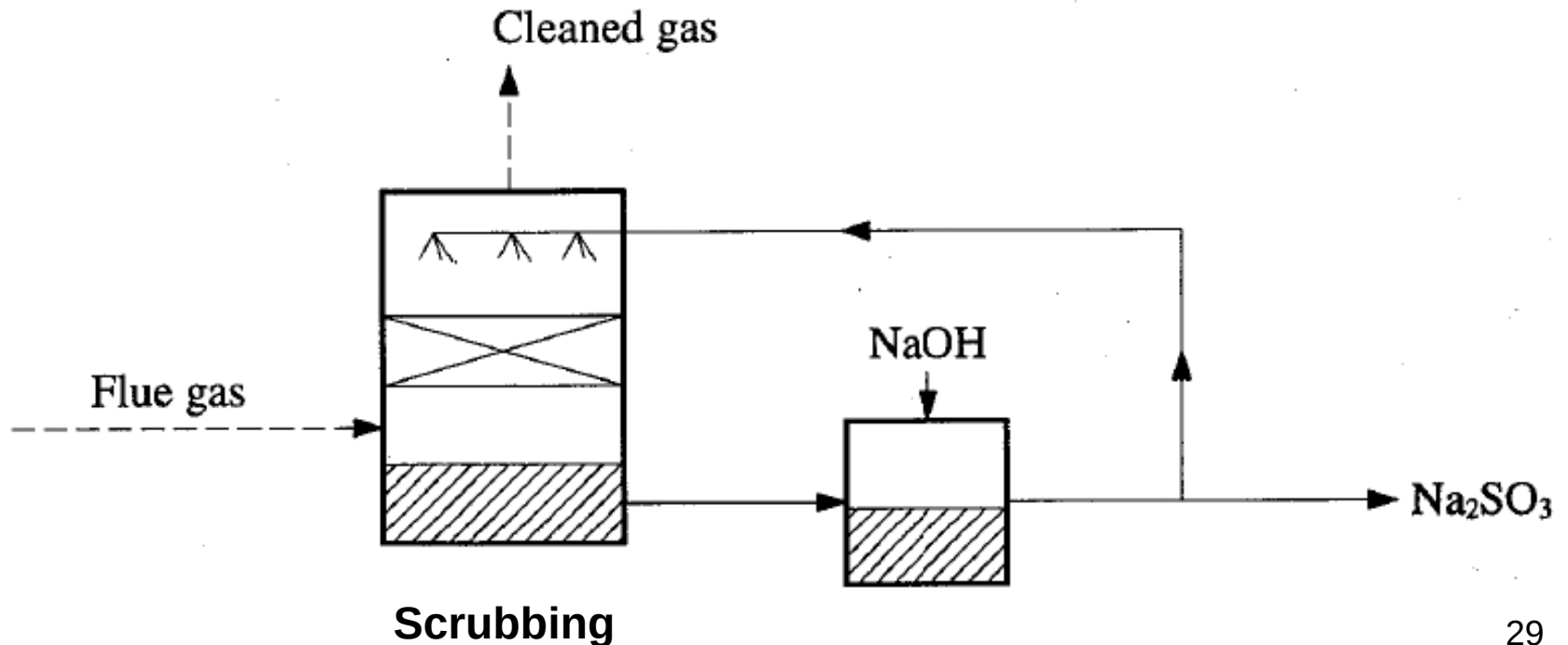
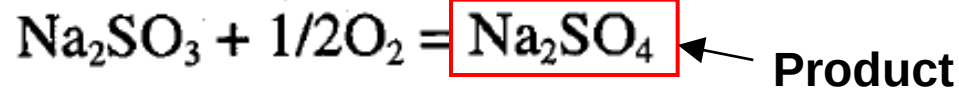
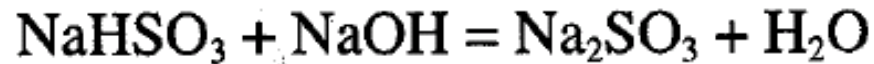


(b) Direct HDS process



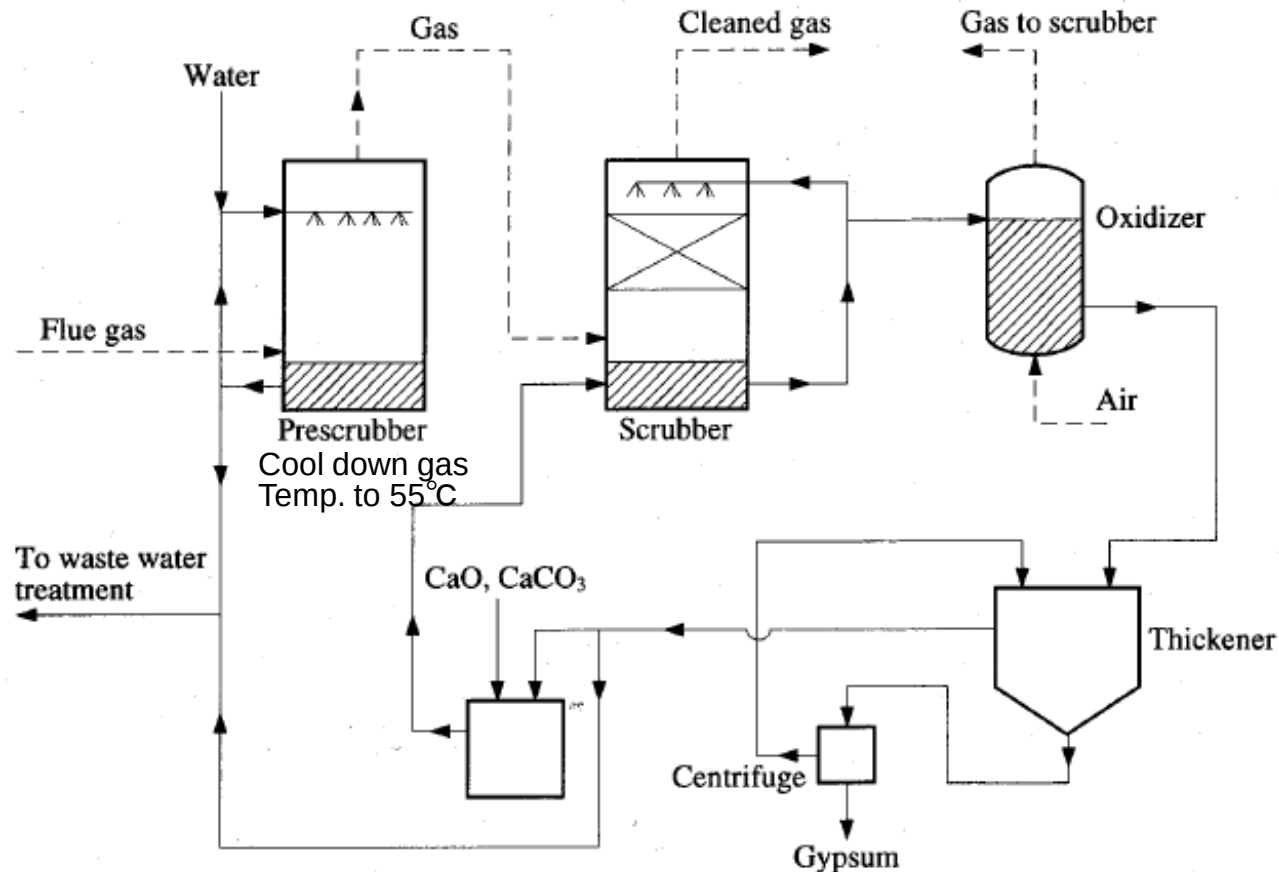
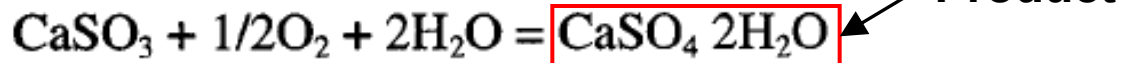
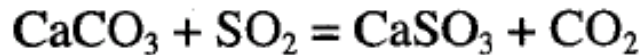
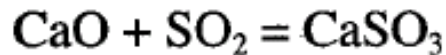
Desulfurization Process

Sodium sulfite recovery process



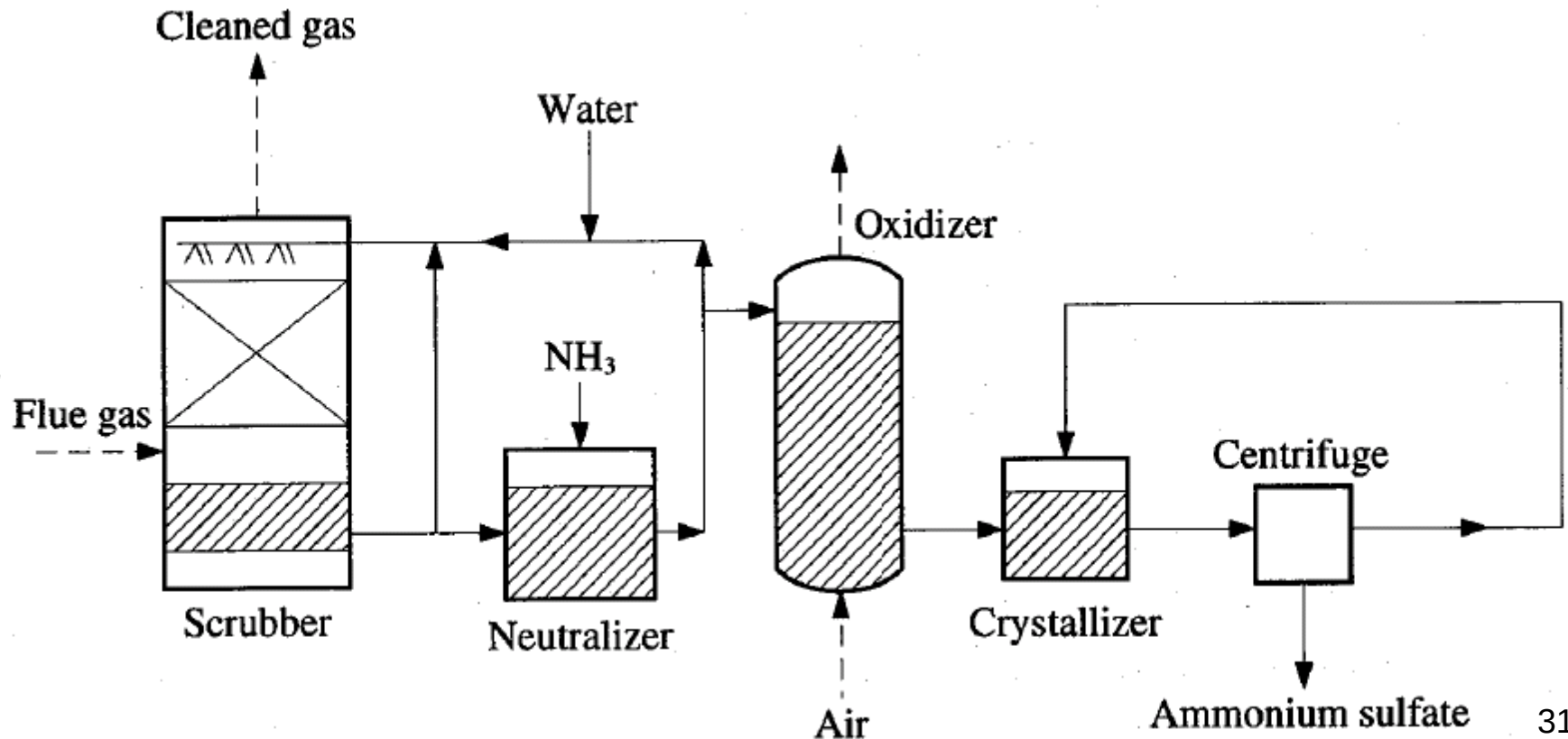
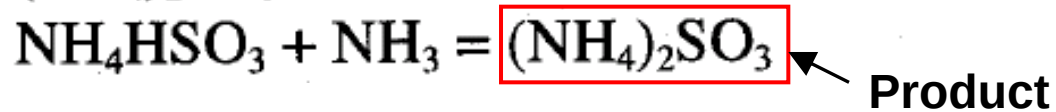
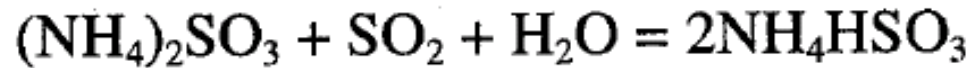
Desulfurization Process

Flowsheet of lime/limestone-gypsum process (with prescrubber for high purity gypsum production)

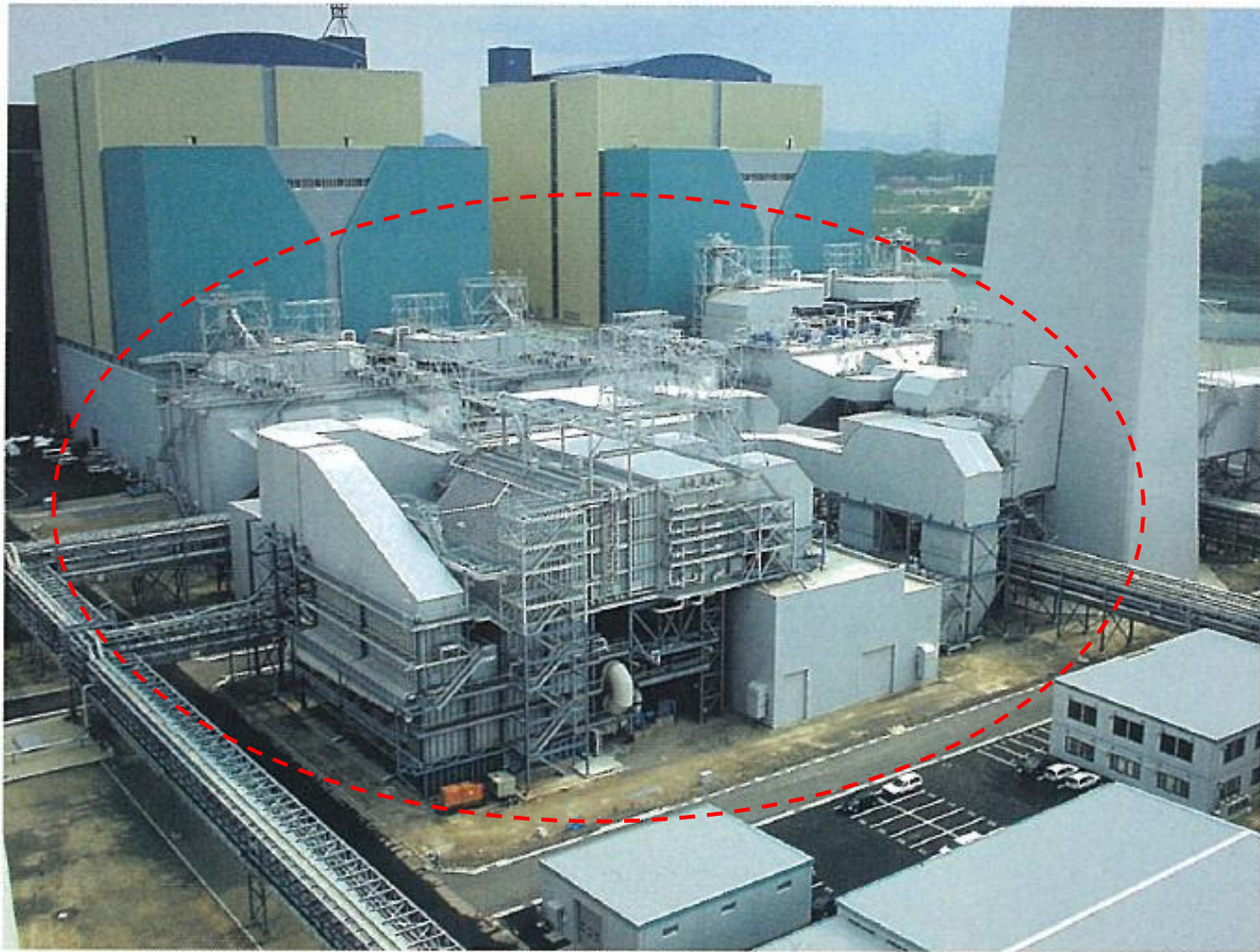


Desulfurization Process

Ammonia scrubbing for ammonium sulfate production



Desulfurization Equipment



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Emission coefficient of NO_x from kinds of fuels

Town gas	0.5 - 1.6 kg/10 ³ m ³
LPG	1.3 - 2.0 kg/ton
Kerosene	1.3 - 2.0 kg/kl
Heavy oil	2.5 - 4.0 kg/kl

Emission coefficient of NO_x from facilities

Unit: NO₂ converted kg/10⁸kcal

Fuel Facilities	C heavy oil	B heavy oil	A heavy oil	Kerosene	Light oil	LNG	Coal
Power generation boiler	58.29	57.89	32.21	26.71	13.91	23.31	75.43
Industrial boiler	40.96	41.72	23.21	19.25	10.02	16.38	53.01
Diesel power generation	752.9	711.1	398.9	318.2	410.2	-	-
Gas turbine	160.5	151.6	85.0	67.8	87.4	75.3	-
Gas generating furnace	50.32	47.53	26.66	21.26	27.41	23.61	64.33
Iron ore pellet incinerator	46.28	43.71	24.52	19.56	25.21	21.72	-
Coke oven	273.0	257.8	144.6	115.4	148.7	128.1	349.0
Air-heating stove for blast furnace	77.36	79.82	43.83	35.87	46.30	30.74	-
Petroleum heating furnace (iso)	42.86	44.22	24.28	19.87	25.65	17.14	-
Brick burning furnace (series)	213.5	201.7	113.1	90.24	116.3	100.2	273.0
Cement firing furnace (dry system)	119.6	112.9	63.35	50.53	65.15	56.11	-
Ceramics firing furnace (series)	95.12	89.84	50.39	40.20	51.82	44.63	121.6
Glass melting furnace (series)	256.5	242.3	135.9	108.4	139.8	120.4	327.9

(JEA⁽²⁾, MITI⁽³⁾)

SOx and NOx emission coefficient from cars

Kinds of cars*	SOx emission coefficient g/No. of car·km	NOx emission coefficient g/No. of car·km
Passenger car	0.032	1.255
Light passenger car	0.021	0.267
General truck	1.214	5.454
Small truck	0.042	2.427
Light truck	0.034	0.524
Bus	0.502	6.158

* Average of Japanese cars. (JEA⁽²⁾)

Engine load ratio by ship operating mode (JEA⁽²⁾)

Unit: %

Engine Mode	Diesel	Turbine
Full	85	100
Standby full	52	65
Half	10.6	20.5
Slow	5.3	15
Dead slow	3.6	13

Empirical formula of exhaust coefficient for ships (JEA⁽²⁾)

Diesel engine using heavy oil A

Quantity y	Power x	Formula
1 NO _x (Nm ³ /h)	x (ps/h)	$y = 1835x^{1.125} \times 10^{-3}$
2 Fuel consumption (kg/h)	x (ps/h)	$y = 0.15x + 25.24$
3 Exhaust (Nm ³ /h)	x (ps/h)	$y = 5.05x + 490.96^{37}$

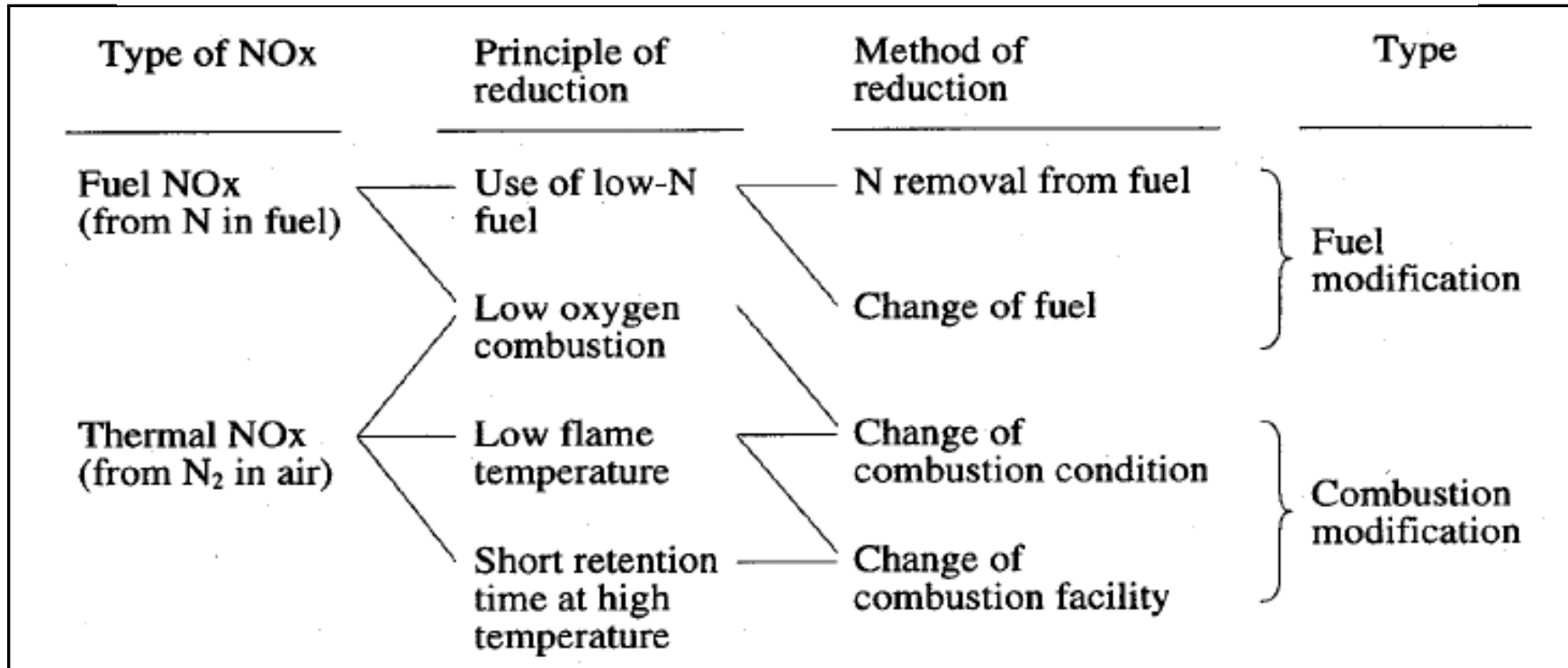
Emission amount of NO_x from an airplane engine

Unit: Nm³/s

Airplane type Mode	DC-8	B-747	B-737	NAMC-YS-11
Idle	0.211	0.827	0.061 to 0.085	0.028 to 0.034
Approach	2.441	6.506	0.630 to 0.805	0.200 to 0.201
Climb	9.403	52.589	—	—
Take off	14.382	94.063	3.100 to 3.5	0.552

Note: The number in the table is amount from an engine, so that total amount of NO_x from an airplane is obtained by multiplying numbers of engine.

Principles and methods of NOx reduction



NOx Concentration in Combustion Gas (ppm)

	Gas N = 0%	Oil N = 0.1 - 0.5%	Coal N = 1 - 3%
Without CM	200 - 300	300 - 500	500 - 1000
With CM	50 - 100	80 - 200	200 - 400

(CM : combustion modification)

The great majority of NOx comes from combustion of fossil fuels, and almost all of it is in the form of NO at the time of occurrence. Some part of NOx generated by combustion is called fuel NOx results from the reaction of nitrogen in the air at a high temperature, and is therefore called thermal NOx.

Investment cost for combustion modification

Control technique	Cost (yen/Nm ³ /hr)
LNB + TSC + FGR	657
LNB + FGR	491
TSC + FGR	475
LNB + TSC	480
TSC	292
LNB	129
OSC	26
Mean	467

* Including change of burner tip.

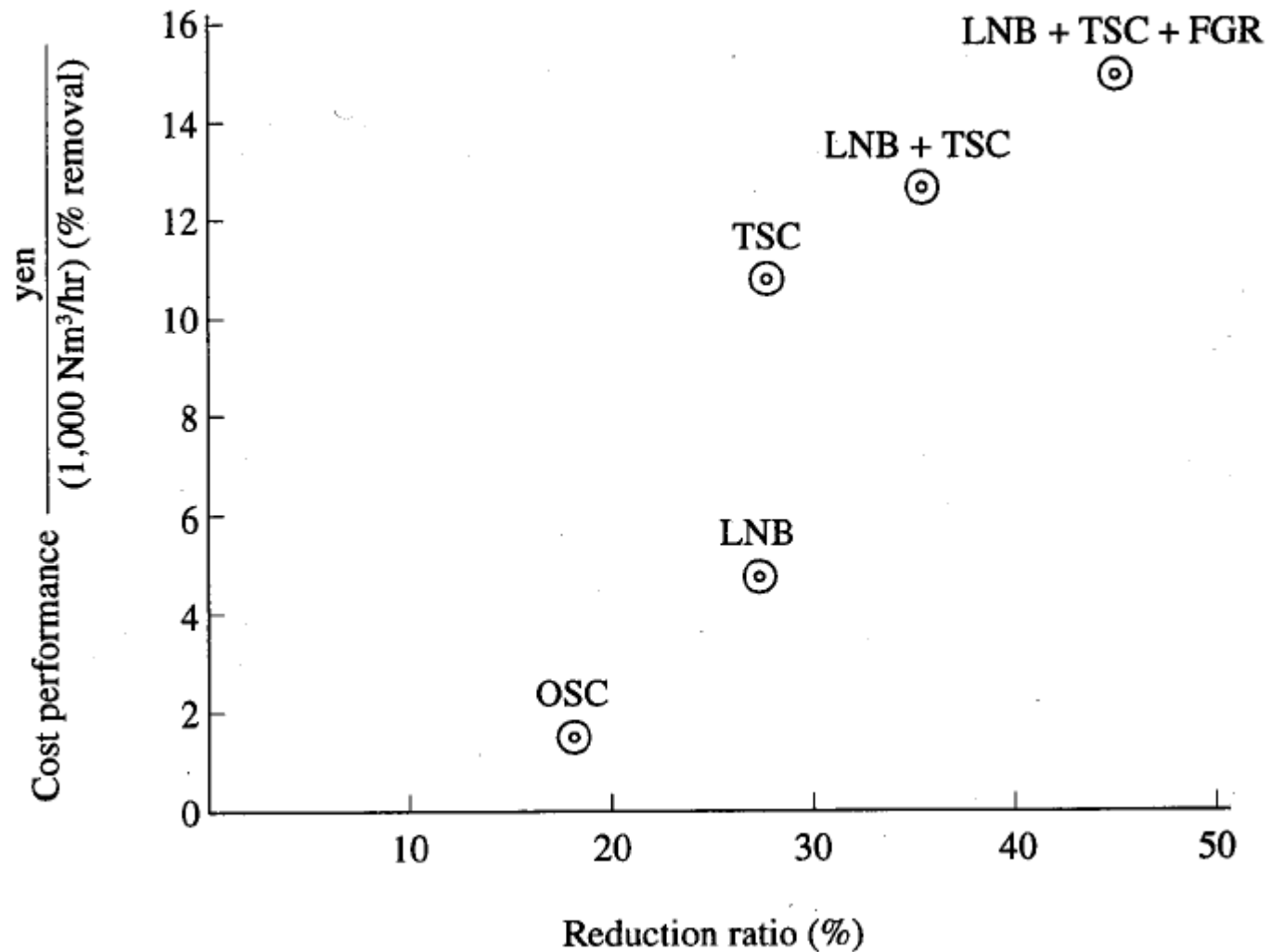
LNB : low NO_x burner

TSC : two-stage combustion

FGR : flue gas recirculation

OSC : off-stoichiometric combustion

Cost performance of NOx control techniques applied to boilers



NOx reduction method

Removal of NOx

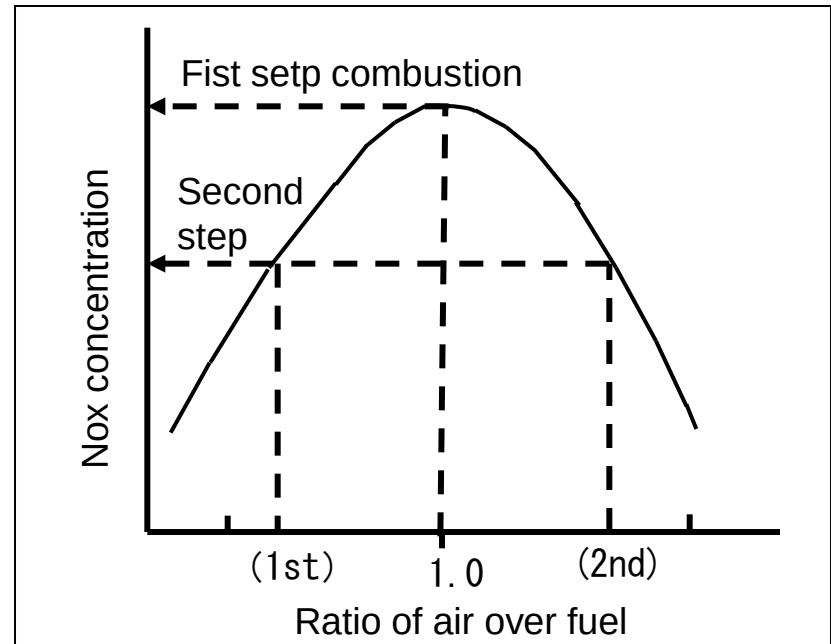
Basics of NOx reduction

- Change low N containing fuel
(Heavy oil → light oil, LNG)
- Low O₂ combustion
- Low temperature combustion
(→ control ratio of air and fuel)
- to shorten combustion time at high temperature

Denitrization — Ammonia

catalytic denitrization method

- Temp. 300~400°C (decompose to N₂&H₂O)
 $4\text{NO} + 4\text{NH}_3 + \text{O}_2 \rightarrow 4\text{N}_2 + 6\text{H}_2\text{O}$
 $6\text{NO}_2 + 8\text{NH}_3 \rightarrow 7\text{N}_2 + 12\text{H}_2\text{O}$
- Composition of catalyst : vanadium , Tungsten, Molybdenum oxide, Titanium oxide
- Shape of catalyst: sand, Honeycomb , plate
- Shape of catalyst : high efficiency, no byproduct, easy operation, no waste water

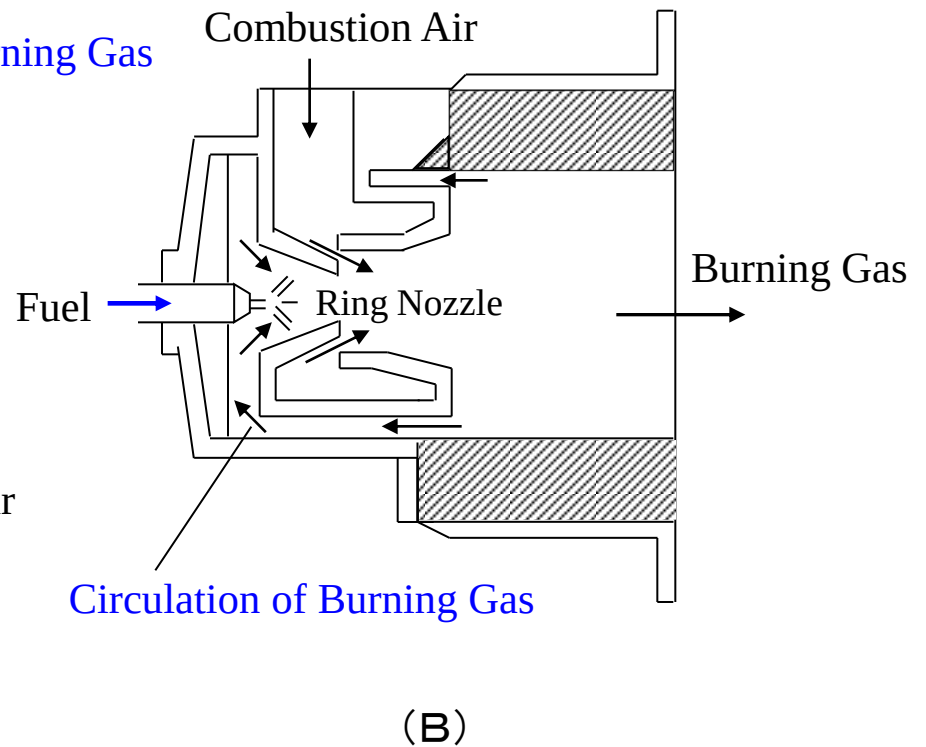
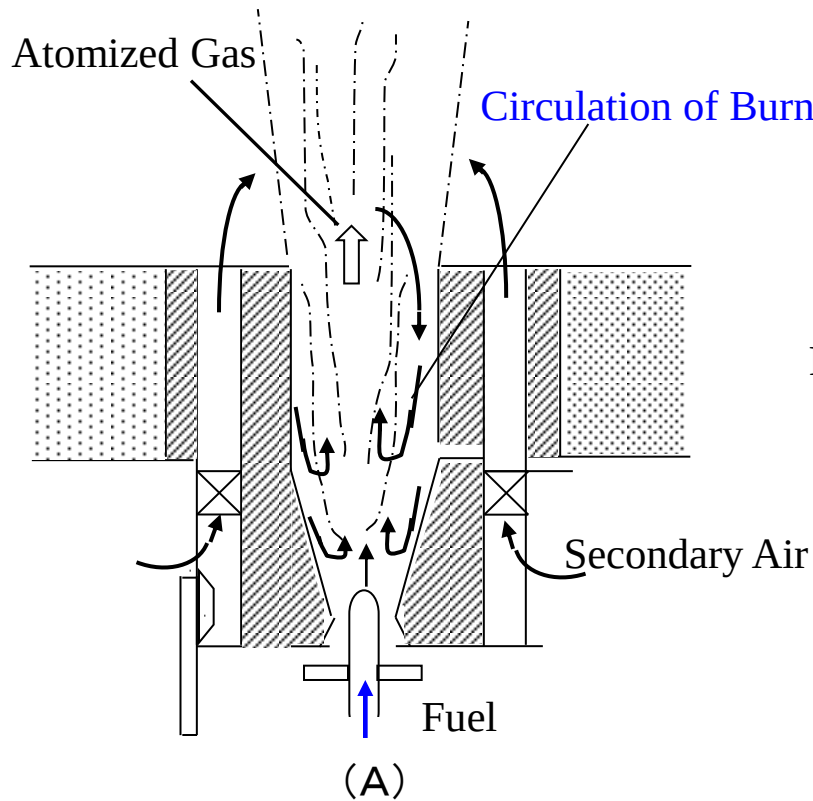


Relationship between ratio of air over fuel and conc. of NOx

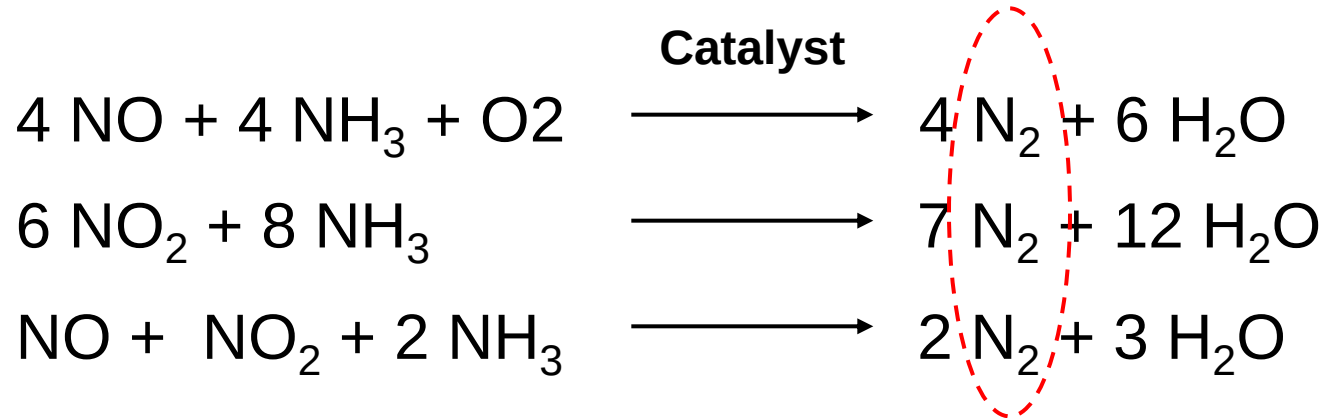
<Theory of second step combustion>

- Ratio of air over fuel < 1 → lack of O₂
→ to reduce Nox generation
- Ratio of air over fuel > 1 → Supply of much excess of air → to reduce Nox generation

Examples of Self-Recycling Low NO_x Burner



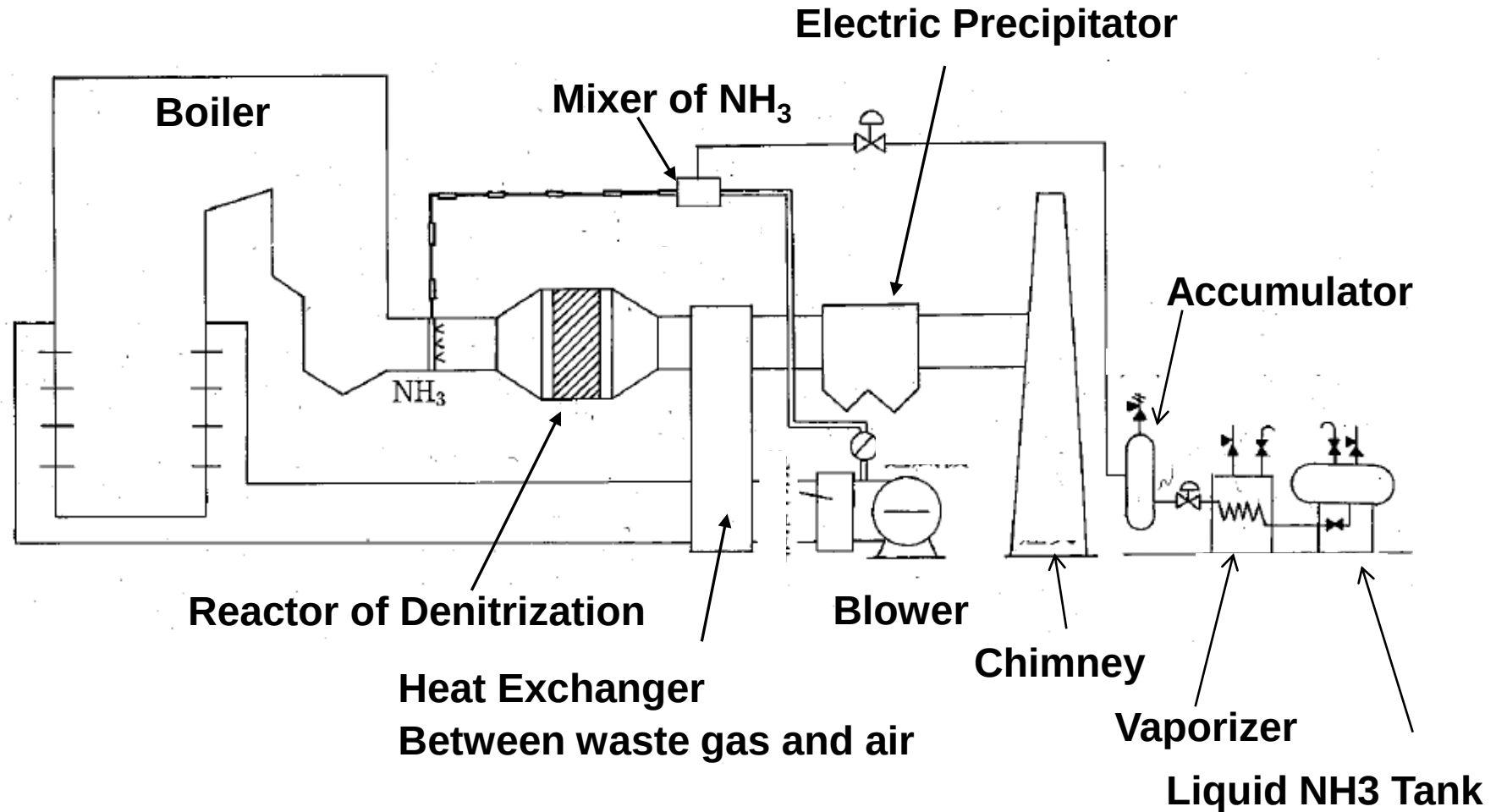
Denitrization of selective contacted reduction



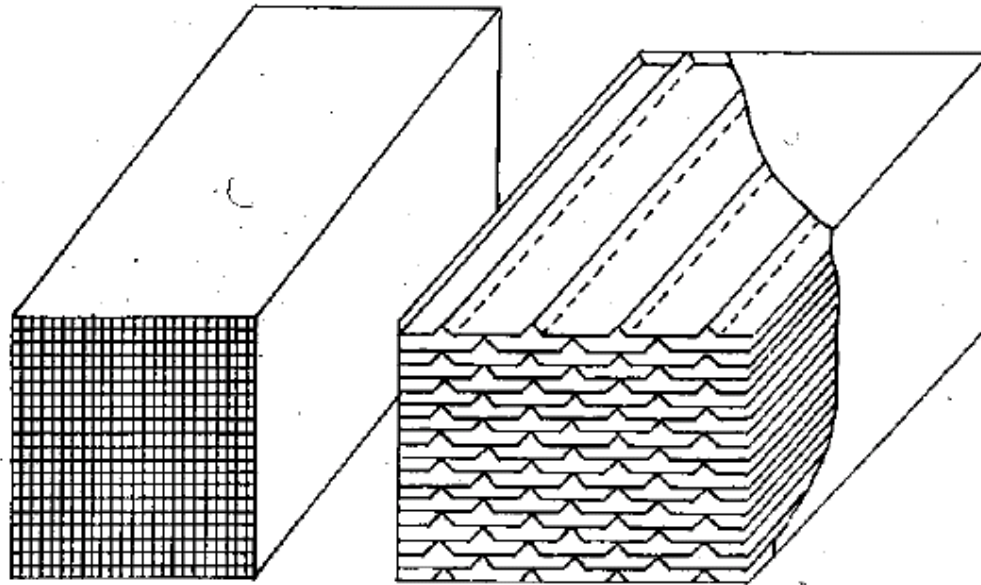
Temperature: **300 °C ~ 400 °C**

Catalyst : vanadium , Tungsten, Molybdenum oxide,
Titanium oxide

Typical flow of Denitrization of waste gas from a boiler



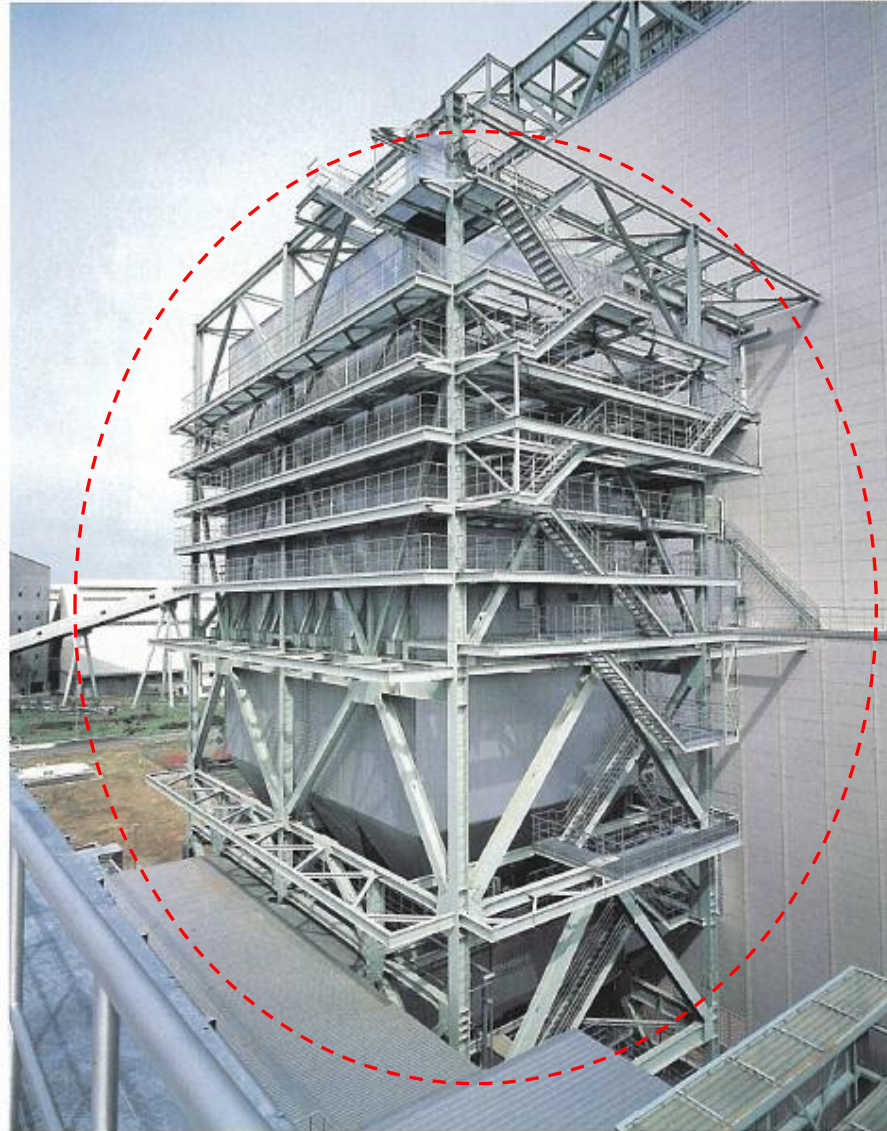
Typical structures of Denitrization Catalysts



Honey-comb Type

Plate Type

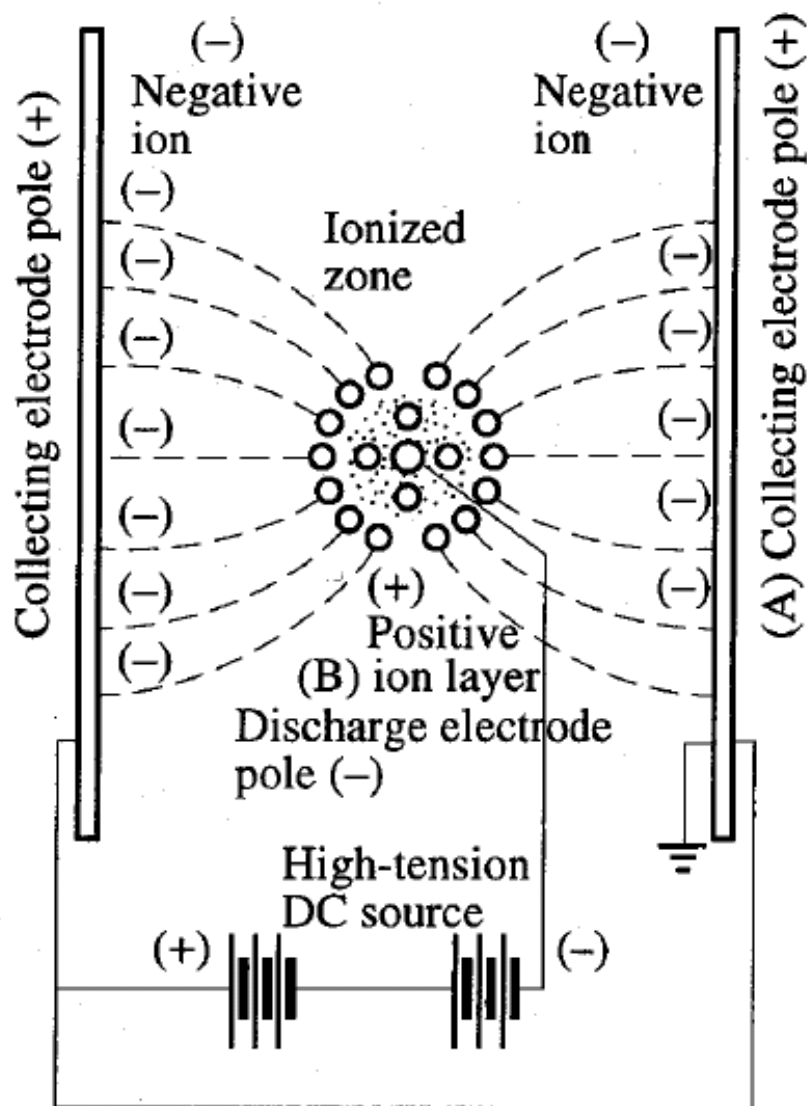
Denitrization Equipment



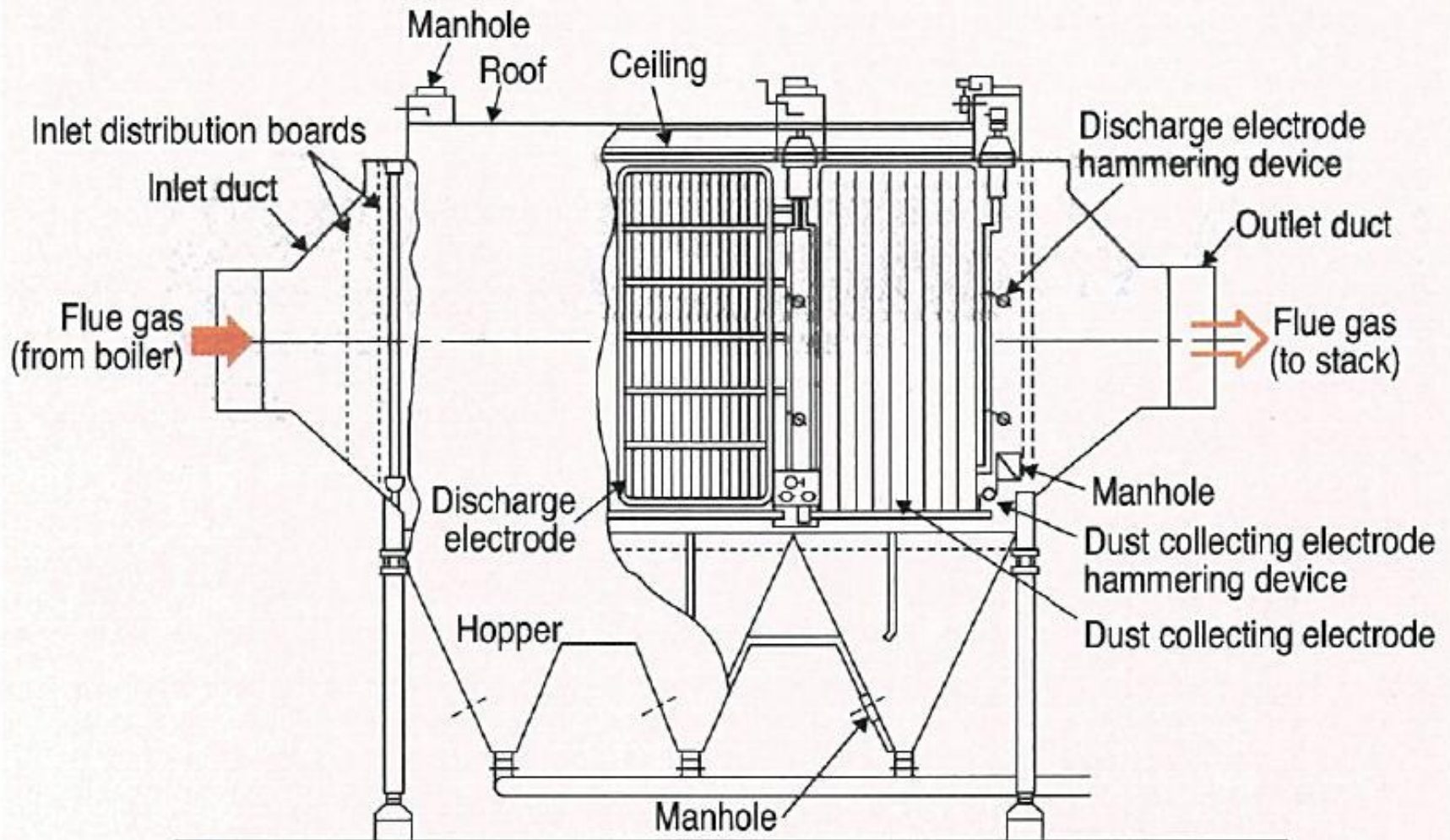
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5. Emission coefficient of NO_x and its reduction methods
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7. Hazardous gas treatment
8. Absorption methods
9. Adsorption methods

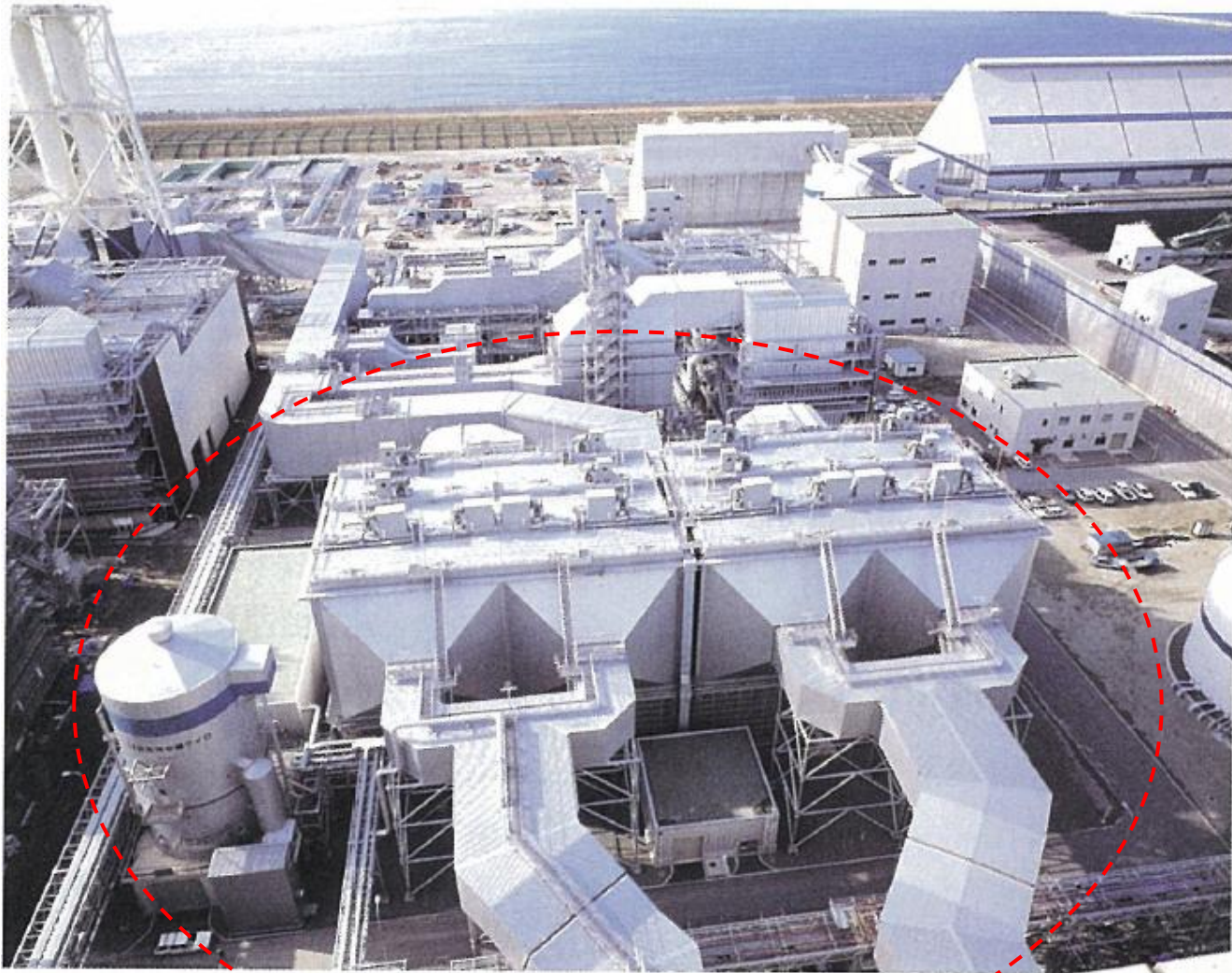
Electric field in an electrostatic precipitator (plate type)



Electrostatic Precipitator



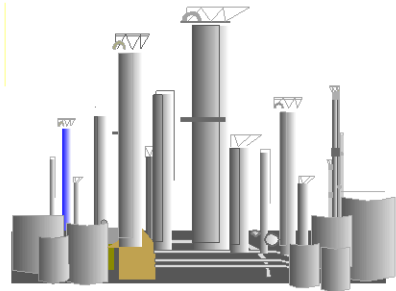
Electrostatic Precipitator



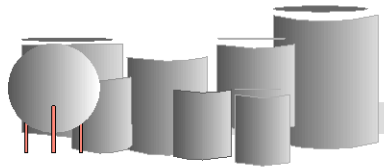
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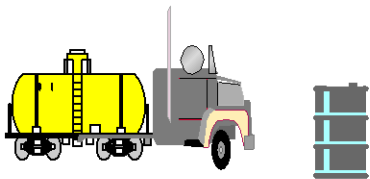
Waste Gas Treatments



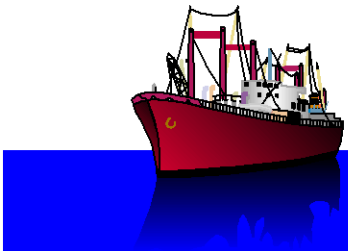
from Process



from Tanks



from Loading



from Shipping

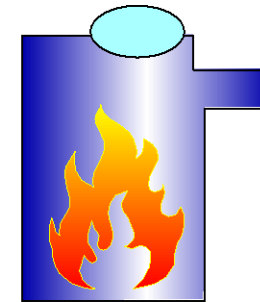
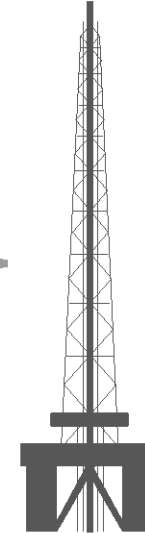


フレアースタック Flare stack



Incinerator / Heater

焼却炉
(加熱炉)

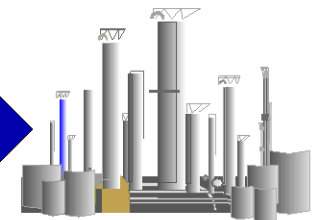
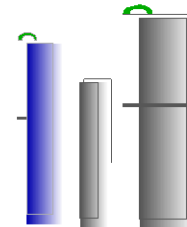


Absorption

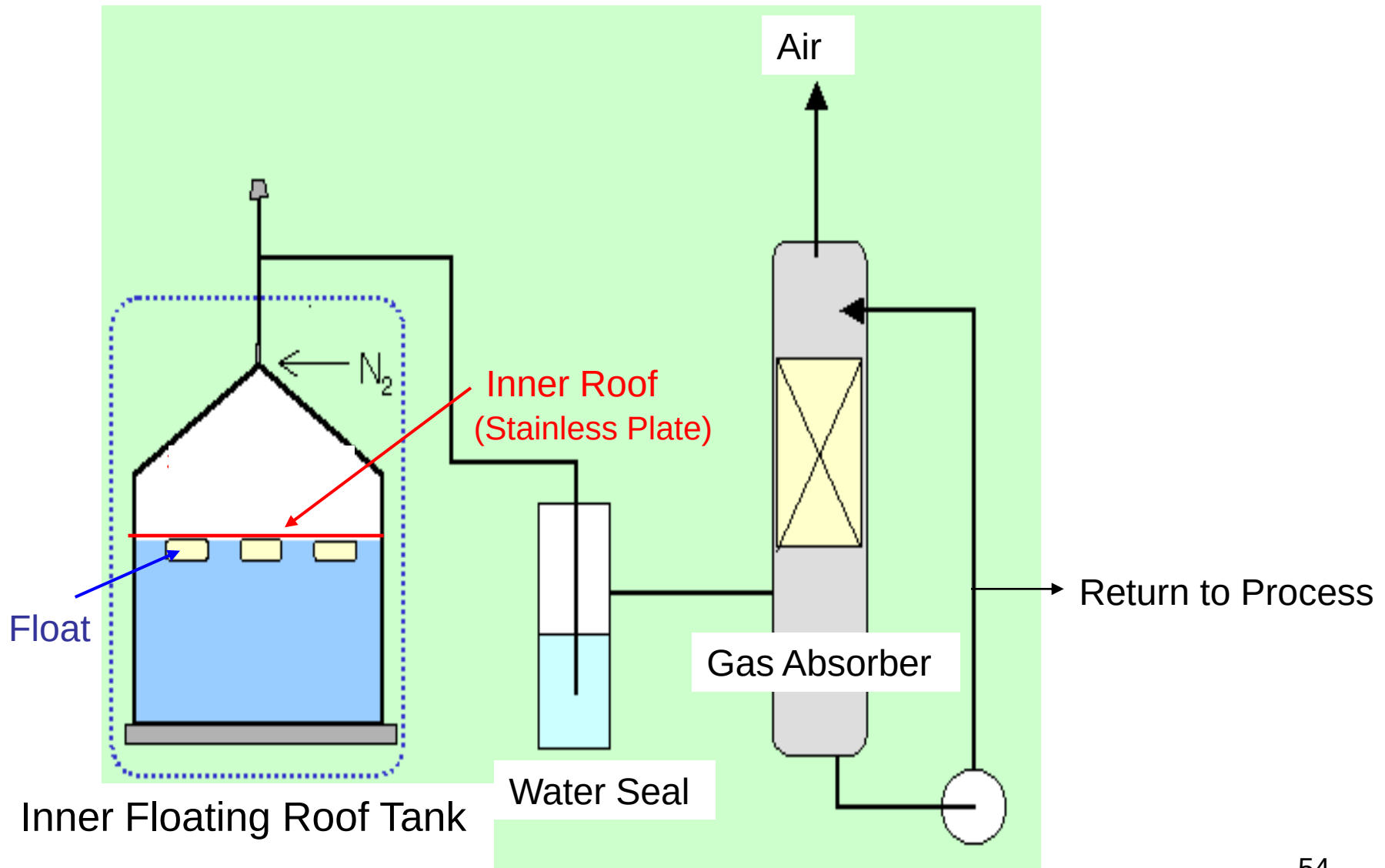
吸収



Recovery



Waste Gas Recovery system from a Tank



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Treatment of Various Gases with Absorption Process

Treatment of Hydrogen Chloride

Hydrogen chloride (HCl) is a colorless, irritating gas, which fumes in moist air. It is readily soluble in water; the solution is highly acidic and strongly corrosive to metals.

Water scrubbing is most extensively used to remove hydrogen chloride, but an alkaline solution is also employed as the absorbent to enhance absorption efficiency.

Process		Outline
Absorption	Water scrubbing	Because of the high solubility in water, a high absorption efficiency can be achieved by increasing the liquid/gas ratio. The spent absorbent solution may be discharged after neutralization, or hydrogen chloride may be recovered from it.
	Absorption with Alkali	A caustic soda solution or a slurry of slaked lime is used as the absorbent when an especially high absorption efficiency is required. Reaction formulae : $\text{NaOH} + \text{HCl} = \text{NaCl} + \text{H}_2\text{O}$ $\text{Ca(OH)}_2 + 2\text{HCl} = \text{CaCl}_2 + 2\text{H}_2\text{O}$

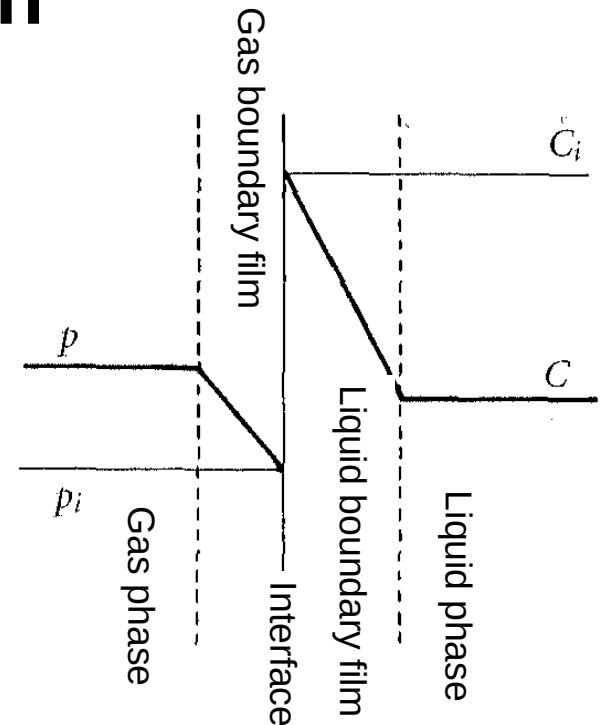
Theory of gas absorption

<Double film theory>

Two boundary film : Vapor side and liquid side,
to reduce diffusion velocity

- Gas phase film coefficient of mass k_G
- Liquid phase film coefficient of mass k_L

Driving force of diffusion:
difference of pressure and concentration



< Film coefficient of mass and Total coefficient of mass >

Gas phase diffusion velocity = Liquid phase diffusion velocity

NA: Mass transfer amount by unit time

$$N_A = k_G (p - p_i) = k_L (C_i - C) \quad (\text{Stable condition, mass transfer amount})$$

$$N_A = K_G (p - p_i) = K_L (C_i - C) \quad (\text{Alternate with total coefficient of mass})$$

k_G & k_L : impossible to measure

→ alternate with Gas phase total coefficient of mass K_G and Liquid phase total coefficient of mass K_L

Selection of gas absorption equipment

<Gas phase control and liquid phase control>

Gas absorbed

Suitable type of equipment

Low solubility
gas

Control by liquid
phase coefficient

Equipment to
reduce liquid
phase resistance

Gas diffusion
type equipment

Perforated plate column
Bubble cap column
Jet scrubber

High solubility
gas

Control by gas
phase coefficient

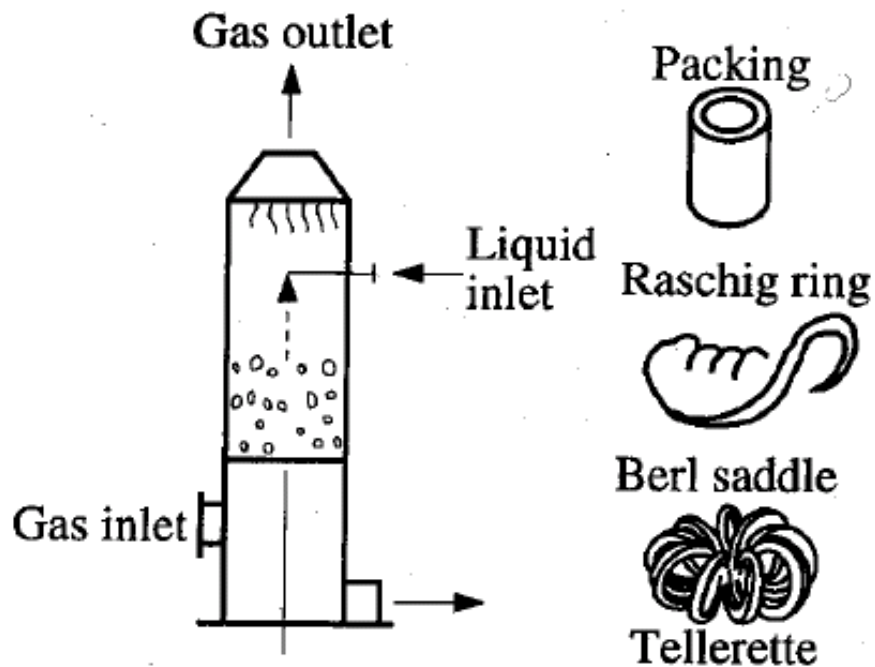
Equipment to
reduce gas
phase resistance

Liquid diffusion
type equipment

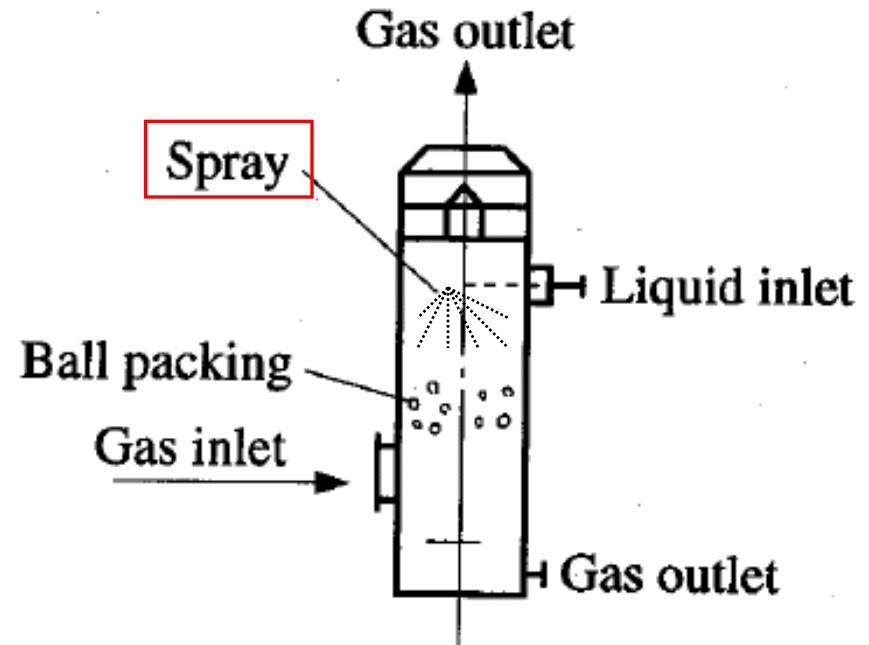
Packed tower
Spray tower
Venturi scrubber
Floating bed scrubber
Wetted-wall tower
Cyclone scrubber
Cross contact flow type

Types of absorption towers (1/6)

Liquid dispersion type



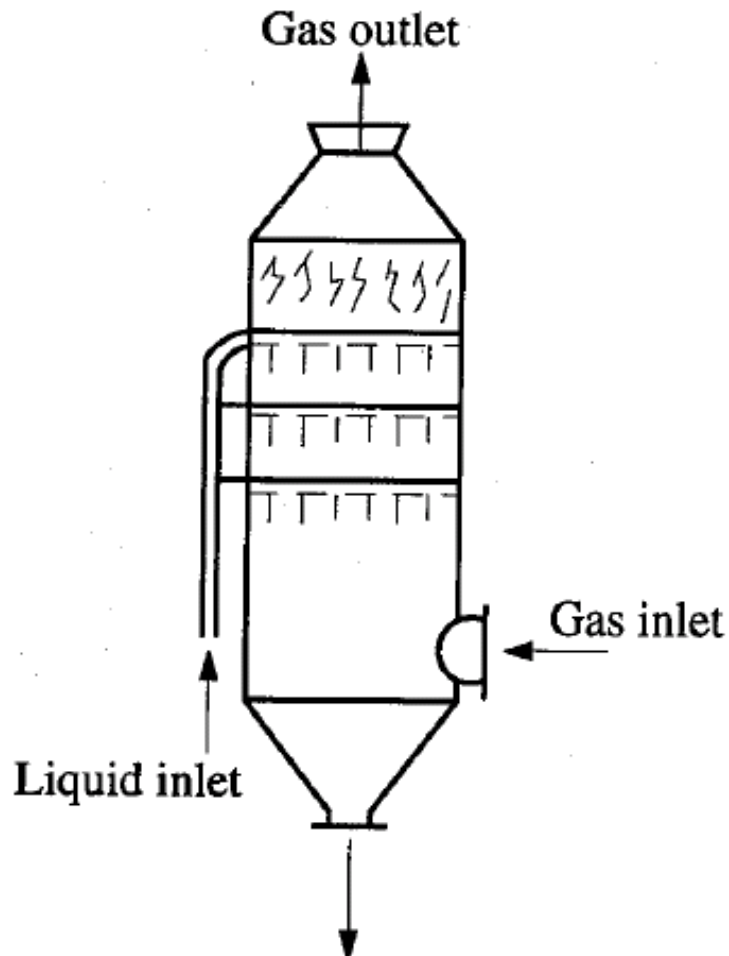
Packed tower



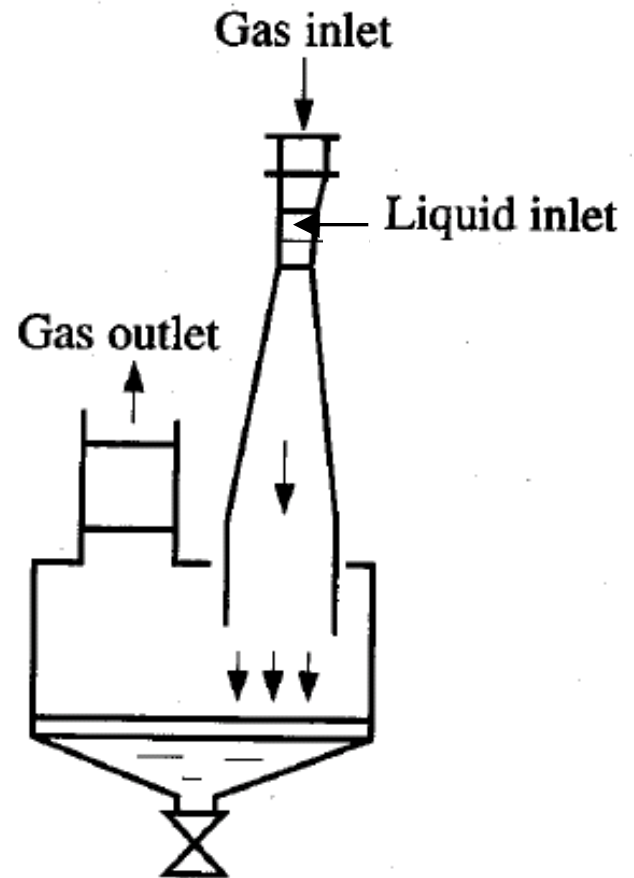
Turbulent
contact absorber

Types of absorption towers (2/6)

Liquid dispersion type



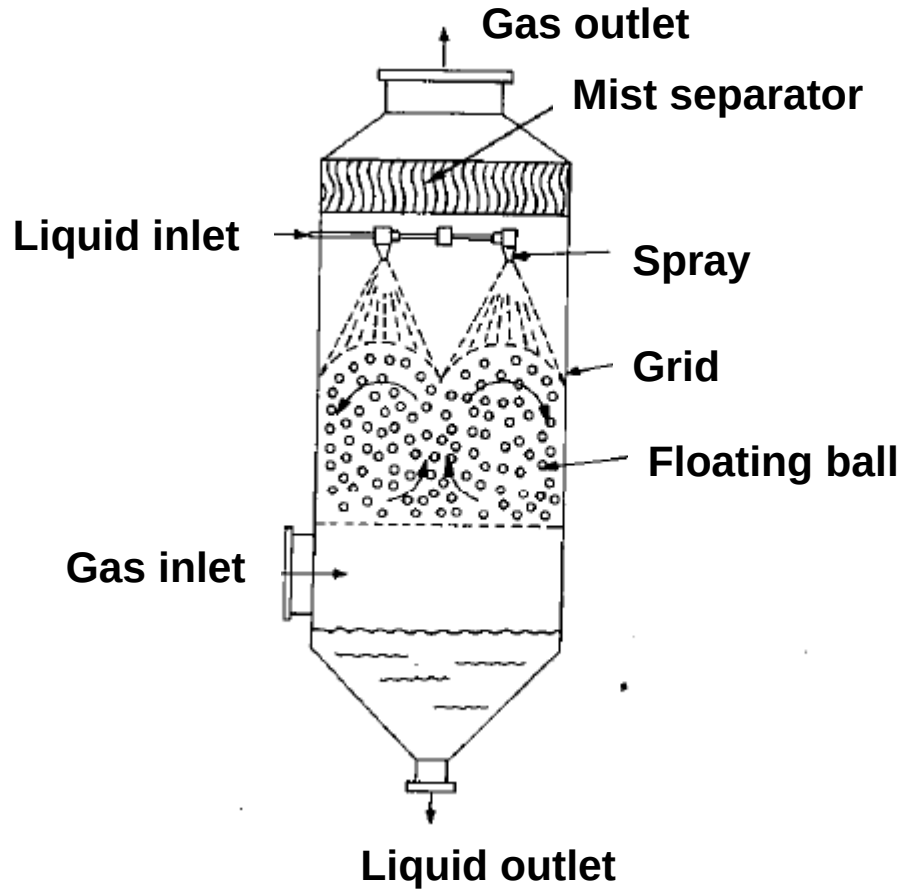
Spray tower



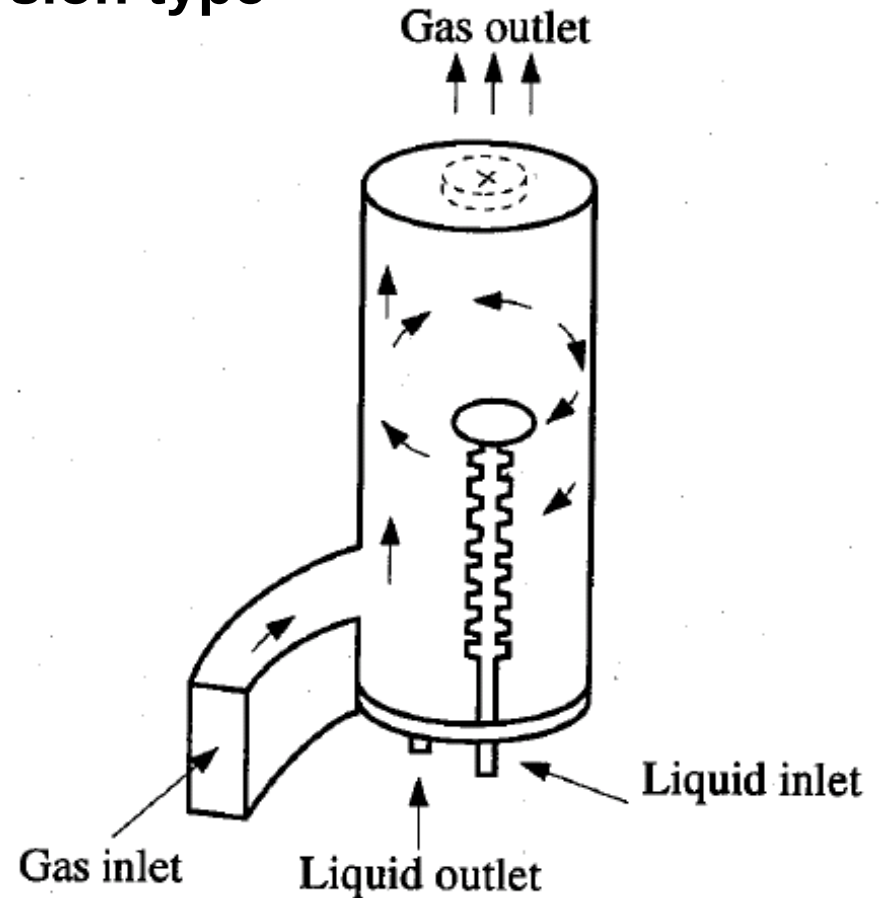
Venturi scrubber

Types of absorption towers (3/6)

Liquid dispersion type



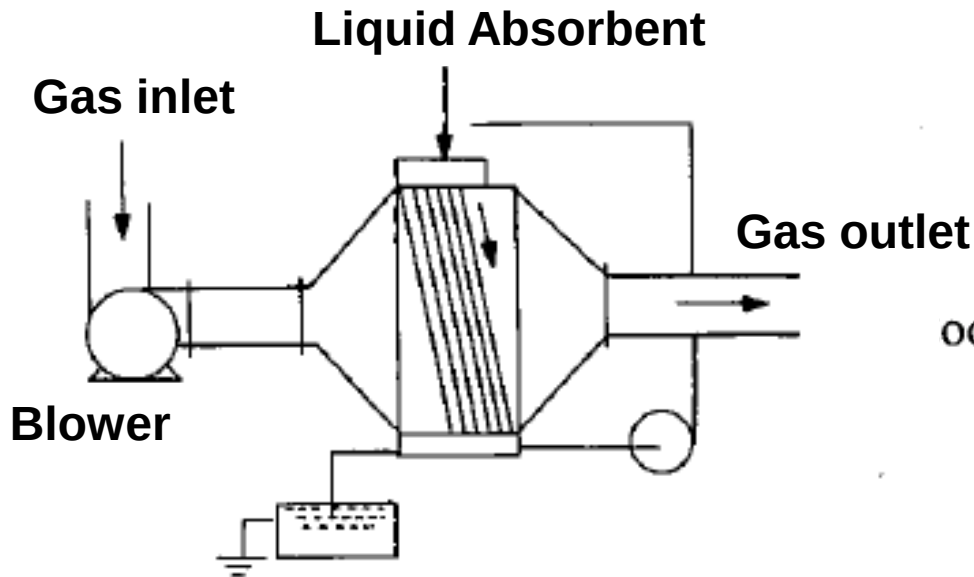
Floating bed scrubber



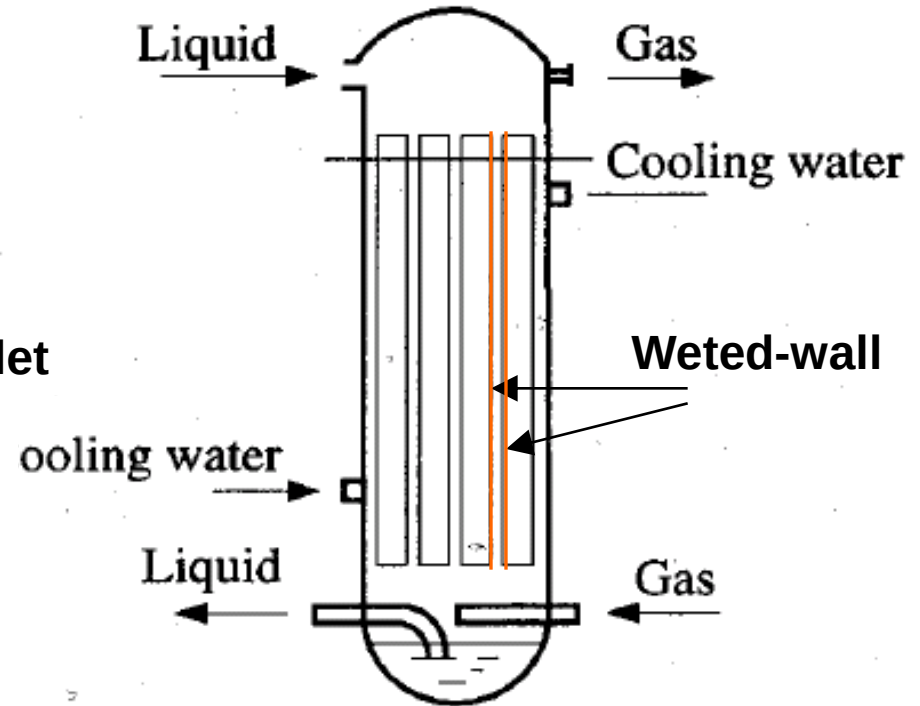
Cyclone scrubber

Types of absorption towers (4/6)

Liquid dispersion type



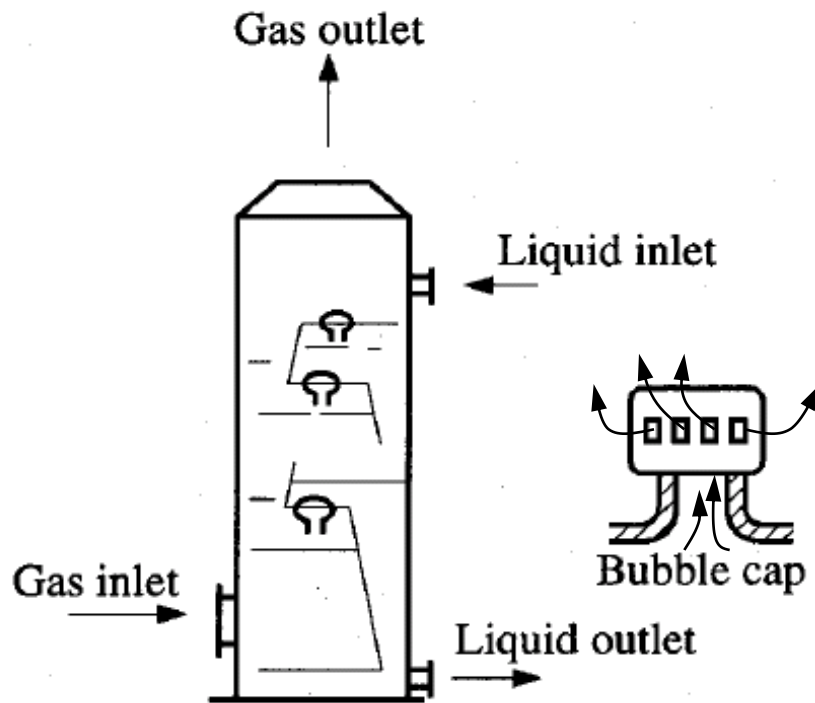
Cross contact flow type



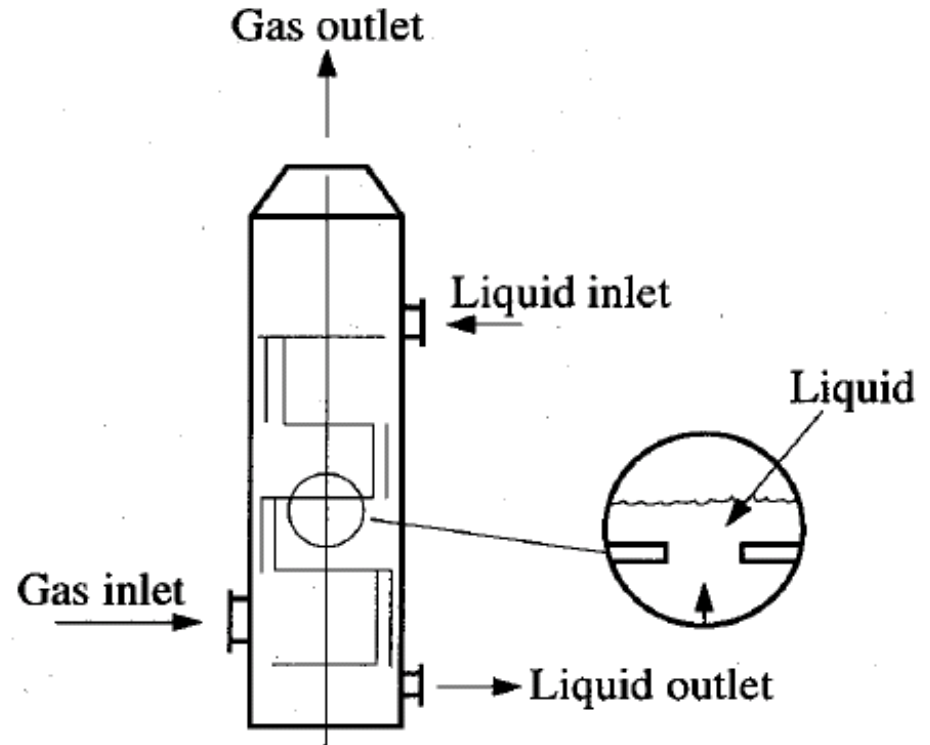
Wetted-wall tower

Types of absorption towers (5/6)

Gas dispersion type



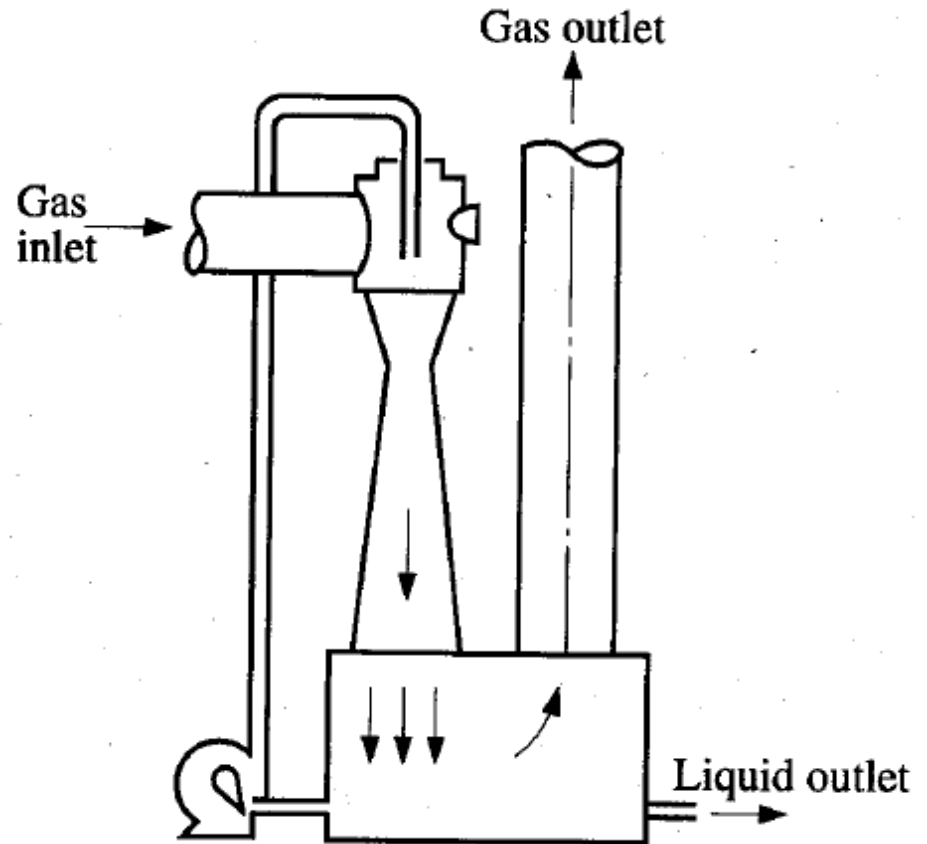
Bubble cap column



Perforated plate column

Types of absorption towers (6/6)

Gas dispersion type

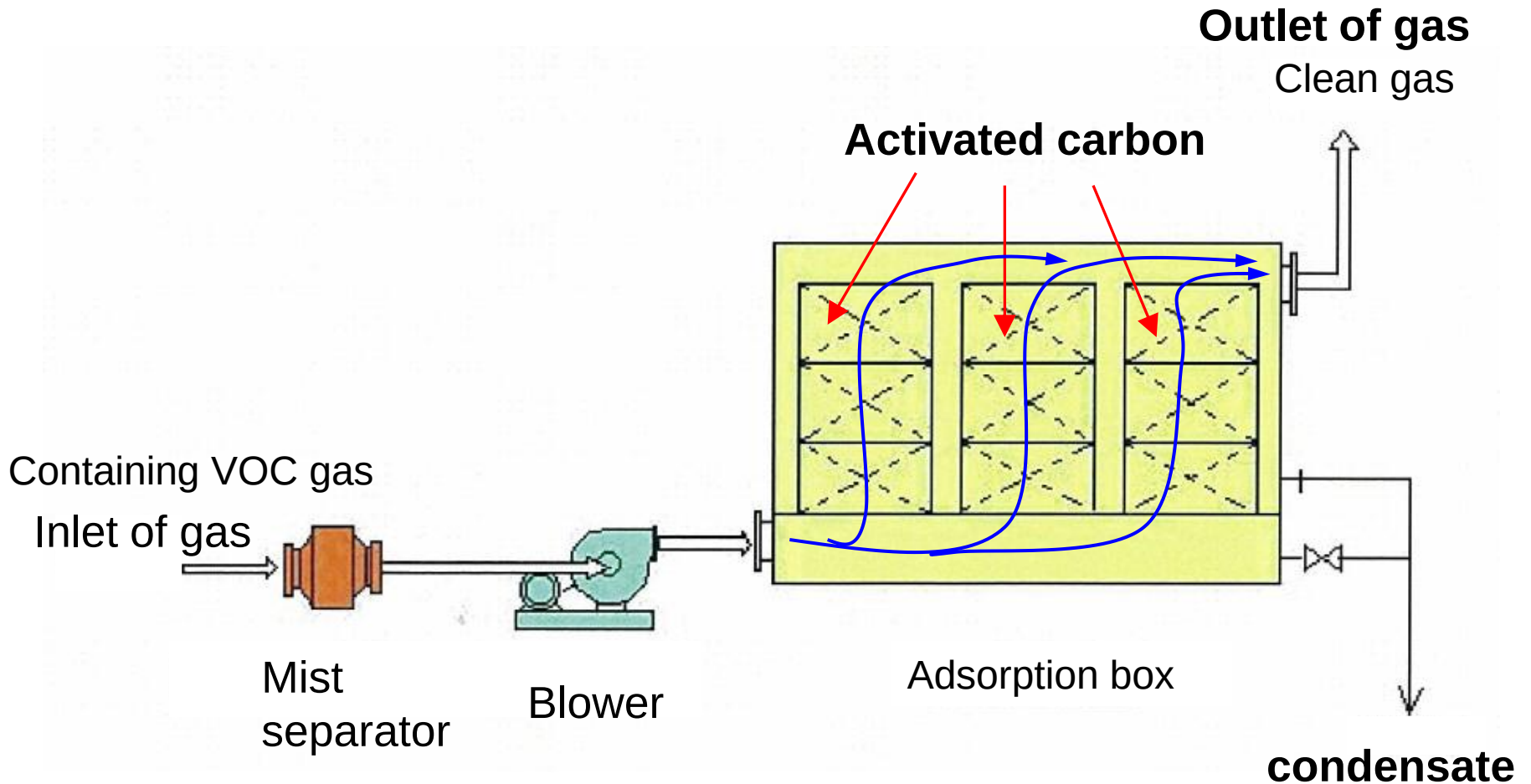


Jet scrubber

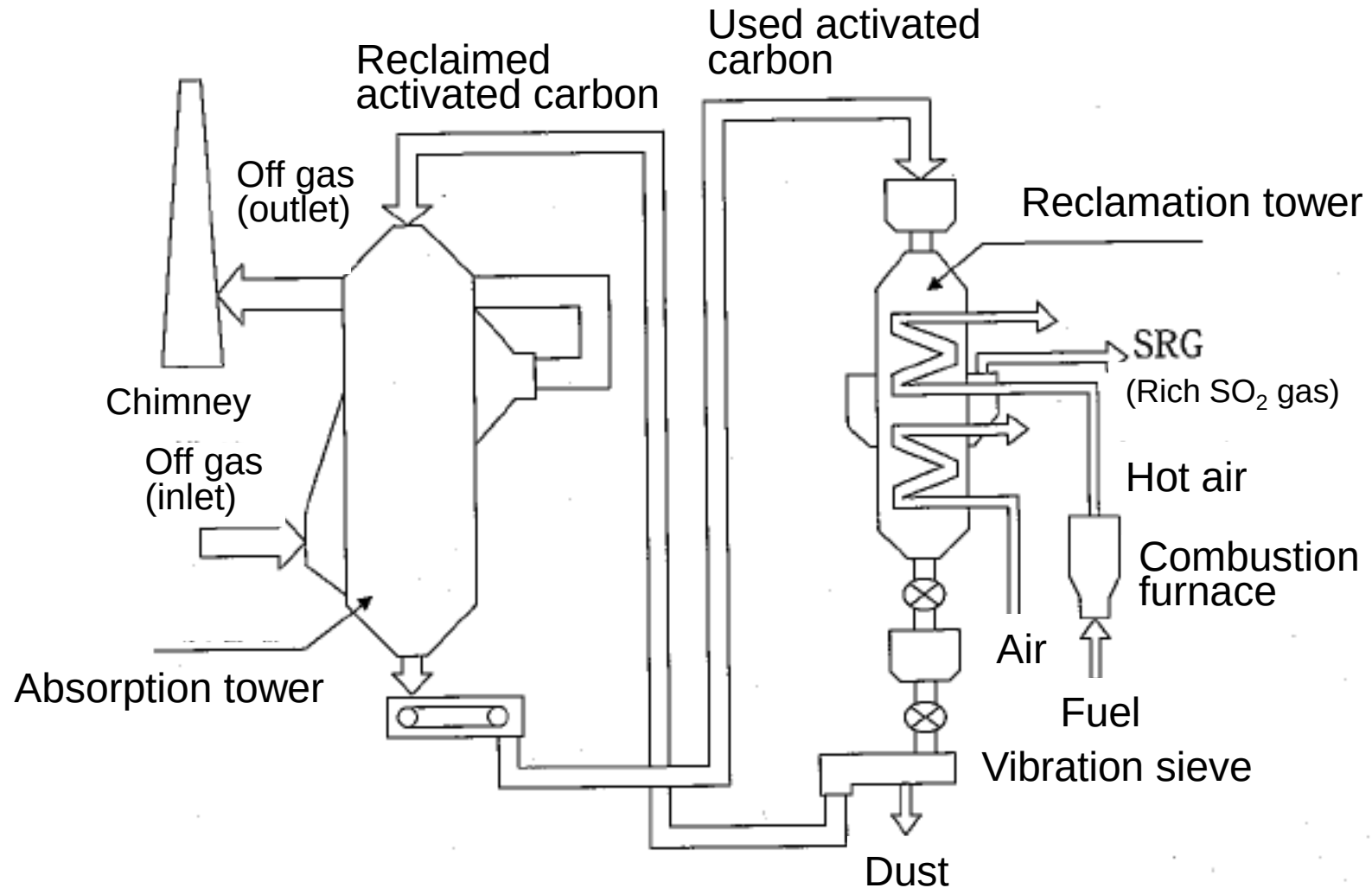
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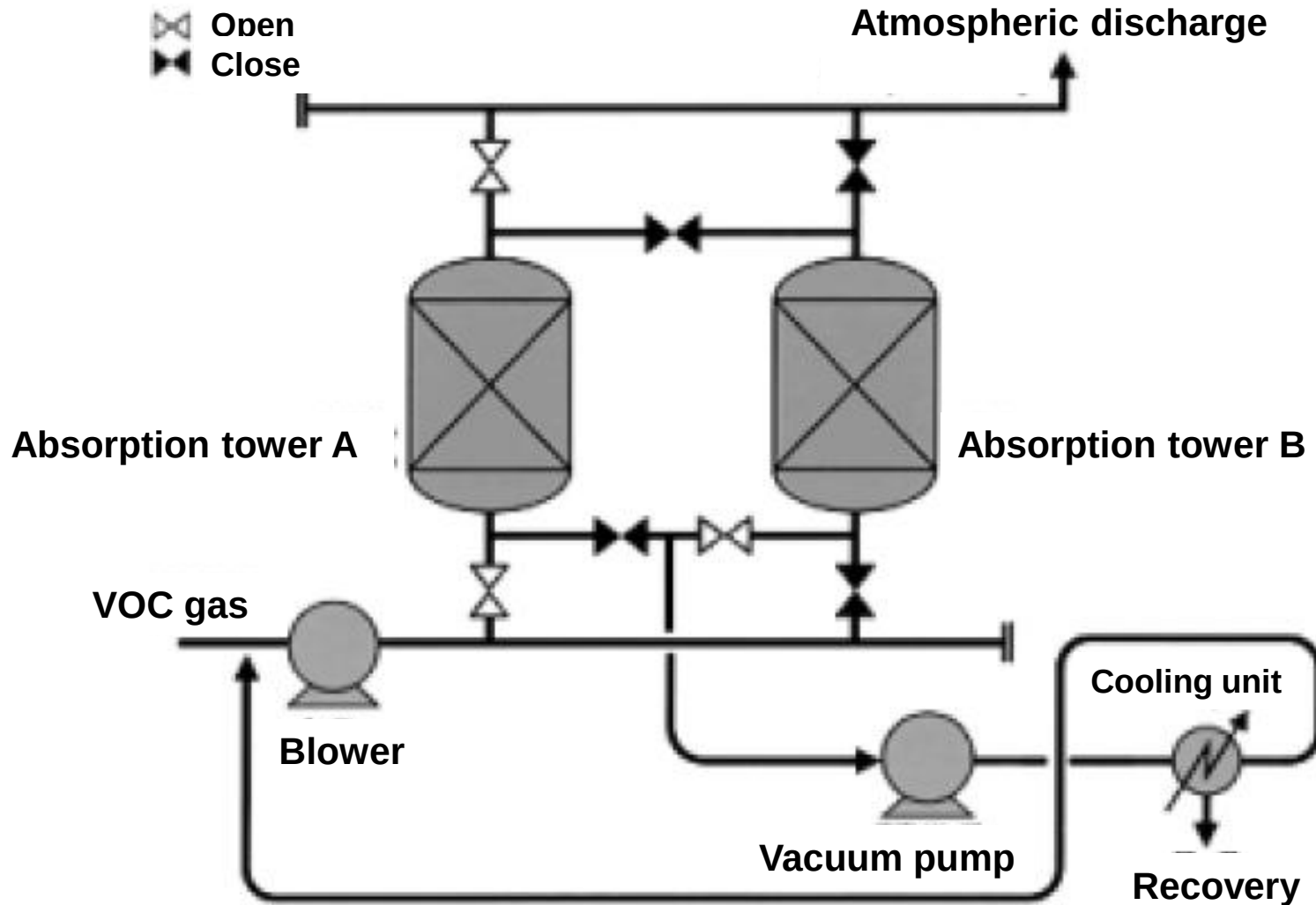
Adsorption with activated carbon



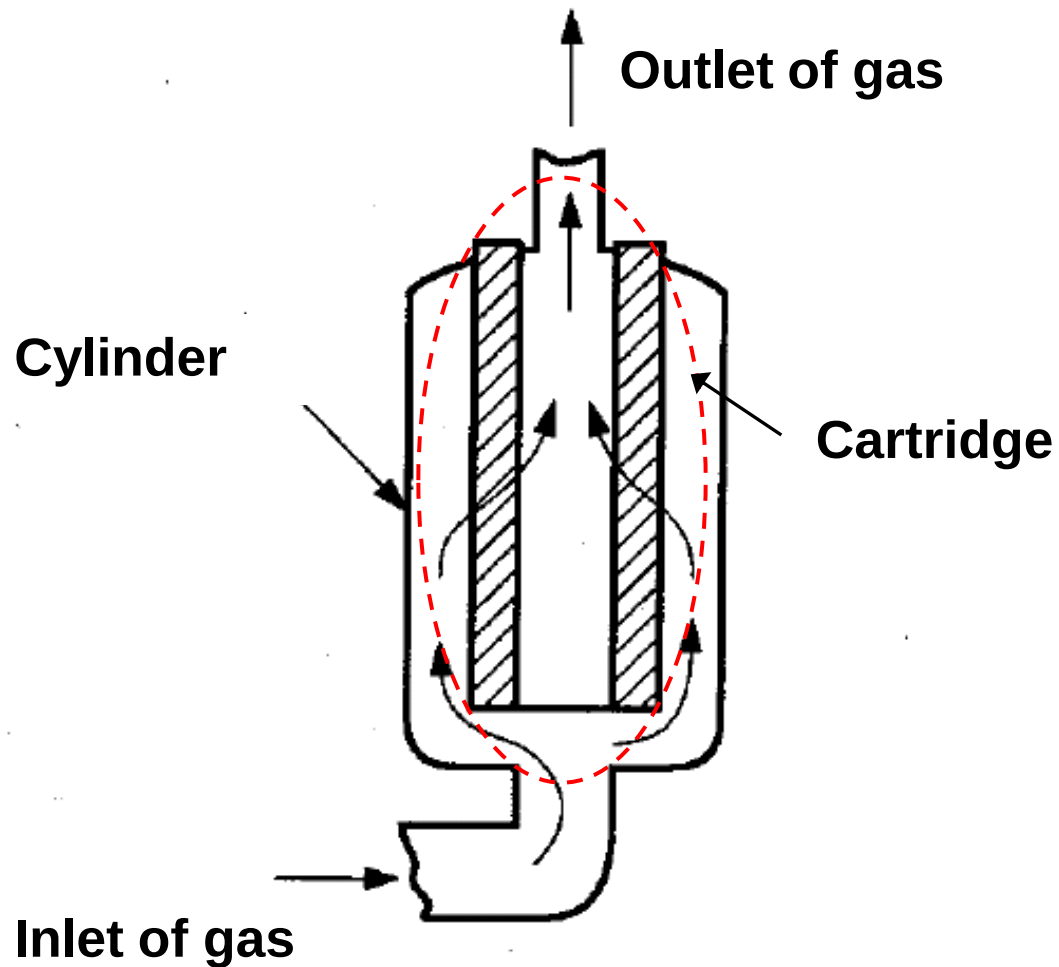
Activated carbon recycle process



Pressure swing process



Cartridge type Adsorption with activated carbon



Thank you for your attention !!

